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Modeling and Optimization of Engineering Systems



A felsőfokú informatikai oktatás minőségének fejlesztése, modernizációja

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COMBINATORIAL FRAMEWORK FOR PROCESS DESIGN AND SYNTHESIS



OUTLINE

- GENERAL INTRODUCTION
- ILLUSTRATION OF THE THEORETICAL AND PRACTICAL DIFFICULTIES IN ALGORITHMIC PROCESS SYNTHESIS
- COMBINATORIAL TECHNIQUE IN PROCESS DESIGN AND SYNTHESIS
- ADDITIONAL APPLICATIONS
- SCHEDULING OF MULTIPURPOSE BATCH PLANTS
- CONCLUDING REMARK
- REFERENCES



GENERAL INTRODUCTION



COMBINATORIAL PROBLEMS IN CHEMICAL ENGINEERING

- Almost all problems in chemical engineering especially in process design and operations, involve major (or at least some) combinatorial aspects.
- Examples
 - Process synthesis
 - Reaction-pathway (mechanism) identification
 - Scheduling
 - Molecular design etc.





CONVENTIONAL APPROACH TO SOLVE PROCESS DESIGN AND OPERATIONS PROBLEMS

- Formulation as a general mathematical programming problem (e.g., MILP, MINLP, NLP)
- Application of a general-purpose solver (e.g., GAMS)
- Outcome:

A practical problem is too complex for the solver

or

a solvable problem is too simple to be practical.





CONVENTIONAL APPROACH TO SOLVE PROCESS DESIGN AND OPERATIONS PROBLEMS (Cont'd)

Solution 1
 Awaiting for a faster computer.
 It may be futile: A computer thousand times faster can solve a problem with only 10 additional binary variables.

 Solution 2 Compromising on the quality of the mathematical model.

 Solution 3 Exploit the specific structure of the problem to accelerate the search.





OUR GENERAL PHILOSOPHY IN SOLVING COMPLEX PROCESS DESIGN AND OPERATIONS PROBLEMS

To develop

a problem formulation that manifests the unique structure of the class of problems

and

a solution procedure that exploits the specific structure of the problem.

- Result: enormous acceleration (industrial problems become solvable)
- Requirement: in-depth understanding of both the engineering and mathematical aspects of the problem
- The efficacy of our paradigm will be illustrated with process synthesis and scheduling.





ALGORITHMIC PROCESS SYNTHESIS

Given:

set of products, set of raw materials, mathematical models of the operating units

Generate:

optimal process or best processes or every feasible process

Optimality criteria:

cost, waste generation, controllability, risk, combinations of them





QUESTION

Is there any method for algorithmic process synthesis?





CONVENTIONAL MATHEMATICAL PROGRAMMING PROBLEM



Comment: It is unsuitable for process synthesis.





ALGORITHMIC PROCESS SYNTHESIS



Comment: Model generation is the heart of a synthesis problem.



ALGORITHMIC PROCESS SYNTHESIS



Comment: The major activity is performed manually.





RIGOROUS SUPER-STRUCTURE

Super-structure that guarantees the optimality.





FORMAL DEFINITION: RIGOROUS SUPER-STRUCTURE

- Process synthesis problems are not specified as standard optimization problem (objective function and constraints).
- Suppose that systematic procedure is available so that a valid mathematical programming model can be generated for a network of the given operating units.
- A network of operating units is defined to be a rigorous super-structure if the optimality of the resultant solution cannot be improved for any instance of the class of problems by any other procedure for network and model generation.





HOW CAN A RIGOROUS SUPER-STRUCTURE BE GENERATED

- Step1. Exploring key features of the structures of feasible processes (or the structures of optimal processes) which are valid for each instance of the class of problems.
- Step2. Developing an algorithm that can generate a network including all structures possessing every key feature of these structures.

Illustration: separation network synthesis





DIFFICULTIES IN ALGORITHMIC PROCESS SYNTHESIS: ILLUSTRATION BY SEPARATION NETWORK SYNTHESIS





PROBLEM DEFINITION

Given:

multicomponent feed-streams,

single or multicomponent product-streams,

operating units (separators, dividers, mixers)

Generate:

the cost-optimal network





OPERATING UNITS

Separator simple and sharp



Mixer



Divider







COST FUNCTION OF A SEPARATOR

- Concave
- Strictly monotone increasing
- Zero for zero mass-load







SEPARATION NETWORK SYNTHESIS (SNS)







ILLUSTRATION OF THE DIFFICULTY OF SNS







UNEXPECTED PROPERTY: RECYCLING







SUMMARY OF STRUCTURAL PROPERTIES OF OPTIMAL SEPARATION NETWORKS

| Product streams | Pu | Pure | | Multicomponent | |
|-----------------|------------|------------|------------|----------------|--|
| Feed streams | Single | Multiple | Single | Multiple | |
| recycling | impossible | possible | possible | possible | |
| redundancy | impossible | possible | possible | possible | |
| premixing | impossible | possible | impossible | possible | |
| bypassing | impossible | impossible | possible* | possible * | |

* Maximal bypass is not necessary optimal





PROVED STATEMENTS ON THE STRUCTURAL PROPERTIES OF OPTIMAL SEPARATION NETWORKS

- If a network producing pure product-streams is optimal, each of its dividers must be in a loop of this network (concave, strictly monotone increasing, zero for zero mass-load cost function).
- An optimal separation network with a linear cost function do not contain recycling.
- Optimal separation networks with a nonlinear cost function may include redundant separators (concave, strictly monotone increasing, zero for zero mass-load cost function).
- An optimal separation network with a linear cost function may contain non-maximal bypasses.



SNS WITH LINEAR COST FUNCTION

This type of SNS problems is examined by:

Floudas (1987)

Wehe and Westerberg (1987)

Quesada and Grossmann (1995)





- Available algorithmic methods are usually based on incomplete super-structures.
- Available algorithmic mathematical programming models
 - do not exploit specific features of the class of problems, and
 - have nonlinear (bilinear) constraints.





PROPOSED METHOD

Features of the new method:

- Based on a rigorous super-structure
- Exploits the combinatorial features of the class of problems
- Generates better solution
- Faster





It generates the rigorous super-structure.





Step 1. (Initialization.)

- Step 1.1. Let each feed-stream (raw material) be represented by a vertex. Let each product-stream be represented by a vertex.
- Step 1.2. Assign a divider to every feed-stream and connect each feed-stream to the corresponding divider, and a mixer to each product-stream and connect the outlet stream from the mixer to the corresponding product-stream.





- Step 2. (Creating separators and establishing bypasses.)
 - Step 2.1. Create all types of separators, each of which performs a separation between any pair of components in the feed-stream into the divider, and connect an outlet stream from the divider to another separator.
 - Step 2.2. Connect the outlet-streams from the divider to the mixers for the product-streams if it is plausible.





Step 3. (Creating dividers.)

Consider every separator in the structure.

- Step 3.1. Assign a divider to each outlet stream from the separator.
- □ Step 3.2. Repeat Steps 2 and 3.





CLASS OF PROBLEMS TO ILLUSTRATE THE SUPER-STRUCTURE GENERATION

| Stream | | Component | |
|------------------|---|-----------|---|
| Feed-stream 1 | А | В | С |
| Feed-stream 2 | А | В | С |
| Product-stream 1 | А | В | - |
| Product-stream 2 | - | В | С |
| Product-stream 3 | - | - | С |


































[A,B,0]

[0,B,C]

M

M>









[A,B,0]

[0,B,C]

M

M





[A,B,0]

[0,B,C]

[0,0,C]





































MATHEMATICAL MODEL BASED ON RIGOROUS SUPER-STRUCTURE

Generated algorithmicallyLP





EXAMPLE SNS 1 (Quesada and Grossmann, 1995)

| Component | А | В | С |
|------------------|----|----|----|
| Feed-stream | 10 | 10 | 10 |
| Product-stream 1 | 6 | 4 | 2 |
| Product-stream 2 | 4 | 6 | 8 |

The objective function to be minimized is the sum of the total flows into the separators.



















EXAMPLE SNS 2 (Quesada and Grossmann, 1995)

| Component | А | В | С | | D |
|----------------------|------------|-----------|--------|--------|-----|
| Feed-stream 1 | 6 | 4 | 0 | | 0 |
| Feed-stream 2 | 8 | 6 | 10 |) | 6 |
| Feed-stream 3 | 0 | 0 | 5 | | 5 |
| Degree of Difficulty | 4 | 1 | | 4 | |
| | | | | | |
| Product | Sum of the | Component | | | |
| | components | | Inform | nation | |
| Product-stream 1 | 15 | A≥9 | B≤3 | C≤3 | D=0 |
| Product-stream 2 | 20 | B≥7 | C≥7 | B=C | |
| Product-stream 3 | 15 | D≥9 | A=0 | | |







Structure obtained by Quesada and Grossmann (1995) The value of the cost function is 138.7.







Optimal structure generated by the new method:

The value of the cost function is 104.3.





COMPARISON IN SOLVING EXAMPLE SNS 2

| Method based on | Number of variables | Type of model | Optimal solution | Computation time |
|---|---------------------|---------------|------------------|------------------|
| Quesada and Grossmann's super-structure | 113 | nonlinear | 138.7 | 0.74* |
| Proposed rigorous super- structure | 90 | linear | 104.3 | 0.55** |

* From the publication: on IBM RS600/530.
Note that we were not able to duplicate the result.
** On a PC (Pentium, 100MHz) with GAMS as the solver



CONCLUDING REMARKS ON SEPARATION NETWORK SYNTHESIS

- This simple class of synthesis problems illustrates:
 - the difficulty of synthesis
 - the need for mathematical foundation
 - algorithmic solution (optimality guaranteed)





COMBINATORIAL TECHNIQUE IN PROCESS DESIGN AND SYNTHESIS





INTRODUCTION

MINLP

```
min g(x,y)
```

s.t.

```
\begin{array}{l} \mathsf{f}(\mathsf{x},\,\mathsf{y}) \leq & \\ \mathsf{x} \in \mathfrak{R}^{\mathsf{n}} \,,\, \mathsf{y} \in \{0,\,1\}^{\mathsf{m}} \end{array}
```

- Most MINLP model can not represent a practical problem.
- Additional information is embedded implicitly in the model of a practical problem.
- Idea: this information can effectively control the procedure.





ILLUSTRATIVE EXAMPLE PNS 1

Operating units: $c \rightarrow 1$ $f \rightarrow 2$ A $E \rightarrow 3$ c $F \rightarrow 3$ c $F \rightarrow 4$ $G \rightarrow 5$ $D \rightarrow 6$ F $K \rightarrow 7$ + H



Raw materials: E, G, J, K, L

Feasible flowsheet





EXAMPLE PNS 1

Product: A Raw materials: E, G, J, K, L Plausible operating units

| Type | Inputs | Outputs |
|------|--------|---------|
| 1 | С | A, F |
| 2 | D | A, B |
| 3 | E, F | С |
| 4 | F, G | C, D |
| 5 | G, H | D |
| 6 | J | F |
| 7 | K, L | Н |





Number of

operating units:7binary variables:7combinations:127 (=27-1)





SYNTHESIS OF AN INDUSTRIAL PROCESS (EXAMPLE PNS 2)

Product: A61

Raw materials: A1, A2, A3, A4, A6, A7, A8, A11, A15, A17, A18, A19, A20, A23, A27, A28, A29, A30, A34, A43, A47, A49, A52, A54





PLAUSIBLE OPERATING UNITS

| No. | Туре | Inputs | Outputs |
|-----|-----------|-----------------|---------------|
| 1 | Feeder | A1 | A5 |
| 2 | Reactor | A2, A3, A4 | A9 |
| 3 | Reactor | A3, A4, A6, A11 | A10 |
| 4 | Reactor | A3, A4, A5 | A12 |
| 5 | Reactor | A3, A4, A5 | A13 |
| 6 | Reactor | A7, A8, A14 | A16 |
| 7 | Reactor | A8, A14, A18 | A16 |
| 8 | Separator | A9, A11 | A21, A22, A24 |
| 9 | Separator | A10, A11 | A22, A24, A37 |
| 10 | Separator | A12 | A25, A26 |
| 11 | Separator | A13 | A25, A31 |
| 12 | Dissolver | A15, A16 | A32 |





PLAUSIBLE OPERATING UNITS (Cont'd)

| No. | Туре | Inputs | Outputs |
|-----|------------|-------------------------|---------------|
| 13 | Reactor | A14, A17, A18, A19, A20 | A33 |
| 14 | Reactor | A6, A21 | A35 |
| 15 | Washer | A22, A23 | A48 |
| 16 | Washer | A5, A24 | A36 |
| 17 | Separator | A5, A11, A25 | A37, A38, A39 |
| 18 | Separator | A11, A26 | A40, A42 |
| 19 | Reactor | A14, A27, A28, A29, A30 | A41 |
| 20 | Separator | A11, A31 | A40, A42 |
| 21 | Centrifuge | A32 | A44, A45 |
| 22 | Washer | A33, A34 | A46 |
| 23 | Separator | A36 | A14, A48 |
| 24 | Separator | A38 | A14, A48 |





PLAUSIBLE OPERATING UNITS (Cont'd)

| No. | Туре | Inputs | Outputs |
|-----|--------------|----------|----------|
| 25 | Filter | A41 | A50, A51 |
| 26 | Washer | A43, A44 | A53 |
| 27 | Filter | A46 | A55, A56 |
| 28 | Separator | A47, A48 | A5, A57 |
| 29 | Separator | A48, A49 | A5, A58 |
| 30 | Separator | A50 | A59, A60 |
| 31 | Dryer | A51, A54 | A61 |
| 32 | Dryer | A52, A53 | A61 |
| 33 | Dryer | A54, A55 | A61 |
| 34 | Distillation | A59 | A62, A63 |
| 35 | Separator | A60 | A64, A65 |





Number of

operating unit:35binary variables:35combinations:34 billion

subproblems at a B&B (worst case): 130 million





SOURCE OF COMPLEXITY

Combinatorial nature of the problem





COMBINATORIAL TOOLS

- Our rigorous technique is based on combinatorics, especially,
- on the following items.
 - P-graph
 - New structure representation.
 - Axioms
 - The fundamental properties of combinatorially feasible process structures (e.g., every operating unit has at least one path leading to a product).
 - Algorithms
 - Effective and rigorous combinatorial algorithms for process synthesis.





STRUCTURAL REPRESENTATION

- Simple directed graphs are incapable of providing an unambiguous representation in process synthesis.
- Process graphs or P-graphs are introduced for structural representation in process synthesis.





CONVENTIONAL AND P-GRAPH REPRESENTATION







FORMAL DEFINITION: P-GRAPH

- A P-graph can be considered as a directed bipartite graph.
 - M is the set of materials O is the set of operating units, where $O \subseteq \wp(M) \times \wp(M), O \cap M = \emptyset$
- If (α,β)∈O, then, α is the input set, and β is the output set of this operating unit.
- Pair (M,O) is defined to be a P-graph with the set of vertices MUO and the set of arcs

 $\{(x,y): y=(\alpha,\beta)\in O \& x\in\alpha\} \cup \{(y,x): y=(\alpha,\beta)\in O \& x\in\beta\}.$







M1={A, B, C, D, E, F} O1={({B, C}, {A}), ({D, E}, {B, C}), ({F}, {A, C})}







FORMAL DESCRIPTION OF THE COMBINATORIAL COMPONENT OF PNS

- Let a finite set of materials M be given.
- The combinatorial components of a PNS problem is given by triplet (P,R,O)

where

 $P \subseteq M$ is the set of products to be produced

R⊆M is the set of raw materials

 $O \subseteq \wp(M) \times \wp(M)$ is the set of operating units.

• It is assumed that $P \cap R = \emptyset$.





P-GRAPH REPRESENTATION OF A SYNTHESIS PROBLEM PNS 2





— operating unit


AXIOMS OF COMBINATORIALY FEASIBLE PROCESS STRUCTURES

For given process synthesis problem, a P-graph satisfying the following five axioms is a combinatorially feasible structure.

- (S1) Every final product is represented in the structure.
- (S2) A material represented in the structure is a raw material if and only if it is not an output of any operating unit represented in the structure.
- (S3) Every operating unit represented in the structure is defined in the synthesis problem.
- (S4) Any operating unit represented in the structure has at least one path leading to a product.
- (S5) If a material belongs to the structure, it must be an input to or output from at least one operating unit represented in the structure.





ILLUSTRATIVE EXAMPLE FOR THE COMBINATORIALLY FEASIBLE STRUCTURES: EXAMPLE PNS 1

Operating units given:



Available raw materials: E, G, J, K, L Product: A





COMBINATORIALLY FEASIBLE STRUCTURES OF EXAMPLE PNS 1







COMBINATORIALLY FEASIBLE STRUCTURES OF EXAMPLE PNS 1 (Cont'd)







COMBINATORIALLY FEASIBLE STRUCTURES OF EXAMPLE PNS 1 (Cont'd)







SYNTHESIS OF AN INDUSTRIAL PROCESS (EXAMPLE PNS 2)

Product: A61

Raw materials: A1, A2, A3, A4, A6, A7, A8, A11, A15, A17, A18, A19, A20, A23, A27, A28, A29, A30, A34, A43, A47, A49, A52, A54





The five axioms reduce the

34 billion combinations of the operating units to 3,465 combinatorially feasible structures.

The optimal solution is included in the set of 3465 feasible structures.





ILLUSTRATION OF THE REDUCTION IN THE SEARCH SPACE







ILLUSTRATION OF THE REDUCTION IN THE SEARCH SPACE







ALGORITHMIC GENERATION OF THE MAXIMAL STRUCTURE





MAXIMAL STRUCTURE

- The union of all combinatorially feasible structures is called the maximal structure.
- The maximal structure is a rigorous superstructure.





MAXIMAL STRUCTURE OF THE ILLUSTRATIVE EXAMPLE PNS 1







ALGORITHM MSG: GENERATION OF THE MAXIMAL STRUCTURE

Input:

Synthesis problem given by set of raw materials set of products set of candidate operating units Output:

maximal structure





ALGORITHM MSG: GENERATION OF THE MAXIMAL STRUCTURE

- inputs: sets M, P,R, O; comment: P \subseteq M, R \subseteq M, O \subseteq p(M)×p(M), O \cap M=Ø, P \cap R=Ø;
- **output:** maximal structure (m,o) of synthesis problem (P, R, O);

begin

reduction part of the algorithm; composition part of the algorithm; end







```
O:=O\φ⁻(R);
M:=\Psi(0);
r:=\Psi^{-}(O)\setminus(\Psi^{+}(O)\cup R);
while r is not empty do
begin
let x be an element of r;
M:=M\setminus\{x\};
o:= φ<sup>+</sup>({x});
0:=0\o;
r:=(r\cup( \Psi^+(o)\ \Psi^+(O)))\{x};
end;
if P \cap M \neq P then stop;
comment: there is no maximal structure;
```







p:=P; m:= \emptyset ; o:= \emptyset ; while p is not empty do begin let x be an element of p; m:=m \cup {x}; o_x:= ϕ^{-} ({x}); o:=o \cup o_x; p:=(p \cup Ψ^{-} (o_x))\(R \cup m); end; m:= Ψ (o);

Note: The complexity of algorithm MSG is polynomial.





Example (Generation of the maximal structure)

Materials:

```
M={A, B, C, D, E, F, G, H, I, J, K, L, M,N, Q, T, U, V},
```

Product:

 $P=\{B\}$

Raw materials:

R={F, H, M, T}

Operating units:

```
 \begin{split} & O = \{(\{C, D, F\}, \{A\}), (\{D\}, \{B,G\}), \\ & (\{E\}, \{B, U\}), (\{F, G\}, \{C, D\}), \\ & (\{G, H\}, \{D\}), (\{H, I\}, \{E\}), \\ & (\{G, H\}, \{D\}), (\{H, I\}, \{E\}), \\ & (\{J, K\}, \{E\}), (\{M\}, \{G\}), \\ & (\{J, K\}, \{E\}), (\{M\}, \{G\}), \\ & (\{N, Q\}, \{H\}), (\{T, U\}, \{I\}), \\ & (\{V\}, \{J\})\}. \end{split}
```













Sturcture generated by statements st1 and st2; materials belonging to set r of st3 are underlined.







Structure generated after the first iteration of loop lp4.

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Structure generated after the third iteration of loop lp4.







Structure of the first iteration of loop Ip7.





Structure of the second iteration of loop lp7.



















Structure after the fifth iteration of loop lp7.











ALGORITHMIC GENERATION OF FEASIBLE STRUCTURES





OBSERVATION

The axioms are not in procedural form to generate process structures: additional tool is required





DECISION-MAPPING

Decision-mapping is a novel mathematical notion to render the complex decisions in process synthesis consistent and complete.





FORMAL DEFINITION: DECISION MAPPING

- Mapping or function is a subset of a Cartesian product of domain D and range R.
- Function f is a set of pairs (x, y) where x∈D and y=f(x)∈R; this set of pairs is denoted by f[D].
- Let ∆ be a mapping from M to the set of subsets of O, i.e., ∆[M] _ M× ℘ (O). This mapping determines the set of operating units producing material X for any X∈M.
- Δ(X)={(α, β):(α, β)∈O and X∈β} where m is a subset of M X is an element of m.
- δ[m]={(X, δ(X)):X∈m} is a decision mapping on m if δ(X) is a subset of Δ(X) for each X∈m.

(See Friedler et al., 1995b)





Example



Maximal decision mapping Δ represents the whole structure where

 $\Delta[\{A, B, C, D, E,\}] = \{(A, \Delta(A)), (B, \Delta(B)), (C, \Delta(C)), (D, \Delta(D)), (E, \Delta(E)), (F, \Delta(F))\}$





Example (Cont'd)



Decision mapping $\delta 1$ represents a substructure where $\delta 1[\{A, B\}] = \{(A, \delta_1(A)), (B, \delta_1(B))\}$





ALGORITHM SSG FOR GENERATING ALL SOLUTION-STRUCTURES OF A SYNTHESIS PROBLEM

Input: Maximal structure

Output:

All solution-structures of the synthesis problem





ALGORITHM SSG FOR GENERATING ALL SOLUTION-STRUCTURES OF A SYNTHESIS PROBLEM

input: M, P, R, ∆[M];

comment: P, R, Δ [M] belong to synthesis problem (P, R, O), where

 $\begin{array}{l} \mathsf{P}_{\underline{\subset}}\mathsf{M}, \ \mathsf{R}_{\underline{\subseteq}}\mathsf{M}, \ \mathsf{P}_{\underline{\frown}}\mathsf{R} = \varnothing, \ \Delta(\mathsf{x}) = \{(\alpha, \ \beta) | (\alpha, \ \beta) \in \mathsf{O} \ \& \ \mathsf{x}_{\underline{\in}}\beta\}, \ \Delta(\mathsf{x}) = \emptyset \Leftrightarrow \mathsf{x}_{\underline{\in}}\mathsf{R}, \end{array}$

 Δ [M] = {(x, Δ (x))|x \in M}, δ [m] is a decision-mapping on (M, O); **output:** all solution-structures of synthesis problem (P, R, O); **global variables:** R, Δ [M];

begin if $P = \emptyset$ then stop; SSG(P, \emptyset , \emptyset) end



```
procedure SSG( p, m, \delta[m] )
begin
if p = \emptyset then begin write \delta[m]; comment: \delta[m] defines a solution-structure;
                 return
                                  end
let x \in p;
\mathsf{C}:= \wp(\Delta(\mathsf{x})) \setminus \{\emptyset\};
for all c \in C do
                 begin
                 if \forall y \in m, c \cap \delta(y) = \emptyset & (\Delta(x) \setminus c) \cap \delta(y) = \emptyset
                  then
                     begin
                    \delta[\mathsf{m} \cup \{\mathsf{x}\}] := \delta[\mathsf{m}] \cup \{(\mathsf{x}, \mathsf{c})\};
                    SSG(p\cupmat<sup>in</sup> (c))\(R\cupm\cup{x}), m\cup{x}, \delta[m\cup{x}])
                     end
                 end
return
end
```


COMBINATORIALLY FEASIBLE STRUCTURES OF EXAMPLE PNS 1 GENERATED BY ALGORITHM SSG



















EXAMPLE PNS 1

Operating units given



- Available raw materials: E, G, J, K, L
- Product: A



Depth of recursion: 0 **{1}***, {2}, {1, 2} \Rightarrow procedure SSG(p, m, δ [m]) p={A}, m= \emptyset begin if p = \emptyset then begin write $\delta[m]$; p={A} return end let $x \in p$; $p = \{A\}, x = A$; C:= $(\Delta(\mathbf{x})) \setminus \{\emptyset\}; \Delta(\mathbf{A}) = \{1, 2\}$ for all $c \in C$ do $C = \{ \{1\}, \{2\}, \{1, 2\} \}, c = \{1\}$ begin if $\forall y \in m$, $c \cap \delta(y) = \emptyset$ & $(\Delta(x) \setminus c) \cap \delta(y) = \emptyset$ true m= \emptyset , c={1}, Δ (A)={1, 2} then begin $\delta[m \cup \{x\}] := \delta[m] \cup \{(x, c)\}; m = \emptyset, x = A, c = \{1\}$ SSG(p \cup matⁱⁿ (c))\(R \cup m \cup {x}), m \cup {x}, δ [m \cup {x}]) $\delta[\emptyset] = \emptyset$ \leftarrow $p={A}, mat^{in} ({1}) = {C}, R={E, J, G, K, L}$ m=∅, x=A end end return end 113











{1}*, {2}, {1, 2} \Rightarrow procedure SSG(p, m, $\delta[m]$) p= \emptyset , m={A, C, F} **{3}***, {4}, {3, 4} begin **{1}***, {6}, {1, 6} if $p = \emptyset$ then begin write $\delta[m]$; $p = \emptyset$ \leftarrow end return let $x \in p$; C:= $\wp(\Delta(\mathbf{x})) \setminus \{\emptyset\};$ for all $c \in C$ do begin if $\forall y \in m$, $c \cap \delta(y) = \emptyset$ & $(\Delta(x) \setminus c) \cap \delta(y) = \emptyset$ then begin $\delta[\mathsf{m} \cup \{\mathsf{x}\}] \coloneqq \delta[\mathsf{m}] \cup \{(\mathsf{x}, \mathsf{c})\};$ SSG(p \cup matⁱⁿ (c))\(R \cup m \cup {x}), m \cup {x}, δ [m \cup {x}]) end end return end



Depth of recursion: 3







```
{1}*, {2}, {1, 2}
procedure SSG( p, m, \delta[m] ) p={F}, m={A, C}
                                                                                                {3}*, {4}, {3, 4}
begin
                                                                                                {1}, {6}*, {1, 6}
if p = \emptyset then begin write \delta[m]; p = \{F\}
               return
                              end
let x∈p; p={F}, x=F;
C:= \wp(\Delta(\mathbf{x})) \setminus \{\varnothing\}; \Delta(\mathsf{F}) = \{1, 6\}
for all c \in C do C = \{ \{1\}, \{6\}, \{1, 6\} \}, c = \{6\} \}
               begin
               if \forall y \in m, c \cap \delta(y) = \emptyset & (\Delta(x) \setminus c) \cap \delta(y) = \emptyset false
               m={A, C}, c={6}, \Delta(F)={1, 6}
                then
                  begin
                  \delta[m \cup \{x\}] := \delta[m] \cup \{(x, c)\};
                  SSG(p\cupmat<sup>in</sup> (c))\(R\cupm\cup{x}), m\cup{x}, \delta[m\cup{x}])
                  end
               end
return
end
```

 \Rightarrow







{1}*, {2}, {1, 2}
{3}*, {4}, {3, 4}
{1}, {6}, {1, 6}*







procedure SSG(p, m, δ [m]) p={F}, m={A, C} begin if p = \emptyset then begin write $\delta[m]$; p={F} return end let $x \in p$; $p = \{F\}, x = F$; C:= $\wp(\Delta(\mathbf{x})) \setminus \{\varnothing\}; \Delta(\mathsf{F}) = \{1, 6\}$ for all $c \in C$ do $C = \{ \{1\}, \{6\}, \{1, 6\} \}, c = \{1, 6\} \}$ begin if $\forall y \in m$, $c \cap \delta(y) = \emptyset$ & $(\Delta(x) \setminus c) \cap \delta(y) = \emptyset$ true m={A, C}, c={1, 6}, Δ (F)={1, 6} then begin $\delta[m \cup \{x\}] := \delta[m] \cup \{(x, c)\}; m = \{A, C\}, x = F, c = \{1, 6\}$ SSG(p \cup matⁱⁿ (c))\(R \cup m \cup {x}), m \cup {x}, δ [m \cup {x}]) $p={F}, mat^{in} ({1, 6}) = {C, J}, R={E, J, G, K, L}$ m={A, C}, x=F end end return

end

 \leftarrow











procedure SSG(p, m,
$$\delta[m]$$
) p={F}, m={A, C}
begin
if p = \emptyset then begin write $\delta[m]$; p={F}
return end
let x \in p; p={F}, x=F;
C:= $\wp(\Delta(x))\setminus\{\emptyset\}$; $\Delta(F)=\{1, 6\}$
for all c \in C do C={ {1}, {6}, {1, 6} }
begin
if $\forall y \in m, c \cap \delta(y) = \emptyset & (\Delta(x)\setminus c) \cap \delta(y) = \emptyset$
then
begin
 $\delta[m \cup \{x\}] := \delta[m] \cup \{(x, c)\};$
SSG(p \cup matⁱⁿ (c))\(R \cup m \cup {x}), m \cup {x}, $\delta[m \cup$ {x}])
end
 \Rightarrow end
 \leftarrow return



{1}*, {2}, {1, 2}
{3}, {4}*, {3, 4}



 \leftarrow









Depth of recursion: 3 **{1}***, {2}, {1, 2} \Rightarrow procedure SSG(p, m, $\delta[m]$) p= \emptyset , m={A, C, F} {3}, **{4**}*, {3, 4} begin **{1}***, {6}, {1, 6} if $p = \emptyset$ then begin write $\delta[m]$; $p = \emptyset$ \leftarrow end return let $x \in p$; C:= $\wp(\Delta(\mathbf{x})) \setminus \{\emptyset\};$ for all $c \in C$ do begin if $\forall y \in m$, $c \cap \delta(y) = \emptyset$ & $(\Delta(x) \setminus c) \cap \delta(y) = \emptyset$ then begin $\delta[\mathsf{m} \cup \{\mathsf{x}\}] \coloneqq \delta[\mathsf{m}] \cup \{(\mathsf{x}, \mathsf{c})\};$ SSG(p \cup matⁱⁿ (c))\(R \cup m \cup {x}), m \cup {x}, δ [m \cup {x}]) end end return Δ end δ[{A, C, F}]



123

Solution 3



{1}*, {2}, {1, 2}

procedure SSG(p, m, δ [m]) p={F}, m={A, C} {3}, **{4**}*, {3, 4} begin {1}**, {6}***, {1, 6} if $p = \emptyset$ then begin write $\delta[m]$; $p = \{F\}$ return end let $x \in p$; $p = \{F\}, x = F$; C:= $\wp(\Delta(\mathbf{x})) \setminus \{\emptyset\}; \Delta(\mathsf{F}) = \{1, 6\}$ for all $c \in C$ do $C = \{ \{1\}, \{6\}, \{1, 6\} \}, c = \{6\} \}$ begin if $\forall y \in m$, $c \cap \delta(y) = \emptyset$ & $(\Delta(x) \setminus c) \cap \delta(y) = \emptyset$ false m={A, C}, c={6}, Δ (F)={1, 6} then begin $\delta[m \cup \{x\}] := \delta[m] \cup \{(x, c)\};$ SSG(p \cup matⁱⁿ (c))\(R \cup m \cup {x}), m \cup {x}, δ [m \cup {x}]) end \Rightarrow end return end







{1}*, {2}, {1, 2}

procedure SSG(p, m, δ [m]) p={F}, m={A, C} {3}, **{4**}*, {3, 4} begin {1}, {6}, **{1, 6}*** if p = \emptyset then begin write $\delta[m]$; p={F} return end let $x \in p$; $p = \{F\}, x = F$; C:= $\wp(\Delta(\mathbf{x})) \setminus \{\varnothing\}; \Delta(\mathsf{F}) = \{1, 6\}$ for all $c \in C$ do $C = \{ \{1\}, \{6\}, \{1, 6\} \}, c = \{1, 6\} \}$ begin if $\forall y \in m$, $c \cap \delta(y) = \emptyset$ & $(\Delta(x) \setminus c) \cap \delta(y) = \emptyset$ true m={A, C}, c={1, 6}, Δ (F)={1, 6} then begin $\delta[m \cup \{x\}] := \delta[m] \cup \{(x, c)\}; m = \{A, C\}, x = F, c = \{1, 6\}$ SSG(p \cup matⁱⁿ (c))\(R \cup m \cup {x}), m \cup {x}, δ [m \cup {x}]) $p={F}, mat^{in} ({1, 6}) = {C, J}, R={E, J, G, K, L}$ m={A, C}, x=F end end return

 \leftarrow



















{1}*, {2}, {1, 2}
{3}, {4}, {3, 4}*



 \leftarrow











Solution 5





{1}*, {2}, {1, 2}

procedure SSG(p, m, δ [m]) p={F}, m={A, C} {3}, {4}, **{3, 4}*** begin {1}**, {6}***, {1, 6} if $p = \emptyset$ then begin write $\delta[m]$; $p = \{F\}$ return end let x∈p; p={F}, x=F; C:= $\wp(\Delta(\mathbf{x})) \setminus \{\varnothing\}; \Delta(\mathsf{F}) = \{1, 6\}$ for all $c \in C$ do $C = \{ \{1\}, \{6\}, \{1, 6\} \}, c = \{6\} \}$ begin if $\forall y \in m$, $c \cap \delta(y) = \emptyset$ & $(\Delta(x) \setminus c) \cap \delta(y) = \emptyset$ false m={A, C}, c={6}, Δ (F)={1, 6} then begin $\delta[m \cup \{x\}] := \delta[m] \cup \{(x, c)\};$ SSG(p \cup matⁱⁿ (c))\(R \cup m \cup {x}), m \cup {x}, δ [m \cup {x}]) end \Rightarrow end return



δ[{A, C}]





{1}*, {2}, {1, 2}



 \leftarrow













← return end







{1}*, {2}, {1, 2}
{3}, {4}, {3, 4}*



procedure SSG(p, m, δ [m]) p={C}, m={A}







{1}, **{2}***, {1, 2}

```
procedure SSG( p, m, \delta[m] ) p={A}, m=\emptyset
     begin
     if p = \emptyset then begin write \delta[m]; p = \{A\}
                     return
                                    end
     let x \in p; p = \{A\}, x = A;
     C:= (\Delta(\mathbf{x})) \setminus \{\emptyset\}; \Delta(\mathbf{A}) = \{1, 2\}
     for all c \in C do C = \{ \{1\}, \{2\}, \{1, 2\} \}, c = \{2\}
                    begin
                     if \forall y \in m, c \cap \delta(y) = \emptyset & (\Delta(x) \setminus c) \cap \delta(y) = \emptyset true
                     m=\emptyset, c={2}, \Delta(A)={1, 2}
                      then
                        begin
                        \delta[m \cup \{x\}] := \delta[m] \cup \{(x, c)\}; m = \emptyset, x = A, c = \{2\}
                                                                                                                             \delta[\emptyset] = \emptyset
                        SSG(p\cupmat<sup>in</sup> (c))\(R\cupm\cup{x}), m\cup{x}, \delta[m\cup{x}])
\leftarrow
                        p={A}, mat^{in} ({2}) ={D}, R={E, J, G, K, L}
                        m=∅, x=A
                        end
                     end
     return
     end
                                                                                                                                          136
```



RECURSIVE STEPS OF ALGORITHM SSG

| Number | Depth of | Parameter | Parameter | Parameter | Remark |
|---------|-----------|-----------|-----------|-------------------------------|--------------|
| of call | recursion | р | m | δ[m] | |
| 1 | 0 | {A} | Ø | Ø | Initial call |
| 2 | 1 | {C} | {A} | {(A,{1})} | |
| 3 | 2 | {F} | {A,C} | {(A,{1}),(C,{3})} | |
| 4 | 3 | Ø | {A,C,F} | {(A,{1}),(C,{3}),(F,{1})} | Solution #1 |
| 5 | 3 | Ø | {A,C,F} | {(A,{1}),(C,{3}),(F,{1,6})} | Solution #2 |
| 6 | 2 | {F} | {A,C} | {(A,{1}),(C,{4})} | |
| 7 | 3 | Ø | {A,C,F} | {(A,{1}),(C,{4}),(F,{1})} | Solution #3 |
| 8 | 3 | Ø | {A,C,F} | {(A,{1}),(C,{4}),(F,{1,6})} | Solution #4 |
| 9 | 2 | {F} | {A,C} | {(A,{1}),(C,{3,4})} | |
| 10 | 3 | Ø | {A,C,F} | {(A,{1}),(C,{3,4}),(F,{1})} | Solution #5 |
| 11 | 3 | Ø | {A,C,F} | {(A,{1}),(C,{3,4}),(F,{1,6})} | Solution #6 |
| 12 | 1 | {D} | {A} | {(A,{2})} | |
| 13 | 2 | {F} | {A,D} | {(A,{2}),(D,{4})} | |
| 14 | 3 | Ø | {A,D,F} | {(A,{2}),(D,{4}),(F,{6})} | Solution #7 |





RECURSIVE STEPS OF ALGORITHM SSG (Cont'd)

| Number | Depth of | Parameter | Parameter | Parameter | Remark |
|---------|-----------|-----------|------------|---|--------------|
| of call | recursion | р | m | δ[m] | |
| | | | | | |
| 15 | 2 | {H} | {A,D} | {(A,{2}),(D,{5})} | |
| 16 | 3 | Ø | {A,D,H} | {(A,{2}),(D,{5}),(H,{7})} | Solution #8 |
| 17 | 2 | {F,H} | {A,D} | {(A,{2}),(D,{4,5})} | |
| 18 | 3 | {H} | {A,D,F} | {(A,{2}),(D,{4,5}),(F,{6})} | |
| 19 | 4 | Ø | {A,D,F,H} | {(A,{2}),(D,{4,5}),(F,{6}),(H,{7})} | Solution #9 |
| 20 | 1 | {C,D} | {A} | {(A,{1,2})} | |
| 21 | 2 | {D,F} | {A,C} | {(A,{1,2}),(C,{3})} | |
| 22 | 3 | {F,H} | {A,C,D} | {(A,{1,2}),(C,{3}),(D,{5})} | |
| 23 | 4 | {H} | {A,C,D,F} | {(A,{1,2}),(C,{3}),(D,{5}),(F,{1})} | |
| 24 | 5 | Ø | {A,C,D,F,H | } {(A,{1,2}),(C,{3}),(D,{5}),(F,{1}),(H,{7}) | Solution #10 |
| 25 | 4 | {H} | {A,C,D,F} | {(A,{1,2}),(C,{3}),(D,{5}),(F,{1,6})} | |
| 26 | 5 | Ø | {A,C,D,F,H | } {(A,{1,2}),(C,{3}),(D,{5}),(F,{1,6}),(H,{7})} | Solution #11 |
| 27 | 2 | {D,F} | {A,C} | {(A,{1,2}),(C,{4})} | |
| 28 | 3 | {F} | {A,C,D} | {(A,{1,2}),(C,{4}),(D,{4})} | |
| 29 | 4 | Ø | {A,C,D,F} | {(A,{1,2}),(C,{4}),(D,{4}),(F,{1})} | Solution #12 |
| 30 | 4 | Ø | {A,C,D,F} | {(A,{1,2}),(C,{4}),(D,{4}),(F,{1,6})} | Solution #13 |
| 31 | 3 | {F,H} | {A,C,D} | {(A,{1,2}),(C,{4}),(D,{4,5})} | |





RECURSIVE STEPS OF ALGORITHM SSG (Cont'd)

| Number | Depth of | Parameter | Parameter | Parameter | Remark |
|---------|-----------|-----------|---------------|--|----------------|
| of call | recursion | р | m | δ[m] | |
| | | | | | |
| 32 | 4 | {H} | {A,C,D,F} | {(A,{1,2}),(C,{4}),(D,{4,5}),(F,{1})} | |
| 33 | 5 | Ø | {A,C,D,F,H} { | {(A,{1,2}),(C,{4}),(D,{4,5}),(F,{1}),(H,{7})} | Solution #14 |
| 34 | 4 | {H} | {A,C,D,F} | {(A,{1,2}),(C,{4}),(D,{4,5}),(F,{1,6})} | |
| 35 | 5 | Ø | {A,C,D,F,H} { | {(A,{1,2}),(C,{4}),(D,{4,5}),(F,{1,6}),(H,{7})} | Solution #15 |
| 36 | 2 | {D,F} | {A,C} | {(A,{1,2}),(C,{3,4})} | |
| 37 | 3 | {F} | {A,C,D} | {(A,{1,2}),(C,{3,4}),(D,{4})} | |
| 38 | 4 | Ø | {A,C,D,F} | {(A,{1,2}),(C,{3,4}),(D,{4}),(F,{1})} | Solution #16 |
| 39 | 4 | Ø | {A,C,D,F} | {(A,{1,2}),(C,{3,4}),(D,{4}),(F,{1,6})} | Solution #17 |
| 40 | 3 | {F,H} | {A,C,D} | {(A,{1,2}),(C,{3,4}),(D,{4,5})} | |
| 41 | 4 | {H} | {A,C,D,F} | {(A,{1,2}),(C,{3,4}),(D,{4,5}),(F,{1})} | |
| 42 | 5 | Ø | {A,C,D,F,H} | } {(A,{1,2}),(C,{3,4}),(D,{4,5}),(F,{1}),(H,{7}))} | Solution #18 |
| 43 | 4 | {H} | {A,C,D,F} | {(A,{1,2}),(C,{3,4}),(D,{4,5}),(F,{1,6})} | |
| 44 | 5 | Ø | {A,C,D,F,H} | } {(A,{1,2}),(C,{3,4}),(D,{4,5}),(F,{1,6}),(H,{7}) | } Solution #19 |





ALGORITHMIC SYNTHESIS BY EXHAUSTIVE SEARCH





ALGORITHMIC SYNTHESIS BY EXHAUSTIVE SEARCH







SELECTION OF THE OPTIMAL NETWORK(S)

- The combinatorial algorithms, MSG, SSG, are independent of the type of mathematical model of the operating units.
- The exhaustive search will be illustrated by two types of models.
- Case I.

 Linear cost functions and models of the operating units (MILP).

Solution procedure: sequence of LP-s.

Note: Algorithm SSG transforms the MILP problem into a sequence of LP-s.





Case II.

- Nonlinear cost functions and linear models of the operating units (MINLP).
- Solution procedure: sequence of SSG-NLP where the cost function of the NLP is separable concave.

Note: this class of NLP problems can be solved effectively, see, e.g., Falk and Soland, 1969





OBSERVATION

- The combinatorial axioms may drastically reduce the search space so that synthesis problems can be solved by exhaustive search (Algorithm SSG).
- The combinatorial part of the synthesis problem may effectively control the synthesis procedure if the search space can be reduced algorithmically.
- For very complex problems, this reduction may not be enough; further acceleration may be necessary.
- Possible way: branch-and-bound exploiting the reduced search space given by the axioms.




ACCELERATED BRANCH & BOUND ALGORITHM FOR SOLVING PNS PROBLEMS





ON THE BRANCH-AND-BOUND ALGORITHM

- Branch-and-bound search is a possible way for solving the MILP or MINLP problems.
- Branch-and-bound generates the optimal solution by solving a system of simplified LP or NLP partial problems by successively partitioning the solution set.
- Suppose that a binary variable expresses the existence or absence of an operating unit (the value is 1 for the former and 0 for the latter).





THE BASIC BRANCH-AND-BOUND SEARCH ILLUSTRATED ON AN ENUMERATION TREE



Notation:

- 1 existence or inclusion of the corresponding operating unit
- 0 absence or exclusion of the corresponding operating unit





Note: Each node of the tree represents one 1/2 (or NLP) problem.

SCIENTIARUM CHICANA CH



Note: In the worst case, 157 partial problems are examined to determine the optimal solution which is always among the 19 combinatorially feasible structures.





EXAMPLE PNS 2

(Industrial synthesis problem with 35 operating units)

Number of partial problems generated by the basic branchand-bound algorithm:

130 million

Number of combinatorially feasible structures:

3465

Note: The large ratio shows high inefficiency.





GENERAL PROPERTIES OF THE BRANCH-AND-BOUND FRAMEWORK IN SOLVING PNS

The basic branch-and-bound algorithm is inefficient in solving a process synthesis problem because:

- □ it leads to a large number of partial problems,
- each partial problem has an unnecessarily, large number of free variables.





ACCELERATED BRANCH AND BOUND ALGORITHM

The accelerated branch-and-bound algorithm

- reduce the size of an individual subproblem through exclusion of those operating units that should not be included in any feasible solution of the subproblem
- speeds up the generation of the optimal solution by minimizing the number of subproblems to be solved





ILLUSTRATIVE EXAMPLE FOR BRANCHING BY ABB

Maximal structure

Product: A

Raw materials: C, F, G, H, I







PARTIAL PROBLEMS GENERATED ON THE BASIS OF THE PRODUCTION OF A



Relation between the operating units and a partial problem

- (based on decisions) included in each structure
- Included in each structure
- (based on maximal neutral extension)
- excluded from each structure

included in at least one structure



ENUMERATION TREE FOR THE ACCELERATED BRANCH-AND-BOUND (WORST CASE)







ILLUSTRATIVE EXAMPLE FOR BRANCHING BY ABB







ENUMERATION TREE (WORST CASE)





157



Relation between the operating units and a partial problem.

included in each structure
(based on decisions)
included in each structure
(based on maximal neutral extension)
excluded from each structure

included in at least one structure











Si: solution Number: partial problem Capital letter: decision point on the maximal structure









Partial problem #2





Enumeration₁ (search) tree (worst case)

Α



Si: solution Number: partial problem Capital letter: decision point on the maximal structure









Partial problem #3





Enumeration₁ (search) tree (worst case)

Α



Si: solution Number: partial problem Capital letter: decision point on the maximal structure









Partial problem #4 (S1)





Enumeration₁ (search) tree (worst case)

A



Si: solution Number: partial problem Capital letter: decision point on the maximal structure









Partial problem #5 (S2)





Enumeration₁ (search) tree (worst case)

Α



Si: solution Number: partial problem Capital letter: decision point on the maximal structure









Partial problem #6





Enumeration₁ (search) tree (worst case)

Α



Si: solution Number: partial problem Capital letter: decision point on the maximal structure









Partial problem #7 (S3)





Enumeration₁ (search) tree (worst case)

Α



Si: solution Number: partial problem Capital letter: decision point on the maximal structure









Partial problem #8 (S4)





Enumeration₁ (search) tree (worst case)

Α



Number: partial problem Capital letter: decision point on the maximal structure









Partial problem #9





Enumeration (search) tree (worst case)











Partial problem #10 (S5)





Enumeration (search) tree (worst case)

A











Partial problem #11 (S6)





Number: partial problem Capital letter: decision point on the maximal structure












Enumeration (search) tree (worst case)



Si: solution Number: partial problem Capital letter: decision point on the maximal structure









Partial problem #13 (S7)





Enumeration (search) tree (worst case)



Number: partial problem Capital letter: decision point on the maximal structure









Partial problem #14 (S8)





maximal structure









Partial problem #15 (S9)





























maximal structure









Partial problem #18 (S10)





maximal structure









Partial problem #19 (S11)





maximal structure













maximal structure



















Partial problem #22 (S12)













Partial problem #23 (S13)























Partial problem #25 (S14)











Partial problem #26 (S15)































Partial problem #29 (S16)






Partial problem #28





Partial problem #30 (S17)







Partial problem #27





Partial problem #31







L

7

Η

5

Partial problem #31



Partial problem #32 (S18)

В

А

Κ

G

D

2







L

7

Η

5

Partial problem #31



Partial problem #33 (S19)





EXAMPLE PNS 2 (Industrial synthesis problem with 35 operating units)







Computational effort required by the basic and accelerated branch-and-bound algorithms in the worst case for Example PNS 2.

Number of partial problems:

- Branch-and-bound algorithm: 130 million
- Accelerated branch-and-bound algorithm: 8008



PROCESS NETWORK SYNTHESIS







SOLUTION OF AN INDRUSTRIAL RETROFIT SYNTHESIS PROBLEM BY THE ACCELERATED BRANCH-AND-BOUND ALGORITHM: OPTIMAL WATER RECYCLING SYSTEM FOR A NITROCELLULOSE PROCESS





PROBLEM SPECIFICATION

- Streams of water with different quality and quantity are generated in various places of the process.
- The temperatures of these streams are diverse.
- The distances between any pair of operating units vary; this affects the cost of piping.
- The process is semicontinuous; therefore, a buffer has to be installed at an operating unit if water is recycled.





PROBLEM SPECIFICATION (Cont'd)

- An operating unit may accept only a given subset of the available streams of water with different quality.
- Industrial water can be used at any operating unit.
- Steam is used to heat recycled water if necessary.
- Retrofitting.
- The objective function includes the cost of industrial water and energy (steam), operating cost, and the investment cost of retrofitting (e.g., new piping).





Original nitrocellulose process

Notation









General features of the existing nitrocellulose process

- Semicontinuous
- Operating units:

mixing (tank) reaction (reactor) separation (centrifuge) washing (autoclave) steaming (tank) high pressure steaming (autoclave) washing (tank) forming (autoclave)

Water consumption: 166.5 m³/t





Possible improvements

additional water recycling modified process structure



STEP 1. Maximal Structure Generation.

Maximal structure

Notation

 $\mathbf{\nabla}$

- operating unit
- material or steam
- raw material
- product





STEP 2.

Generation of the optimal or n-best solutions by the accelerated branch-and-bound algorithm.

Optimal structure

Notation

- operating unit
- material or steam
- raw material
- product
- selected for optimal
- ignored for optimal







COMPARISON OF DIFFERENT SOLUTIONS

| | Energy cost saving | Water cost saving | Investment cost | Total cost |
|-------------|--------------------------|----------------------|--------------------|------------|
| Optimal | 2592 | 1440 | 1130 | . 6488 |
| Second best | 2592 | 1566 | 1260 | 6492 |
| Third best | 2592 | 1420 | 1130 | 6508 |
| Fourth best | 2592 | 1546 | 1260 | 6512 |
| Fifth best | 2592 | 1440 | 1195 | 6553 |
| Recent | | | | 9390 |





INTEGRATED SYNTHESIS OF PROCESS AND HEAT EXCHANGER NETWORKS





INTRODUCTION

- Process synthesis process integration
 - The purpose of process integration is to combine available or planned systems for better performance, e.g., for energy conservation, or pollution reduction, or cost reduction.
 - Process integration usually affects the networks or structures of the systems.
 - For process integration, a convenient process synthesis method is required.





Sources of difficulties

- The combination of already complex problems, i.e., the integration of complex design (synthesis) subproblems.
- Process integration frequently involves at least two classes of synthesis problems.
- The available synthesis methods focus on certain classes of problems, e.g., the synthesis of
 - separation networks.
 - heat exchanger networks.
 - reactor networks.





WHY AVAILABLE SYNTHESIS METHODS CANNOT BE COMBINED TO PERFORM INTEGRATED PROCESS SYNTHESIS

Illustration:

Design of processing systems with heat integration

- The processing system is to be designed as a PNS problem.
- The heat-exchanger network is to be designed as a HEN synthesis (HENS) problem.
- PNS and HENS must be integrated into a super synthesis (to reach the global optimum).
- The available HENS methods assume that the hot and cold streams are specified a priori; it is unsuitable for PNS.





PROPOSED METHOD FOR THE INTEGRATION OF PNS AND HENS

Outline of the Method

- New structure representation as an extension of Pgraph.
- A highly effective combinatorial method (algorithm ABB) controls the procedure.
- The mathematical model of the HENS problem is integrated into the mathematical model of a partial problem of PNS generated by algorithm ABB.





STRUCTURE REPRESENTATION

Heat streams







Latent heat

Penph

hPgaph







Temperature intervals







Temperature intervals for potential connections







Heat exchangers defined by matching intervals







FORMAL DESCRIPTION

Specific operating cost of heat transfer:

$$c_{ij}(Q_{ij}) = A_{ij} \frac{1}{U_{ij}LMTD_{ij}}Q_{ij}$$

where

- Q_{ij} : heat transferred between streams *i* and streams *j*.
- A_{ij} : unit cost of heat exchanger area between streams *i* and *j*.
- U_{ij} : heat transfer coefficient between streams *i* and streams *j*.



$$\begin{aligned} & \text{Mathematical model for process synthesis} \\ & \text{including heat integration} \\ & \min \Biggl[\sum_{o_j \in O} f_j(y_j, x_j) + \sum_{\substack{i \in Hot, j \in Cold \\ I(i) > I(j)}} c_{ij}(Q_{ij}) + \sum_{i \in Hot j \in Cold \ Util} \sum_{Util} CU_j Q_{ij} + \sum_{j \in Cold \ i \in Hot \ Util} \sum_{Util} HU_i Q_{ij} \Biggr] \end{aligned}$$

Constraints on the structure

$$g_k(y_k, o_k, z_k) \le 0, \qquad o_k \in O$$
$$g'_i(m_i) \le 0, \qquad m_i \in M$$

Constraints on the heat balance

 $QB(i) = 0, \quad i \in Hot \cup Cold$





where

- O: set of operating units
- y_k : vector of binary variables for expressing existence (1) or absence (0) of the operating units k
- z_i : size of operating unit o_i
- CU_{i} : the unit-cost of the *j*-th cold utility
- HU_i: the unit-cost of the *i*-th hot utility





EXAMPLE

PNS Part of the Problem Definition

Product

| Name | Req. flow [t/year] | |
|------------|--------------------|--|
| <i>M</i> 1 | 100.0 | |

□ Raw materials

| Name Price[USD/t] | Max. flow [t/year] |
|-------------------|--------------------|
|-------------------|--------------------|

| M5 | 140 | Unlimited |
|-------------|-----|-----------|
| M7 | 900 | Unlimited |
| M9 | 650 | Unlimited |
| <i>M</i> 10 | 500 | Unlimited |
| <i>M</i> 11 | 700 | Unlimited |





Operating units

The linear mathematical models of the operating units: the ratio of the flow rates of the input and output streams of an operating unit is fixed (the relative flow rate is in brackets in the following table).

| # | Input streams | Output streams |
|---|--------------------|----------------|
| 1 | M3(3) | M1(2), M6(1) |
| 2 | M4(1.5) | M1(1), M2(0.5) |
| 3 | M5(1), M6(1) | M3(2) |
| 4 | M6(0.3), M7(1.7) | M3(1), M4(1) |
| 5 | M7(2), M8(1) | M4(3) |
| 6 | M9(1) | M6(1) |
| 7 | M10(1.2), M11(0.8) | M8(2) |
| | | |





Cost Parameters of the Operating Units (MILP Model)

The cost function of an operating unit:

$$C_i = A_i + B_i X_i$$

where Xi is the relative "size" of operating unit *i*.

| Unit | Investment Cost | Operating Cost |
|------|-----------------|----------------|
| 1 | 7,500 | 20 |
| 2 | 6,000 | 200 |
| 3 | 10,000 | 10 |
| 4 | 15,000 | 10 |
| 5 | 10,000 | 120 |
| 6 | 3,000 | 20 |
| 7 | 5,000 | 160 |





HENS part of the Problem Definition

Operating units

| # | Later | nt Heat | Input streams | Output streams | |
|---|----------------|---------|--------------------|-----------------|--|
| | ⁰ C | Param. | | | |
| 1 | - | - | M3(3,70) | M1(2), M6(1,90) | |
| 2 | - | - | M4(1.5) | M1(1), M2(0.5) | |
| 3 | 80 | 20 | M5(1), M6(1,80) | M3(2,60) | |
| 4 | - | - | M6(0.3), M7(1.7) | M3(1,90), M4(1) | |
| 5 | - | - | M7(2), M8(1) | M4(3) | |
| 6 | - | - | M9(1) | M6(1,55) | |
| 7 | - | - | M10(1.2), M11(0.8) | M8(2) | |

Note: The second number in the brackets specifies the temperature of the corresponding stream (if available).




Cost parameters

Cost of heat-exchanger area: 5.0

Cost of utility

| Utility | Туре | Temp.(⁰ C) | Cost |
|---------|------|-------------------------|------|
| 1 | Hot | 10.0 | 20.0 |
| 2 | Cold | 100.0 | 30.0 |





Integrated maximal structure











Heat transfer on the optimal structure







ALGORITHMIC SYNTHESIS OF AZEOTROPIC-DISTILLATION SYSTEMS





AZEOTROPIC-DISTILLATION PROBLEM



- Defined by
 - □ Feed (F)
 - Product (E)
 - Distillation boundaries
 - Phase-splitting regions

Azeotropic-distillation problem represented by RCM





IDENTIFYING OPERATING UNITS







COMBINATORIAL ALGORITHMS



Solution-structure #140





REACTION PATHWAY IDENTIFICATION





REACTION PATHWAY IDENTIFICATION PROBLEM

- Given by the stoichiometric equations of:
 - Overall reaction
 - □Set of elementary reactions
- Example Overall reaction: C₄H₁₀ C₄H₈ + H₂ Set of elementary reactions: (1) C₄H₁₀ + $\ell \rightleftharpoons C_4H_8\ell + H_2$ (2) C₄H₈ $\ell \rightleftharpoons C_4H_8 + \ell$ (3) C₄H₈ $\ell \rightleftharpoons C_4H_6\ell + H_2$





P-GRAPH REPRESENTATION OF REACTION PATHWAYS





SCHEDULING OF MULTIPURPOSE BATCH PLANTS





BUILDING BLOCKS OF THE NEW FRAMEWORK

- New representation technique (S-graph)
- Elementary combinatorial algorithms





REPRESENTATION TECHNIQUE

- Conventional graph representation is convenient for unlimited intermediate storage policy (job-shop).
- It does not represent "non-intermediate storage" policy appropriately.





NEW REPRESENTATION: S-GRAPH

Unified representation for the

recipe

intermediate phase of the scheduling procedure

final schedule

(See Sanmarti et al., 1998 for details)





Initial step (recipe)







Step 1.







Step 2.







Final schedule







GENERAL FEATURES OF THE FRAMEWORK

- It serves as base for specific scheduling algorithms
- It takes into account:
 - complex recipe
 - limited waiting time
 - transfer time
 - due date
 - concurrent equipments
- Can be integrated with process synthesis





EXAMPLE SCH 1

| | | Product | # of batches |
|----------------------------------|----|---------|--------------|
| Number of Equipments Mixer: 4 | | P1 | 2 |
| Nixor: 1 | | P2 | 3 |
| MIXEI. | 4 | P3 | 5 |
| Tank: | 11 | P4 | 2 |
| Packing line: | 4 | P5 | 5 |
| 9 | - | P6 | 4 |
| | | P7 | 5 |
| | | P8 | 5 |
| | | P9 | 1 |
| | | P10 | 1 |
| | | Total | 43 |



Note: Input is in an Excel file



EXTREMELY COMPLEX SCHEDULING PROBLEMS

 Practical scheduling problems can be difficult to solve because of

□ their size,

involvement of continuous and batch operations.

The new framework serves as a base in the development of effective algorithms for extreme problems.





DEVELOPMENT PROCESS OF A SCHEDULING ALGORITHM







EXAMPLE SCH 2 COMPLEX INDUSTRIAL SCHEDULING PROBLEM

Number of products: 123

Number of Equipments

- Mixer: 5
- Tank: 40
- Packing line: 26

Total number of batches: 334

Note: Running time on PC (333 MHz) is less than 15 minutes.





CONCLUDING REMARK

Combinatorial framework may effectively control the solution procedure of complex process design and operations problems





Literature

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Synthesis of optimal processes



Introduction

- Algorithm to generate maximal structure (MSG, Maximal Structure Generation)
- Algorithm to generate all combinatorial feasible solutions (SSG, Solution Structure Generation)
- Generate the optimal solution (ABB, Accelerated Branch and Bound)





Notations

• Let $\psi^-(o)$ denotes the set of all input materials of operating units included set o

$$\psi^{-}(o) = \bigcup_{(\alpha,\beta)\in O} \alpha$$

• Let $\psi^+(o)$ denotes the set of all output materials of operating units included set o

$$\psi^+(0) = \bigcup_{(\alpha,\beta)\in \mathbf{0}} \beta$$

Let $\psi(o)$ denotes the set of all input and output materials of operating units included set o

$$\psi(o) = \psi^-(o) \cup \psi^+(o)$$





Notations

- Let φ⁻(m) denotes the set of operating units producing any material included set m
 φ⁻(m) = {(α, β) ∈ o : β ∩ m ≠ Ø}
- Let $\varphi^+(m)$ denotes the set of operating units consuming any material included set m

$$\varphi^+(\mathbf{m}) = \{(\alpha, \beta) \in \mathbf{o} : \alpha \cap \mathbf{m} \neq \emptyset\}$$

Let $\varphi(m)$ denotes the set of operating units producing or consuming any material included set m

$$\varphi(\mathbf{m}) = \varphi^{-}(\mathbf{m}) \cup \varphi^{+}(\mathbf{m})$$





Notations

- The above functions are valid in case of single material or operating unit
 - □ For example $\psi^-(o_i)$ denotes the set of input materials of operating unit o_i , i.e., $\psi^-(o_i) = \psi^-(\{o_i\})$





MSG algorithm





Solution structures

- A P-graph can represent the structure of a production system, but an arbitrary S-graph cannot represent the behavior of the system
- To represent a valid (P, R, O) synthesis problem, the (m, o) P-graph has to fulfill five combinatorial properties



MP I.I.I.

Axioms

(S1) Every final product is represented in the graph

 $\mathcal{P} \subseteq \mathbf{m}$

 (S2) A material type vertex has no input if and only if it represents a raw material

 $\mathbf{m} \setminus \psi^-(\mathbf{o}) = \mathbf{m} \cap \mathcal{R}$

 (S3) Every operating unit type represents an operating unit defined in the synthesis problem

$o \in \mathcal{O}$

 (S4) Every operating unit type vertex has at least one path leading to a vertex representing a final product

 $\forall o_i \in 0, \exists path[o_i, m_i], where m_i \in \mathcal{P}$

 (S5) If a material type vertex belongs to the graph, it must be an input or an output of at least one operating unit type vertex in the graph

 $\mathbf{m} \subseteq \psi(\mathbf{0})$





Solution-structure

- The structures satisfy the five axioms called combinatorially feasible solution-structures or solution-structures
- Nothing other structure is solution-structure





Set of solution-structures

- Let $S(\mathcal{P}, \mathcal{R}, \mathcal{O})$ the set of solution-structures
- The set of solution-structures are closed under union
 - The union of two solution-structures is a solutionstructure

$$\begin{split} \sigma_1 \in S(\mathcal{P}, \mathcal{R}, \mathcal{O}) \& \sigma_2 \in S(\mathcal{P}, \mathcal{R}, \mathcal{O}) \to \\ \sigma_1 \cup \sigma_2 \in S(\mathcal{P}, \mathcal{R}, \mathcal{O}) \end{split}$$




Maximal structure

• Let $\mu(\mathcal{P}, \mathcal{R}, \mathcal{O})$ the union of all solution-structure

$$\mu(\mathcal{P}, \mathcal{R}, \mathcal{O}) = \bigcup_{\sigma \in S(\mathcal{P}, \mathcal{R}, \mathcal{O})} \sigma$$

- If the set of $S(\mathcal{P}, \mathcal{R}, \mathcal{O})$ is not empty, the $\mu(\mathcal{P}, \mathcal{R}, \mathcal{O})$ is called the maximal structure of the synthesis problem
- The maximal structure is a solution-structure
- Each solution-structure is a substructure of the maximal structure





MSG algorithm

The MSG (Maximal Structure Generation) algorithm generates the maximal structure of a synthesis problem in polynomial time





Initialize the input of MSG

- Define the following sets
 - $\square \mathcal{M} \text{the set of materials}$
 - $\square \mathcal{P}$ the set of final products
 - $\square \mathcal{R}$ the set of raw materials
 - $\square \mathcal{O}$ the set of plausible operating units
- The connection of the operating units through the materials defines the initial network
 - The axiom (S3) satisfies





The main steps of MSG

- The MSG algorithm consists of two main parts
 - Reduction
 - Remove materials and operating units violates axioms (S2) or (S5)
 - Composition
 - Collect the operating units which can take part of the production of a final product





Reduction part

$$\mathcal{O} := \mathcal{O} \setminus \varphi^{-}(\mathcal{R});$$

$$\mathcal{M} := \psi(\mathcal{O});$$

$$\mathbf{r} := \psi^{-}(\mathcal{O}) \setminus (\psi^{+}(\mathcal{O}) \cup \mathcal{R});$$

while $\mathbf{r} \neq \emptyset$ do
let $x \in \mathbf{r};$

$$\mathcal{M} := \mathcal{M} \setminus \{x\};$$

 $\mathbf{o} := \varphi^{+}(\{x\});$
 $\mathcal{O} := \mathcal{O} \setminus \mathbf{o};$
 $\mathbf{r} := \left(\mathbf{r} \cup (\psi^{+}(\mathbf{o}) \setminus \psi^{+}(\mathcal{O}))\right) \setminus \{x\};$
if $\mathcal{P} \cap \mathcal{M} \neq \mathcal{P}$ then
stop;





Composition part

```
\mathbf{p} \coloneqq \mathcal{P}; \mathbf{m} \coloneqq \emptyset; \mathbf{o} \coloneqq \emptyset;
while p \neq \emptyset do
                 let x \in p;
                 \mathbf{m} \coloneqq \mathbf{m} \cup \{x\};
                 O_x \coloneqq \varphi^-(\{x\});
                 0 \coloneqq 0 \cup 0_{\gamma};
                 \mathbf{p} \coloneqq (\mathbf{p} \cup \psi^{-}(\mathbf{o}_{x})) \setminus (\mathcal{R} \cup \mathbf{m});
\mathbf{m} \coloneqq \psi(\mathbf{0});
```





Example

- Let the synthesis problem is the following
 - $\label{eq:matrix} \square \ \mathcal{M} = \{\mathsf{A}, \, \mathsf{B}, \, \mathsf{C}, \, \mathsf{D}, \, \mathsf{E}, \, \mathsf{F}, \, \mathsf{G}, \, \mathsf{H}, \, \mathsf{I}, \, \mathsf{J}, \, \mathsf{K}, \, \mathsf{L}, \, \mathsf{M}, \, \mathsf{N}, \, \mathsf{Q}, \, \mathsf{T}, \, \mathsf{U}, \\ \mathsf{V}\}$

$$\Box \mathcal{P} = \{\mathsf{B}\}$$

$$\Box \mathcal{R} = \{\mathsf{F}, \mathsf{H}, \mathsf{M}, \mathsf{T}\}$$

 $\begin{array}{l} \bigcirc \mathcal{O} = \{ O1 = (\{C, D, F\}, \{A\}), \ O2 = (\{D\}, \{B, G\}), \\ O3 = (\{E\}, \{B, U\}), \ O4 = (\{F, G\}, \{C, D\}), \\ O5 = (\{G, H\}, \{D\}), \ O6 = (\{H, I\}, \{E\}), \\ O7 = (\{J, K\}, \{E\}), \ O8 = (\{M\}, \{G\}), \ O9 = (\{N, Q\}, \\ \{H\}), \ O10 = (\{T, U\}, \{I\}), \ O11 = (\{V\}, \{J\}) \} \end{array}$





Example (initial network)







- Remove operating units producing raw materials
 - Operating unit O9 produces raw material H







Remove materials not produced but consumed
 Materials L, N and Q







 The elements of r (denoted by red on figures) are violates axioms (S4)







First remove material K

Also remove operating unit O7 which is consuming K







- Remove material V
 - Also remove operating unit O11
 - Put material J into r







- Remove material J
 - Set r is empty
 - Reduction part ends







- All final product is presented in the graph
- Composition part can be started
- Notations in figures
 - p materials have to be examined, i.e., have to be produced (denoted by red color)
 - m examined materials, i.e. the production has been decided (denoted by blue)
 - o operating units already included into the structure (denoted by blue)





- First final product (material B) has to be produced
- Operating unit O2 and O3 can produce B







Material D and E must be produceD can be produced by O4 and O5







- Material E and G must be produce
- E can be produced by O6







- Material G and I must be produce
- G can be produced by O8







- Material I must be produce
- I can be produced by O10







- Material U must be produce
- U can be produced by O3







Set p is empty

Operating unit O1 is not in the graph







The set of material of the P-graph is the input and output materials of the operating units







SSG algorithm





Introduction

- Any solution structure can be optimal with appropriate parameters
- The generation of all solution structure can be useful
 - Analyzing them one by one
 - Solving the problem by exhaustive search
 - Verifying the search space reduction
 - It can provide a good basis for an efficient algorithm





Decision mapping

- Decision mapping is a tool which helps to represents the decisions during optimization and the decisions became consistent
- The decision mapping describes the decision which operating units will be used to produce a set of materials
 - Which operating units will take place in the solutionstructure
- A decision is consistent if it is not inconsistent with the previous decisions





Formal description of decision mapping

- Let $m \subseteq \mathcal{M}$, moreover $\forall x \in m$, $\delta(x) \subseteq \varphi^{-}(x)$ and $\Delta(x) = \varphi^{-}(x)$
- $\Delta[m] = \{(x, \Delta(x)) | x \in m\}$ is a mapping over m
- $\delta[m] = \{(x, \delta(x)) | x \in m\}$ is a decision mapping over m
- The complement of decision mapping δ over m is $\overline{\delta}[m] = \{(x, y) | x \in m, y = \varphi^{-}(x) \setminus \delta(x)\}$





Decision mapping

- The mapping is a set of pairs, where the first element of a pair is a material, the second element of the pair is the set of operating units which can produce the material
- In case of decision mapping the second element of the pair is the set of material which are chosen to produce the material
- In case of complement the second element of the pair is the set of material which are excluded from the structure





Decision mapping

- If there are parenthesis after δ or Δ, it means the parameter is a material and the result is a set of operating units
- If there are brackets after δ or Δ , it means the parameter is a set of materials and the result is a set of pairs (defined above)





Example

Operating units O1 and O2 are included in the structure, O3 is excluded from the structure

$$\Box \Delta(A) = \{O1, O3\}, \delta(A) = \{O1\}$$

$$\Box \Delta(B) = \{O2\}, \ \delta(B) = \{O2\},\$$

$$\Box \Delta(C) = \{O2, O3\}, \delta(C) = \{O2\}$$

$$\Box \Delta (\mathsf{D}) = \Delta (\mathsf{E}) = \Delta (\mathsf{F}) = \emptyset$$

$$\delta(\mathsf{D}) = \delta(\mathsf{E}) = \delta(\mathsf{F}) = \emptyset$$







Example

- Decision mapping can be defined for any set of materials
 - $\Delta [\{A, B, C, D, E, F\}] = \{(A, \Delta(A)), (B, \Delta(B)), (C, \Delta(C)), (D, \Delta(D)), (E, \Delta(E)), (F, \Delta(F))\} = \{(A, \{O1, O3\}), (B, \{O2\}), (C, \{O2, O3\}), (D, \emptyset), (E, \emptyset), (F, \emptyset)\}$







Consistent decision mapping

- Decision mapping $\delta[m]$ is consistent if • $|m| \le 1$ or • $(\delta(w) \circ \delta(w)) + \overline{\delta}(w) \circ \overline{\delta}(w) = \Lambda(w) \circ \Lambda(w)$
 - $\Box \left(\delta(x) \cap \delta(y) \right) \cup \overline{\delta}(x) \cap \overline{\delta}(y) = \Delta(x) \cap \Delta(y) \quad \text{for all} \\ x, y \in \mathbf{m}$





Variables in SSG algorithm

- p materials have to be examined, i.e., have to be produced
- m examined materials, i.e., the production has been decided
- ${}^{\bullet} \delta[m]$ decision mapping representing the previous decisions
- x the material chosen for decision
- C the set of possible decisions about material x
- c the current decision (set of operating units)





Initialization of the SSG algorithm

begin if $\mathcal{P} = \emptyset$ then stop; SSG($\mathcal{P}, \emptyset, \emptyset$); end





SSG algorithm

```
procedure SSG(p, m, δ[p])
begin
```

```
\text{if }p= \emptyset \text{ then }
```

```
print \delta[m];
```

```
return;
```

```
let x \in p;
```

$$\mathbf{C} \coloneqq \wp \big(\Delta(x) \big) \setminus \{ \emptyset \};$$

for all $c \in C$ do

if $\forall y \in m, c \cap \overline{\delta}(y) = \emptyset$ and $\Delta(x) \setminus c \cap \delta(y) = \emptyset$ then SSG($p \cup \psi^{-}(c) \setminus (\mathcal{R} \cup m \cup \{x\}), m \cup \{x\}, \delta[m] \cup \{(x, c)\});$

end





SSG

- The algorithm has same similarity with the composition part of the MSG algorithm
- It starts from the products and make decisions about the productions
- Multiple decisions available → search tree represents the work of the algorithm




Example

Continue the example from the previous section, where maximal structure has been generated







Initialization

Initialization defines the materials have to be produced







First step

3 possible decisions







Search tree

The work of the SSG algorithm





Result

There are 13 solution-structures









ABB algorithm





Introduction

- MSG and SSG take into account only structural informations
- Parameters are also important
- Mathematical model is needed
 - MILP model





Mathematical model

- Aim is to minimize the overall cost
 - Investment cost
 - Operational cost
 - Material cost

Constraints

- Lower bounds on the amounts of products to be manufactured to meet the demand
- Availability of raw materials
- Mass balance





Decision variables

- Two variables for each operating unit
 - □ y_i denotes the existence of operating unit $o_i \in O$ in the solution
 - □ x_i denotes the capacity of operating unit $o_i \in O$ in the solution





Cost of operating units

Investment and operational cost are similar, we do not distinguish them







Cost of operating units

- The cost of operating unit o_i $y_i(fix_i + prop_ix_i)$
- Linearization
 - The cost

$$fix_iy_i + prop_ix_i$$

Additional constraint

 $x_i \leq cap_i y_i$

• Where cap_i is the maximum capacity of o_i





Cost of raw materials

• The overall consumption of raw material m_j

 $\sum_{o_i \in \varphi^+(j)} x_i i r_{ij}$

□ Where ir_{ij} is the consumption rate of m_j by $o_i \in O$

• The cost of raw material r_i

$$price_{j} \sum_{o_{i} \in \varphi^{+}(j)} x_{i} ir_{ij}$$

□ Where $price_j$ is the price of raw material $r_j \in \mathcal{R}$





Objective function

$$\min \sum_{o_i \in \mathcal{O}} (fix_i y_i + prop_i x_i) + \sum_{r_j \in \mathcal{R}} \left(price_j \sum_{o_i \in \varphi^+(j)} x_i ir_{ij} \right)$$





Constraint from linearization of objective function

 $x_i \le cap_i y_i \quad o_i \in \mathcal{O}$





Availability of raw materials

$$\sum_{o_i \in \varphi^+(j)} x_i i r_{ij} \le max_j \quad m_j \in \mathcal{R}$$





- Lower bounds on the amounts of products to be manufactured to meet the demand
- Product can be produced and purchased

$$\sum_{o_i \in \varphi^-(j)} x_i or_{ij} - \sum_{o_i \in \varphi^+(j)} x_i ir_{ij} \ge \min_j \quad m_j \in \mathcal{P}$$

□ Where or_{ij} is the production rate of m_j by $o_i \in O$





Mass balance

$$\sum_{\substack{o_i \in \varphi^-(j) \\ m_j \in \mathcal{M} \setminus (\mathcal{R} \cup \mathcal{P})}} x_i or_{ij} \ge \sum_{\substack{o_i \in \varphi^+(j) \\ \mathcal{R} \cup \mathcal{P}}} x_i ir_{ij}$$





The last three constraints can be merged

$$l_j \leq \sum_{o_i \in \varphi^-(j)} x_i or_{ij} - \sum_{o_i \in \varphi^+(j)} x_i ir_{ij} \leq u_j$$
$$m_j \in \mathcal{M}$$

Where

- $l_j = -max_j$ and $u_j = 0$ if $m_j \in \mathcal{R}$
- $l_j = min_j$ and u_j is an arbitrary big number if $m_j \in \mathcal{P}$
- $l_j = 0$ and u_j represents the remaining amount of material m_j if $m_j \in \mathcal{M} \setminus (\mathcal{R} \cup \mathcal{P})$





Example

- Define the MILP model of following the maximal structure
- The input and output ratios are given as weights of the arcs



Example (parameters)

| Operating unit | сар | fix | prop |
|-------------------|-----|-----|------|
| 01 | 10 | 5 | 5 |
| 02 | 10 | 10 | 10 |
| 03 | 10 | 5 | 5 |

| Materials | min | max | price |
|-----------|-----|-----|-------|
| А | | 10 | 2 |
| В | | 20 | 1.5 |
| E | 5 | | |



Example (model)

 $\min 5y_1 + 8.5x_1 + 10y_2 + 26.5x_2 + 5y_3 + 5x_3$ s.t. $0 < x_1 < 10y_2$

| U | \geq | $\boldsymbol{\lambda}_1$ | | $10y_2$ |
|-----|--------|--------------------------|--------|-----------|
| 0 | \leq | x_2 | \leq | $10y_{2}$ |
| 0 | \leq | x_3 | \leq | $10y_{3}$ |
| -10 | \leq | $-x_1 - 3x_2$ | \leq | ∞ |
| -20 | \leq | $-x_1 - 7x_2$ | \leq | ∞ |
| 0 | \leq | $2x_1 - 10x_3$ | \leq | ∞ |
| 0 | \leq | $3x_3$ | \leq | ∞ |
| 5 | \leq | $10x_2 + 7x_3$ | \leq | ∞ |





Solving the model

- General MILP solver
- SSG algorithm and LP solver for each solution structure
- General branch and bound method
- ABB





Search tree



General branch and bound

SSG





ABB

- Based on SSG
 - Same search tree
- Lower bound generated by solving the relaxed MILP
- Input maximal structure
- Output optimal structure





New variables in the ABB algorithm

- U value of the current best solution
- current_best the current best solution
- bound lower bound of the subproblem





Initialization of the ABB algorithm

begin

- $U = \infty;$
- $ABB(\mathcal{P}, \emptyset, \emptyset);$
- if $U < \infty$ then
 - print current_best;

else

print "There is no solution";

end





ABB algorithm

```
procedure ABB(p, m, \delta[p])
begin
    let x \in p;
    \mathbf{C} \coloneqq \wp(\Delta(x)) \setminus \{\emptyset\};
    for all c \in C do
         if \forall y \in m, c \cap \overline{\delta}(y) = \emptyset and (\Delta(x) \setminus c) \cap \delta(y) = \emptyset then
             \mathbf{p}' = (\mathbf{p} \cup \psi^{-}(\mathbf{c})) \setminus (\mathcal{R} \cup \mathbf{m} \cup \{x\});
             \mathbf{m}' = \mathbf{m} \cup \{x\};
             \delta[\mathbf{m}'] = \delta[\mathbf{m}] \cup \{(x, \mathbf{c})\};
             bound = BOUND(\delta[m']);
             if U \ge bound then
                  if p' = \emptyset then
                      U = bound;
                      currentbest = \delta[m'];
                  else
                      ABB(p', m', \delta[m']);
```

end





Neutral extension

• $\delta_x[m \cup \{x\}] = \delta[m] \cup \{(x,d)\}$ is a **direct neutral** extension of $\delta[m]$ consistent decision mapping, if $x \in (\psi^-(\varphi(\delta[m])) \cup \mathcal{P}) \setminus (m \cup \mathcal{R}), d \subset \Delta[m]$, and *c* is inconsistent if $c \in \wp(\delta(x)) \setminus \{\emptyset, d\}$

I.e., only d is consistent decision

- $\delta_n[m_n]$ (n = 0,1,...) decision mapping is a **neutral** extension of $\delta_0[m_0]$ if there exists $\delta_0[m_0]$, $\delta_1[m_1]$, ..., $\delta_n[m_n]$ such that $\delta_i[m_i]$ is direct neutral extension of $\delta_{i-1}[m_{i-1}]$ (i = 1,2,...,n)
- $\hat{\delta}[\hat{m}]$ consistent decision mapping is the **maximal neutral extension** of $\delta[m]$, if it is neutral extension of $\delta[m]$ and it has no neutral extension





Initialization of the extended ABB algorithm

begin

 $U = \infty;$

let $\hat{\delta}[\hat{m}]$ the maximal neutral extension of $\delta[m]$;

$$\mathbf{p} = \left(\psi^{-}\left(\varphi(\hat{\delta}[\hat{\mathbf{m}}]\right)\right) \cup \mathcal{P} \setminus (\hat{\mathbf{m}} \cup \mathcal{R});$$

if $p = \emptyset$ then

 $U = \text{BOUND}(\hat{\delta}[\hat{m}]);$

update currentbest;

else

ABB(p, \hat{m} , $\hat{\delta}[\hat{m}]$);

if $U < \infty$ then

print current_best;

else

print "There is no solution";

end





Extended ABB algorithm

| procedure ABB(p, m, δ [p]) |
|---|
| begin |
| let $x \in p$; |
| $C := \wp \big(\Delta(x) \big) \setminus \{ \emptyset \};$ |
| for all $c \in C$ do |
| if $\forall y \in m, c \cap \overline{\delta}(y) = \emptyset$ and $(\Delta(x) \setminus c) \cap \delta(y) = \emptyset$ then |
| $\mathbf{p}' = \left(\psi^-\left(\varphi\big(\delta\big[\mathbf{\widehat{m}}'\big]\big)\right)\right) \cup \mathcal{P} \setminus \big(\mathbf{\widehat{m}}' \cup \mathcal{R}\big);$ |
| $\mathbf{m}' = \mathbf{m} \cup \{x\};$ |
| $\delta[\mathbf{m}'] = \delta[\mathbf{m}] \cup \{(\mathbf{x}, \mathbf{c})\};$ |
| let $\widehat{\delta}[\widehat{\mathbf{m}}']$ the maximal neutral extension of $\delta[m'];$ |
| $bound = BOUND(\hat{\delta}[\hat{m}']);$ |
| if $U \ge bound$ then |
| if $p' = \emptyset$ then |
| U = bound; |
| $currentbest = \delta[\widehat{\mathbf{m}}'];$ |
| else |
| $ABB(\mathrm{p}',\widehat{\mathrm{m}}',\widehat{\delta}[\widehat{\mathrm{m}}']);$ |

end





Acceleration

(B,{O2,O3}) (B,{O2}) (B,{O3}) (D,{O4}) (D,{O4,O5}) (D,{O4,O5}) (D,{O4}) (E,{O6}) (D,{O5}) (D,{O5}) Search tree (G,{O2,O8}) (G,{O2,O8}) (G,{O2,O8}) (G,{O2,O8}) (G,{O2,O8}) (G,{O2,O8}) (I,{O10}) (G,{O2}) without neutral (G,{O2} (G,{O2}) (G,{O2}) (G,{O2}) (G,{O2} extension (U,{O3}) (E,{O6}) (E,{O6}) (E,{O6}) (E,{O6}) (E,{O6}) (E,{O6}) (I,{O10}) (I,{O10}) (I,{O10}) (I,{O10}) (I,{O10}) (I,{O10}) (U,{O3}) (U,{O3}) (U,{O3}) (U,{O3}) (U,{O3}) (U,{O3}) Search tree with neutral extension 355



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Synthesis of Reliable Process Networks



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- Introduciton.
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Introduciton

- The system reliability, or in other words the probability of an error-free operation, has been a research area for long time (Neumann, 1956).
- In the conventional approach there are some points which is not clear enough (rigorously), i.e.
 - the concept and structure of the system model
 - the definition of operability
- To overcome the difficulties and to reach new results, application of the P-graph methodology for the studying of the process networks is proposed.
- Hereinafter, the conventional system model is generalized.





Conventional model and Pgraph model








The concept of the network model

- A network is built up of operating units.
- The structure of the network is described by the system model.
- An operating unit is either working, or not.

 $x_i = \begin{cases} 1 \text{ if the i operating unit is working} \\ 0 \text{ if the i operating unit is not working} \end{cases}$ $X = (x_1, x_2, \dots x_n) \text{ a state of the system}$

- The operability of the system is a function of states: $\exists \Psi(x_1, x_2, ..., x_n) = \begin{cases} 1 & \text{if the system is working} \\ 0 & \text{if the system is not working} \end{cases}$
- Note that it is a monotone logic function.





Definition of reliability

- The space describing the possibly states of the system $\Omega = \{0,1\}^n = \{(0,0,...,0), (0,0,...,1), ..., (1,1,...,1)\}$
- The state of the system, an elementary event $(b_1, b_2, ..., b_n) \in \Omega$
- A system event $E = \{(x_1, x_2, ..., x_n) \in \Omega : \varphi(x_1, x_2, ..., x_n) = 1\}$
- Let O be the "system is working" system event $O = \{(x_1, x_2, ..., x_n) \in \Omega : \Psi(x_1, x_2, ..., x_n) = 1\}$
- The Reliability of the system = the probability of the event O R = P(O)





Probability of system events

- Let the probability of the states of the operating units be $p_i = P(x_i = 1)$ $1 - p_i = P(x_i = 0)$
- For the elementery event $(b_1, b_2, ..., b_n) \in \Omega$
- the probability of its supervention is

$$P((x_1, x_2, ..., x_n) = (b_1, b_2, ..., b_n)) = \prod_{i=1}^n p_i^{b_i} (1 - p_i)^{(1 - b_i)}$$

The probability of a system event is given by the

$$P(A) = \sum_{(x_1, x_2, \dots, x_n) \in A} \prod_{i=1}^n p_i^{x_i} (1 - p_i)^{(1 - x_i)}$$

- polynom.
- Thus, there exists a polynom for reliability as well $R = P(\Psi(x_1, x_2, ..., x_n) = 1) = Q(p_1, p_2, ..., p_n)$





Characteristic polynoms

An arbitrary E system event

$$E = \{(x_1, x_2, ..., x_n) \in \Omega : \varphi(x_1, x_2, ..., x_n) = 1\}$$

Characteristic polynom is that Q polynom, for which

$$Q(x_1, x_2, ..., x_n) = 1 \quad ha \quad (x_1, x_2, ..., x_n) \in E$$
$$Q(x_1, x_2, ..., x_n) = 0 \quad ha \quad (x_1, x_2, ..., x_n) \notin E$$
and

 $Q(p_1, p_2, ..., p_n) = P(E)$ ha $p_1 = P(x_1 = 1), p_2 = P(x_2 = 1), ..., p_n = P(x_n = 1)$





Characteristic polynoms (2)

Let us consider the following system event

$$\varphi(x_1, x_2, x_3) = x_2 \lor x_1 \land x_2 \land x_3$$
$$E = \{ (x_1, x_2, x_3) \in \Omega : \varphi(x_1, x_2, x_3) = 1 \}$$

Then

$$Q(x_1, x_2, x_3) = x_2 + x_1 * (1 - x_2) * x_3, \quad x_1, x_2, x_3 \in [0, 1]$$

Why?

Because the system events defined by the clouses of the logical function are disjoint (+) and the system events defined by variables that build up the clouses are independent (*).





Two specific characteristic polynoms

The probability of the i-th operating unit is

$$p_i = P(x_i = 1)$$
 $1 - p_i = P(x_i = 0)$

• Serial system $\Psi(x_1, x_2, ..., x_n) = x_1 \wedge x_2 \wedge ... \wedge x_n$

$$R = P(\Psi(x_1, x_2, ..., x_n) = 1) = \prod_{i=1}^n p_i$$

$$Q(x_1, x_2, ..., x_n) = x_1 * x_2 * ... * x_n$$

• Parallel system $\Psi(x_1, x_2, ..., x_n) = x_1 \lor x_2 \lor ... \lor x_n$

$$R = P(\Psi(x_1, x_2, ..., x_n) = 1) = 1 - \prod_{i=1}^n (1 - p_i)$$
$$Q(x_1, x_2, ..., x_n) = 1 - (1 - x_1) * (1 - x_2) * ... * (1 - x_n)$$





Reliability of process networks

- A process network is considered working, if the set of working operating units has a subset that represents a solution structure.
- Our goal is to produce the logic functions
- $\Psi(x_1, x_2, ..., x_n)$ that define the "system is working" system event.
- A $\Phi(X)$ logical function can be given, for which
- $\Phi(x_1, x_2, ..., x_n) = 1$ if and only if the operating units given by $(x_1, x_2, ..., x_n)$ represent a solution structure.



es

The number of solution structures

Let us consider the system event where the operating part is the solution structure

$$A = \{(x_1, x_2, ..., x_n) \in \Omega : \Phi(x_1, x_2, ..., x_n) = 1\}$$

Let S be the characteristic function of the A system event

$$S(x_1, x_2, ..., x_n)$$

from this
$$S(x) = S(x, x, ..., x)$$

Then the number of solution structures is:

$$2^n S(\frac{1}{2})$$





The number of solution structers: An example

There are N parallel operating unit

$$\Psi(X) = \Phi(x_1, x_2, \dots, x_n) = x_1 \lor x_2 \lor \dots \lor x_n$$

• With disjoint clauses (Only n number of clauses!) $\Psi(X) = x_1 \vee \overline{x_1} x_2 \vee \ldots \vee \overline{x_1} \overline{x_2} \ldots \overline{x_{n-1}} x_n$ $S(x) = x + (1-x)x + \ldots + (1-x)^{n-1}x$ $S(\frac{1}{2}) = \frac{1}{2} + \frac{1}{4} + \ldots + \frac{1}{2^n}$ $2^n S(\frac{1}{2}) = 2^n - 1$



Reliability of process networks

Step I.:

 $\Phi(x_1, x_2, ..., x_n) = \Phi_0 \wedge \Phi_1 \wedge \Phi_2$ $\Phi_0(x_1, x_2, ..., x_n) = \bigwedge_{\substack{X \in P \ j \in J \\ X \in \beta_j}} x_j$ $\Phi_1(x_1, x_2, ..., x_n) = \bigwedge_{\substack{j \in J \\ X \in \alpha_j/R}} (\overline{x_j} \vee \bigvee_{\substack{h \in J \\ X \in \beta_h}} x_h)$ $\Phi_2(x_1, x_2, ..., x_n) = \bigwedge_{\substack{j \in J \\ P \cap \beta_j = \emptyset}} (\overline{x_j} \vee \bigvee_{\substack{h \in J \\ \beta_j \cap \alpha_h}} x_h)$

Step II.:

- Disjoint normal form
- With the help of syntactic rules





Reliability of process networks

Step III.:

• Calculate $\Psi(x_1, x_2, ..., x_n)$

Delete the negative variables from

$$\Phi(x_1, x_2, \dots, x_n)$$

Step IV.:

Generate the disjoint closes

$$\Psi(X) = L_1 \lor L_2 \lor \ldots \lor L_s$$

$$\Psi(X) = L_1 \lor \overline{L_1} L_2 \lor \overline{L_1} \overline{L_2} L_3 \lor \ldots \lor \overline{L_1} \overline{L_2} \ldots \overline{L_{s-1}} L_s$$

Remark: This can explode!

But it is not necessary to geneerate them explicitly!





Another way: Prime structures

Step I.:

- Calculate $\Psi(x_1, x_2, ..., x_n)$ $\Psi(X) = K_1 \lor K_2 \lor ... \lor K_s$ $K_i = x_{i_1} \land x_{i_2} \land ... \land x_{i_l} \quad i \in \{1, 2, ..., s\}$
- where $i_1, i_2, ... i_l$ are operating units of the i-th prime structure

Step II.:

Generate the disjoint clauses

 $\Psi(X) = K_1 \vee \overline{K_1} K_2 \vee \overline{K_1} \overline{K_2} K_3 \vee \ldots \vee \overline{K_1} \overline{K_2} \ldots \overline{K_{s-1}} K_s$





Calculating reliability

• In cases before the disjunction of disjoint clauses $\Psi(X) = K_1 \vee \overline{K_1} K_2 \vee \overline{K_1} \overline{K_2} K_3 \vee ... \vee \overline{K_1} \overline{K_2} ... \overline{K_{s-1}} K_s$ $\Psi(X) = \bigvee_{i=1}^r (\bigwedge_{j=1}^l z_{i_j}) \quad ahol \quad z_i = x_i \text{ vagy } \overline{x_i}$ $u_{i_j} = \begin{cases} 1 \quad \text{if} \quad z_{i_j} = x_{i_j} \\ 0 \quad \text{if} \quad z_{i_j} = \overline{x_{i_j}} \end{cases}$

$$R = P(\Psi(X) = 1) = \sum_{i=1}^{r} \prod_{j=1}^{l} p_{i_j}^{u_{i_j}} (1 - p_{i_j})^{(1 - u_{i_j})}$$





Calculating reliability

• It is not necessary to produce the $\Psi(X)$ function explicitly







Calculating reliability

This procedure gives the system reliability.

$$K_1^* = K_1$$

$$K_2^* = K_2 \setminus (K_1 \cap K_2)$$

$$K_3^* = K_3 \setminus ((K_1 \cap K_3) \setminus ((K_2 \cap K_3) \setminus (K_1 \cap K_2 \cap K_3)))$$

$$P(K_3^*) = P(K_3) - (P(K_1K_3) - (P(K_2K_3) - P(K_1K_2K_3)))$$

procedure(inpSTR) while($K_i = nextPRIM != \emptyset$) $\begin{cases} K_i^* = K_i \setminus (\bigcup_{j=1}^{i-1} K_j^* \cap K_i) \\ R = R + P(K_i^*) \end{cases}$





A third way: Cutting sets

- A set of operating units H is called to be a cutting set if in case the operating units are not working, then the system is also not working.
- Let E be the set of cutting sets, then:

$$R = 1 - \sum_{H \in E} \prod_{i \in H} \left[1 - p_i \right] \prod_{i \notin H} \left[p_i \right]$$

The aggregate value is the sum of the probabilities of events when the system is not working.

$$E = \{(x_1, x_2, ..., x_n) \in \Omega : \Psi(x_1, x_2, ..., x_n) = 0\}$$
$$R = P(E)$$





Example: Function of solution structures

• Step I.: $\Phi(x_1, x_2, x_3) = \Phi_0 \land \Phi_1 \land \Phi_2$ $\Phi_0(x_1, x_2, x_3) = x_3$ $\Phi_1(x_1, x_2, x_3) = (\overline{x_3} \lor x_1 \lor x_2) \land (\overline{x_3} \lor x_2)$ $\Phi_2(x_1, x_2, x_3) = (\overline{x_1} \lor x_3) \land (\overline{x_2} \lor x_3)$

Step II.:

$$\Phi(x_1, x_2, x_3) = x_2 \wedge x_3$$

- Step III.: None
 - $\Psi(x_1, x_2, x_3) = x_2 \wedge x_3$ $Q(x_1, x_2, x_3) = x_2 * x_3$
- Step IV.: None







Example: Prime structures

There is only one prime structure {2, 3}

Step I.:

There is only one clause

$$\Psi(x_1, x_2, x_3) = x_2 \wedge x_3$$
$$Q(x_1, x_2, x_3) = x_2 * x_3$$

Step II.:

None







Example: Cutting sets

- A set of operating units is a cutting set, if they are switched off, the system does no work.
- Let E be the set of cutting sets
- E={ {2}, {3}, {1,3}, {2,3}, {1,2}, {1,2,3} }





 $\mathbf{R} = 1 - ((2/3)^*(1/2)^*(3/4) + (2/3)^*(1/2)^*(1/4) + \ldots) = 18/48$





Conventional model and P-graph model







Based on solution structures, Example 1

Step I.: $\Phi(x_1, x_2, ..., x_5) = \Phi_0 \land \Phi_1 \land \Phi_2$

 $\Phi_0(X) = x_5$ $\Phi_1(X) = (\overline{x_5} \lor x_3 \lor x_4) \land$ $(\overline{x_4} \lor x_1 \lor x_2 \lor x_3) \land (\overline{x_3} \lor x_1)$ $\Phi_2(X) = (\overline{x_1} \lor x_3 \lor x_4) \land (\overline{x_2} \lor x_4) \land$ $(\overline{x_3} \lor x_5) \land (\overline{x_4} \lor x_5)$

Step II. III. and IV.:

R = 0,8748



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Based on prime structures, Example 1

- Step I.:
- **•** {1,3,5}, {1,4,5}, {2,4,5,}
 - $\Psi(X) = (x_1 \wedge x_3 \wedge x_5) \vee (x_1 \wedge x_4 \wedge x_5)$ $\vee (x_2 \wedge x_4 \wedge x_5)$

Step II.:

$$\Psi(X) = (x_1 \land x_3 \land x_5) \lor (x_1 \land \overline{x_3} \land x_5) \lor (x_1 \land \overline{x_3} \land x_5) \lor (x_1 \land x_2 \land x_4 \land x_5)$$
$$Q(X) = x_1 * x_3 * x_5 + x_1 * (1 - x_3) * x_4 * x_5 + (1 - x_1) * x_2 * x_4 * x_5$$







Based on prime structures, Example 1

The steps of the algorithm

$$\begin{split} K_1^* &\to p_1 = P(K_1) \\ K_1^* \to p_1 = P((x_1 x_3 x_5)) = 0,729 \\ K_2^* \to p_2 = P(K_2) - P(K_1 K_2) \\ K_2^* \to p_2 = P((x_1 x_4 x_5)) - P((x_1 x_3 x_4 x_5)) \\ &= 0,729 - 0,6561 \\ K_3^* \to p_3 = P(K_3) - P(K_1 K_3) - (P(K_2 K_3) - P(K_1 K_2 K_3)) \\ K_3^* \to p_3 = P(x_2 x_4 x_5) - P(x_1 x_2 x_3 x_4 x_5) - ((P(x_1 x_2 x_4 x_5) - P(x_1 x_2 x_3 x_4 x_5))) \\ &= 0,729 - 0,6561 \end{split}$$

$$R = 0,8748$$





Based on cutting sets, Example1

- It is very exhausting to give explicitly
- {5},{1,2},{1,4},{1,5},{2,5},{3,5},,{4,5},{1,2,3},...







Gas network



Fig. 5. A natural gas transmission network in Shelby County, TN [19].







Reliability and synthesis

- A maximal structure is given.
- Which is the most reliable solution?
- Naturally the maximal structure!
- What is value of reliability of a solution?

$$X \in \Omega \text{ és } \Phi(X) = 1$$

$$B_X = \{Y \in \Omega : Y \le X\}$$

$$A_X = \{Y \in \Omega : \Psi(Y) = 1 \text{ és } Y \in B_X\}$$

$$R_X = P(A_X \mid B_X) = P(A_X) / P(B_X)$$

$$R_{(1,1,\dots,1)} = P(\Psi(X) = 1) / P(\Omega) = P(\Psi(X) = 1) = R$$





Reliability and synthesis, Case I.

- How reliable units to be used?
- For a given system, we are looking for the solution for which in the dependence of the reliability of the operating units costs minimum and it suffices the confidence value for the operability of the system.
- Let be $Y = (y_1, y_2, ..., y_n)$ ahol $y_i = P(x_i = 1)$
- The mathematical model:

$$Q(Y) \ge R_{k\bar{u}sz\bar{o}b}$$
$$Y \in [0,1]^n$$
$$\overline{C(Y) \to \min}$$



(2)

Reliability and synthesis, Case I. (2)

 $y_2 + y_1(1 - y_2)y_3 \ge 0,95$ $y_1, y_2, y_3 \in [0,1]$

 $\frac{10}{(1.005 - y_1) + 50} (1.005 - y_2) + \frac{10}{(1.005 - y_3)} \rightarrow \min$



| Eset_I | Gép1 | Gép2 | Gép3 | Rendszer | Küszöb |
|------------------|-----------|-----------|----------------|----------------------------|-----------|
| | X1 | X2 | Х3 | Q=x2+x1(1-x2)x3 | |
| Megbízhatóság | 0,9343698 | 0,6030567 | 0,9355258 | 0,950035567 | 0,95 |
| KöltségParaméter | 10 | 50 | 10 | | |
| Költség_FGV | 86,482579 | 111,87101 | 87,355934 | 285,7095185 | Költség |
| | | | | | |
| 0,05 | 20,00 | | | | |
| 0,1 | 21,05 | | | | |
| 0,15 | 22,22 | | | | |
| 0,2 | 23,53 | | | | |
| 0,25 | 25,00 | | | | |
| 0,3 | 26,67 | | | | |
| 0,35 | 28,57 | 250,00 | | | |
| 0,4 | 30,77 | | | | |
| 0,45 | 33,33 | 200,00 | | | |
| 0,5 | 36,36 | | | | |
| 0,55 | 40,00 | 150.00 | | | |
| 0,6 | 44,44 | 150,00 | | | |
| 0,65 | 50,00 | | | | |
| 0,7 | 57,14 | 100,00 | | | — |
| 0,75 | 66,67 | | | | |
| 0,8 | 80,00 | 50.00 | | | |
| 0,85 | 100,00 | 20,00 | | | |
| 0,9 | 133,33 | | | | |
| 0,95 | 200,00 | 0,00 | | | |
| 1 | 400,00 | | 0,05 0,15 0,25 | 5 0,35 0,45 0,55 0,65 0,75 | 0,85 0,95 |
| | | | | | |

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Reliability and synthesis, Case II.

- Which is the most critical event?
- Which is the most probable critical event, for which in case of its supervention the system is not working?

$$p_{krit} = \max_{\{X \in \Omega \ és \ \Psi(X) = 0\}} P(A_X), \quad A_X = \{Y : Y \in \Omega, \ Y \le X\}$$

$$Q(X) = 0$$

$$X \in \{0,1\}^{n}$$

$$\overline{\sum_{i=1}^{n} p_{i}^{x_{i}} (1 - p_{i})^{(1 - x_{i})}} \to \min = p_{krit}$$

It is proposed to investigate the conditions for the joint failure of the operating units belonging to the zero elements of X!





Reliability and synthesis, Case II. (2)

 The 2nd and 3rd operating units' combined shut down is critical.



| | Gép1 | Gép2 | Gép3 | Rendszer | Küszöb |
|-----------------|----------|----------|----------|-----------------|--------|
| | X1 | X2 | Х3 | Q=x2+x1(1-x2)x3 | |
| Megbízhatóság | 0,927696 | 0,642646 | 0,927215 | 0,950032501 | 0,95 |
| KöltségParaméte | 10 | 100 | 10 | | |
| Költség_FGV | 136,4183 | 279,0535 | 135,529 | 551,0008238 | KTSG |
| | | | | | |
| RendszerLeállás | 1 | 0 | 0 | 0 | 0 |
| | 1 | 0,357354 | 0,072785 | 0,026010007 | |





Reliability and synthesis, Case III.

- Which operating units should be replicated and how many times?
- A network is given with the reliability of its operating units, costs and a given reliability threshold value for the system.
- We are looking for a system produced by the multiplication of the operating units, that suffices the given reliability threshold and has minimal cost.





Reliability and synthesis, Case III. (2)

Should we multiply the units by themselves one by one, or fittingly chosen subsystems?

$$\begin{split} R_1 &= p_1 * p_2 \\ R_2 &= (1 - (1 - p_1) * (1 - p_1)) * (1 - (1 - p_2) * (1 - p_2)) \\ R_3 &= (1 - (1 - p_1 p_2) * (1 - p_1 p_2)) \end{split}$$



 $R_2 \ge R_3$

This holds in general!





Reliability and synthesis, Case III. (3)

 According to this, it is sufficient to multiply the operating units by themselves, until the given confidence level is reached.







Reliability and synthesis, Case III. (4)

If we multiply the operating units, we have to produce the characteristic polynom of the new system.

$$\Psi(x_1, x_2, ..., x_n) \rightarrow Q(x_1, x_2, ..., x_n)$$

$$R(k_1, k_2, ..., k_n, x_1, x_2, ..., x_n) = Q(1 - (1 - x_1)^{k_1}, 1 - (1 - x_2)^{k_2}, ..., 1 - (1 - x_n)^{k_n})$$

• The mathematical model of the problem:

$$k_{1}, k_{2}, \dots, k_{n} \in N$$

$$R(k_{1}, k_{2}, \dots, k_{n}, p_{1}, p_{2}, \dots, p_{n}) \ge p_{k\bar{u}sz\bar{o}b}$$

$$\overline{C(k_{1}, k_{2}, \dots, k_{n}) = k_{1}b_{1} + k_{2}b_{2} + \dots + k_{n}b_{n} \rightarrow \min}$$





Solution of a synthesis problem

• The problem:

$$p_1 = 0,8 \quad p_2 = 0,6 \quad p_3 = 0,9$$

$$c_1 = 10 \quad c_1 = 50 \quad c_1 = 20 \quad p_{kiiszöb} = 0,95$$

$$\Psi(x_1, x_2, x_3) = x_2 + x_1 x_2 x_3$$

$$Q(x_1, x_2, x_3) = x_2 + x_1 (1 - x_2) x_3$$

$$R(2, x_1, x_2, x_3) = Q(2x_1 - x_1^2, 2x_2 - x_2^2, 2x_3 - x_3^2)$$







Solution of a synthesis problem, R>=0,95.

| Töbszörözés | Q=x2+x1(1-x2)x3 | Х3 | X2 | X1 |
|-------------|-----------------|-------------|------------|------------|
| 1X | 0,888 | 0,9 | 0,6 | 0,8 |
| 2X | 0,992064 | 0,99 | 0,84 | 0,96 |
| ЗХ | 0,999424512 | 0,999 | 0,936 | 0,992 |
| 4X | 0,999956484 | 0,9999 | 0,9744 | 0,9984 |
| 5X | 0,999996621 | 0,99999 | 0,98976 | 0,99968 |
| 6X | 0,999999734 | 0,999999 | 0,995904 | 0,999936 |
| 7X | 0,999999979 | 0,9999999 | 0,9983616 | 0,9999872 |
| 8X | 0,999999998 | 0,999999999 | 0,99934464 | 0,99999744 |
| | | | | |
| 0,95 | 0,9504 | 0,99 | 0 | 0,96 |
| 1X | 1 | 0 | 0 | 0 |
| 2X | 2 | 1 | 0 | 1 |
| ЗХ | 3 | 0 | 0 | 0 |
| 4X | 4 | 0 | 0 | 0 |
| 5X | 5 | 0 | 0 | 0 |
| 6X | 6 | 0 | 0 | 0 |
| 7X | 7 | 0 | 0 | 0 |
| 8X | 8 | 0 | 0 | 0 |
| Db | | 2 | 0 | 2 |
| Beruházás | 60 | 20 | 50 | 10 |
| Működőképes | 1 | 1 | 0 | 1 |






Solution of a synthesis problem, R>=0,9999

| Töbszörözés | Q=x2+x1(1-x2)x3 | Х3 | X2 | X1 |
|-------------|-----------------|-------------|------------|------------|
| 1X | 0,888 | 0,9 | 0,6 | 0,8 |
| 2X | 0,992064 | 0,99 | 0,84 | 0,96 |
| ЗХ | 0,999424512 | 0,999 | 0,936 | 0,992 |
| 4X | 0,999956484 | 0,9999 | 0,9744 | 0,9984 |
| 5X | 0,999996621 | 0,99999 | 0,98976 | 0,99968 |
| 6X | 0,999999734 | 0,999999 | 0,995904 | 0,999936 |
| 7X | 0,999999979 | 0,9999999 | 0,9983616 | 0,9999872 |
| 8X | 0,999999998 | 0,999999999 | 0,99934464 | 0,99999744 |
| | | | | |
| 0,9999 | 0,999926001 | 0,99999 | 0 | 0,999936 |
| 1X | 1 | 0 | 0 | 0 |
| 2X | 2 | 0 | 0 | 0 |
| ЗХ | 3 | 0 | 0 | 0 |
| 4X | 4 | 0 | 0 | 0 |
| 5X | 5 | 1 | 0 | 0 |
| 6X | 6 | 0 | 0 | 1 |
| 7X | 7 | 0 | 0 | 0 |
| 8X | 8 | 0 | 0 | 0 |
| Db | | 5 | 0 | 6 |
| Beruházás | 160 | 20 | 50 | 10 |
| Működőképes | 1 | 1 | 0 | 1 |







Solution with other parmeters.



| X1 | . X2 | Х3 | Q=x2+x1(1-x2)x3 | Töbszörözés |
|------------|------------|------------|-----------------|-------------|
| 0,7 | 0,6 | 0,8 | 0,824 | 1X |
| 0,91 | 0,84 | 0,96 | 0,979776 | 2X |
| 0,973 | 0,936 | 0,992 | 0,997773824 | ЗХ |
| 0,9919 | 0,9744 | 0,9984 | 0,999752012 | 4X |
| 0,99757 | 0,98976 | 0,99968 | 0,999971848 | 5X |
| 0,999271 | 0,995904 | 0,999936 | 0,999996752 | 6X |
| 0,9997813 | 0,9983616 | 0,9999872 | 0,999999621 | 7X |
| 0,99993439 | 0,99934464 | 0,99999744 | 0,999999955 | 8X |
| | | | | |
| C | 0,9744 | 0 | 0,9744 | 0,95 |
| C | 0 | 0 | 1 | 1X |
| C | 0 | 0 | 2 | 2X |
| C | 0 | 0 | 3 | ЗХ |
| C |) 1 | 0 | 4 | 4X |
| C | 0 | 0 | 5 | 5X |
| C | 0 | 0 | 6 | 6X |
| C | 0 | 0 | 7 | 7X |
| C | 0 | 0 | 8 | 8X |
| C | 4 | 0 | | Db |
| 10 | 10 | 10 | 40 | Beruházás |
| C | 1 | 0 | 1 | Feltétel |





Solution of the relaxed model

The upper bound of the multiplication has to be determined for each operating unit.

We get an exact upper bound for the costs, but not yet for the multiplication of the units.

$$y_1, y_2, \dots, y_n \in R_+$$

$$R(y_1, y_2, \dots, y_n, p_1, p_2, \dots, p_n) \ge p_{k \mbox{isz} \mbox{ob}}$$

$$\overline{C(y_1, y_2, \dots, y_n) = y_1 b_1 + y_2 b_2 + \dots + y_n b_n} \to \min$$

| Y1 | Y2 | Y3 | Q=(y1,y2,y3) | Küszöb |
|----------|----------|----------|--------------|---------|
| 6,312369 | 0,000427 | 4,201173 | 0,999898417 | 0,9999 |
| 0,8 | 0,7 | 0,9 | | |
| 10 | 50 | 20 | 147,1685129 | Költség |

$$Q(x_1, x_2, x_3) = x_2 + x_1(1 - x_2)x_3$$

$$R(Y, P) = (1 - (1 - p_2)^{y_2}) + (1 - (1 - p_1)^{y_1}) * (1 - p_2)^{y_2} * (1 - (1 - p_3)^{y_3})$$





Exact upper bound for multiplication

• With the help of prime structures.

$$\begin{split} \Psi(X) &= K_1 \lor K_2 \lor \ldots \lor K_s \\ K_i &= x_{i_1} \land x_{i_2} \land \ldots \land x_{i_l} \quad i \in \{1, 2, \ldots, s\} \\ a_j &= \min_{z \in N} \left\{ z : (1 - (1 - p_{j_1})^z) * (1 - (1 - p_{j_2})^z) * \ldots * (1 - (1 - p_{j_l})^z) \ge p_{kiiszob} \right\} \\ k_i &= \max_{j = (1, 2, \ldots, s)} \left\{ v_j = \begin{cases} a_j & \text{if } i \in \{j_1, j_2, \ldots, j_l\} \\ 0 & \text{otherwise} \end{cases} \end{split}$$





Boundaries

| X1 | X2 | Х3 | Q=x2+x1(1-x2)x3 | Töbszörözés | {1,3} | {2} |
|------------|------------|-------------|-----------------|-------------|-------------|------------|
| 0,8 | 0,7 | 0,9 | 0,916 | 1X | 0,72 | 0,7 |
| 0,96 | 0,91 | 0,99 | 0,995536 | 2X | 0,9504 | 0,91 |
| 0,992 | 0,973 | 0,999 | 0,999757216 | ЗХ | 0,991008 | 0,973 |
| 0,9984 | 0,9919 | 0,9999 | 0,999986231 | 4X | 0,99830016 | 0,9919 |
| 0,99968 | 0,99757 | 0,99999 | 0,999999198 | 5X | 0,999670003 | 0,99757 |
| 0,999936 | 0,999271 | 0,999999 | 0,999999953 | 6X | 0,999935 | 0,999271 |
| 0,9999872 | 0,9997813 | 0,9999999 | 0,999999997 | 7X | 0,9999871 | 0,9997813 |
| 0,99999744 | 0,99993439 | 0,999999999 | 1 | 8X | 0,99999743 | 0,99993439 |
| | | | | | | |
| 0,999936 | 0 | 0,99999 | 0,999926001 | 0,9999 | | |
| 0 | 0 | 0 | 1 | 1X | | |
| 0 | 0 | 0 | 2 | 2X | | |
| 0 | 0 | 0 | 3 | ЗХ | | |
| 0 | 0 | 0 | 4 | 4X | | |
| 0 | 0 | 1 | 5 | 5X | | |
| 1 | 0 | 0 | 6 | 6X | | |
| 0 | 0 | 0 | 7 | 7X | | |
| 0 | 0 | 0 | 8 | 8X | | |
| 6 | 0 | 5 | | Db | | |
| 50 | 80 | 50 | 550 | Beruházás | | |
| 1 | 0 | 1 | 1 | Működőképes | | |





Reliability and synthesis. Calculations.

Formulas:

$$\begin{aligned} \Psi(x_1, x_2, \dots, x_n) & \to \quad Q(x_1, x_2, \dots, x_n) \\ R(k_1, k_2, \dots, k_n, x_1, x_2, \dots, x_n) &= Q(1 - (1 - x_1)^{k_1}, 1 - (1 - x_2)^{k_2}, \dots, 1 - (1 - x_n)^{k_n}) \\ R(k, x_1, x_2, \dots, x_n) &= Q(1 - (1 - x_1)^k, 1 - (1 - x_2)^k, \dots, 1 - (1 - x_n)^k) \\ R(2k, x_1, x_2, \dots, x_n) &= R(k, 2x_1 - x_1^2, 2x_2 - x_2^2, \dots, 2x_n - x_n^2) \end{aligned}$$

Iterations:

$$R(k_1, k_2, ..., k_n, p_1, p_2, ..., p_n) =$$

$$Q(1 - (1 - p_1)^{k_1}, 1 - (1 - p_2)^{k_2}, ..., 1 - (1 - p_n)^{k_n})$$

$$\forall i \quad u_{k_i} = 1 - (1 - p_1)^{k_i}$$

$$R(k_1 + 1, k_2 + 1, ..., k_n + 1, p_1, p_2, ..., p_n) = Q(p_1 + u_{k_1}(1 - p_1), p_2 + u_{k_2}(1 - p_2), ..., p_n + u_{k_n}(1 - p_n))$$





Summary

- The reliability of a process systems was defined.
- The concept of characteristic polynoms was introduced.
- A closed formula for the number of solutions was given.
- Three methods for generating reliability and a way for calculating it were introduced.
- A transposition rule to P-graph model was given.
- Case studies were investigated.
- Three synthesis problem, that are based on the measure of reliability were raised and solved.
- Further problems are to be solved.





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Sustainable Energy Supply Chain Synthesis Using the P-graph Methodology







Outline

- Sustainability metrics (ecological footprint, emergy)
- Supply chain design by P-graph framework
- Incorporation of sustainability constraints
- Illustrative example







Cooperation



University of Pannonia, Department Computer Science and Systems



U.S. EPA, Office of Research and Development



footprint



Ecological footprint







Objective

P-graph methodology

Sustainability







Environmental protection





Environmental protection

- Environmental protection is an older concept than sustainability but the two are closely related
- Environmental protection: do not damage the environment unnecessarily, protect
 - the water
 - the soil
 - the air
 - the forest
- Otherwise society will pay the price
 - if not now then later





Learn from the mistakes of the past: Maya empire





Art



| 0 | 1 • | 2 •• | 3 ●●● | 4 •••• |
|----|---------|----------|-----------|-----------|
| 5 | 6 | 7 | 8 | 9 |
| 10 | 11 | 12 | 13 ••• | 14 |
| 15 | 16 • | 17 •• | 18 ••• | 19 |
| 15 | 16 | 17 | 18 | 19 |

Science





Maya empire





Huge cities

Pyramids









Maya empire

- Rapid collapse around 900
- Possible reasons:
 - overpopulation
 - attack
 - trade collapse
 - climate change
 - epidemic
 - agriculture fails





Mesopotamia

- Advanced irrigation system
- The city of Mashkan-shapir was suddenly abandoned
 - the irrigation destroyed the soil in the long run by accumulating mineral salts
- In the San Joaquin valley (USA, California) it happens again



Salt-damaged fields in California's San Joaquin Valley





Big civilizations

- Maya
- Aztecs
- Inca
- Egypt
- Roman
- Mongol
- ...
- They failed because of
 - attack
 - crumbled under they own weight, they were not sustainable





Human beings always disturb the environment











Pollution

It is not dark but smog



London

Monet



Peking



after rain

before rain





Pollution

- Great London smog: December 1952 March 1953
- Several thousand fatality
- It was a kind of whistle blow









Extreme weather



storms



cold



desertification





Water shortage





Aral Sea





Raw material shortage

August 2010, Robert Friedland: We need more copper in the next 20 years than was mined in the last 110 years, those of us in the business don't have any idea where this metal is going to come from









Biodiversity reduction

- Hunting
- Destroying of habitats

 Extinction of species is a natural phenomenon but humans increased its rate





How much water is needed to produce a cup of coffee?



140 L of water (Chapagain and Hoekstra, 2007)





Coal power plans in China

- Total output: 1.95*10¹² kilowatt-hours / year (275 Paks)
- 2.38*10⁹ t / yr coal
 - more than USA, EU and Japán together
 - 13 people dies daily









Coal power plans in China

- In each 7-10 days a new coal power plant is built New York Times, 2006
- India also rely on coal more and more





The concept of sustainability





Definition of sustainability

United Nations, 1987 Brundtland report:

" Sustainable development is development that meets the needs of the present without compromising the ability of future generations to meet their own needs."





Why is sustainability important?

- United States Census Bureau: human population
 2.5 to 6.4 billion 1950-2005
- U.N. Development Program, increase in consumption expenditures 1970-95: Industrial nations 2x and developing nations 2.7X
- Photosynthetic world terrestrial net primary production: 38% used by humans (Running, S.W., 2012. Science, 337, pp. 1458-1459)
- Photosynthetic world primary production: 20% used by humans (Imhoff et al. 2004, Nature, 429)





Motivation



VS.

it ain't easy being green





Sustainability





Sustainability vs. Economy?

- Some says that sustainability and economy can not be reconciled
 - developing nations want to grow first and deal with sustainability later
- The two should be done parallel
- Sustainability map: display different solutions in terms of profit and sustainability

there is room to improve both





Sustainability map






Selection: Constraint on profit







Selection: Constraint on sustainability







Selection: Multi-objective







Selection: Single objective







P-graph framework





Sustainable supply-chain design via P-graph framework

Potential objective functions:

- profit
- ecological footprint
- exergy dissipation
- green net regional product
- ratio between renewable and total emergies

The P-graph framework:

- developed for process synthesis problems
- mathematically rigorous
- synthesize optimal and n-best networks





Building credible scenarios ...

Starting with **building** blocks...

- ... create comprehensive scenarios...
- ... that help decision makers!









Supply chain design as process synthesis



Building blocks







The P-graph framework

- Process systems engineering (PSE)
 - process design (flowsheeting)
 - process synthesis
 - process simulation (analysis)
 - process operation
 - scheduling
- The P-graph framework helps to address and solve process network synthesis problems





P-graph representation (Friedler and Fan, 1992)













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Axioms (S1) $P \subseteq m$ (S2) $x \in R \Leftrightarrow \forall x \in m, d^{-}(x) = 0$







(S1) $P \subseteq m$ (S2) $x \in R \Leftrightarrow \forall x \in m, d^{-}(x) = 0$

Axioms







Axioms (S1) $P \subseteq m$ (S2) $x \in R \Leftrightarrow \forall x \in m, d^{-}(x) = 0$ (S3)

 $O \subseteq O$







Axioms (S1) $P \subseteq m$ (S2) $x \in \mathbb{R} \Leftrightarrow \forall x \in m, d^{-}(x) = 0$ **(S3)** o ⊆ 0 (S4) $\forall y_0 \in o, \exists \text{ path } [y_0; y_1],$ where $y_1 \in P$







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Axioms (S1) $P \subseteq m$ (S2) $x \in \mathbb{R} \Leftrightarrow \forall x \in m, d^{-}(x) = 0$ **(S3)** o ⊆ 0 (S4) $\forall y_0 \in o, \exists \text{ path } [y_0; y_1],$ where $y_1 \in P$ **(S5)** $\forall x \in m, \exists (\alpha; \beta) \in o;$ $x \in \{\alpha \cup \beta\}$









P-graph algorithms

Maximal Structure Generator (MSG)

- maximal structure contains all potential solution structure
- it works in polynomial time

Solution Structures Generator (SSG)

- creates all the solutions one by one
- applicable for small problems

Accelerated Branch-and-Bound (ABB)

- locates the best or n-best optimal structure
- accelerates using the structural properties of P-graph





Process synthesis by P-graph framework







MINLP vs. P-graph framework

| | MINLP | P-graph framework |
|---|--|---|
| Problem given by | Variables, Constraints | Raw materials, products, operating units |
| Generation of the math. model | Manual | Automatic |
| Structural properties of process-networks | Hidden in the math. model | Exploited |
| Number of solutions | Single | Multiple |
| Handling special constraints | Can be incorporated to the math. model | May require modifications of the model generator and solver |





The metrics of sustainability





Sustainability Metrics

- Metric System Property

- Emergy ↔ Energy Resources
- Green Net Prod ↔ Economy
- Fisher Information ↔ System Order





Sustainable Process Index (SPI)

- SPI is a measure developed to evaluate the viability of processes under sustainable economic conditions
- The concept of the SPI is based on the assumption that in a truly sustainable society the basis of economy is the sustainable flow of solar exergy
- SPI evaluates the areas needed to provide the raw materials and energy demands and to accommodate by-product flows from a process in a sustainable way





The algorithm







Calculating the SPI







SPI results

Advantage for public transport



Area for fossil carbon Area for emissions to air Area for emissions to water

461



Country dependent SPI per kWh of electricity







Ecological Footprint of agricultural base products

SPI [m²a/kg]







Ecological Footprint of agricultural base products



High impacts because of tractors and fertilizers





Ecological Footprint agricultural machines and fertilizers



Industrial chemical production, energy provision and emission as main contributions to the Footprint for 1 kg of mineral fertilizer

Fuel consumption and emissions are mainly responsible for the impact of agricultural machines



SPI for Tractor (<70KW), normal workload



Huge differences

Fodder

466

Ecological Footprint of "higher valued" agricultural products

2 500



Fowl

Pig

which is "transferred" to the final meat product





Exergy: Available Energy

- Exergy: thermodynamic work (in Joules) that can be done by bringing energy or mass into equilibrium with environment
 - a cup of hot tea has more exergy on the north pole than in a desert
- Sustainability Criteria: minimize exergy losses during processing
 - $\Box dEx/dt \ge 0$







Emergy

Emergy: the sum of all different kinds of energy previously used (directly and indirectly) to make a product






Emergy: Energy Resources

Emergy: the energy resources (in solar joules) invested by the environment in an operation or in a product

Sustainability Criteria:

- \Box (total emergy of inputs) \rightarrow minimum
- \Box (renewable emergy use) / (total emergy use) \rightarrow 1





Exergy vs. Emergy: Corn vs. Beef



Source: Mayer, A.L., Thurston, H.W., Pawlowski, C.W., The Multidisciplinary Influence of Common Sustainability Indexes, Front. Ecol. Environ, 2, 419-426 (2004).





Ecological Footprint Basics

Land is categorized int
arable land
forest land
pasture land
sea
energy land
built land



blog.lib.umn.edu/tupp0008/environment/2008/02/





Ecological Footprint Basics

- Ecological Footprint (demand) = land area required to meet level of consumption and waste generation by the human population
- Biocapacity (supply) = land area available to support the human population





Ecological Footprint Basics

Assumptions:

- a can track of resources and waste generated
- resource and waste flows can be converted to land area

Sustainability Criteria:

biocapacity is larger than ecological footprint

■ B ≥ EF

- ecological footprint does not increase and biocapacity does not decrease
 - ▲EF ≤ 0 & B ≥ EF





Multi-period operating unit





P-graph representation



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P-graph representation

- Definition of an operating unit: specifies the flowrates and the cost if the relative size is one
- Relative size: a multiplication factor, how much time bigger operating unit is needed than the definition
 - decision variable
 - the flowrates and the proportional part of the cost has to be multiplied accordingly
- If the relative size is 0 then the operating unit does not appear in the solution
 - □ the fix cost is also 0





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Modeling total cost



 $x_1 = 10$ 4*10+20 = 60

 $x_1 = 10, x_2 = 20$ 4*10 + 1*20 = 60



Modeling total cost

- Old method: raw materials and operating units have associated cost
- New method: each operating unit consumes a new material termed mat_cost
 - the operating unit itself does not have cost
 - the cost of mat_cost is one





Modeling total cost

- Considering sustainability does not mean that cost is no longer an issue
- We may want to determine the best network in terms of footprint, but then cost can become a constraint
- A new material called, mat_cost, has to be introduced for the whole network
- A new operating, peeler_fix_cost_prod, unit and a new intermediate material, peeler_fix_cost, has to be introduced for each operating unit in the original network





Modeling total cost

- Old method: x = 10, cost = 4 * 10 + 20 = 60
- New method: x = 10
 - consumption of 40 unit from mat_cost
 - its price is also 40
 - 10 unit of the peeler_fix_cost is also needed
 - only peeler_fix_cost_prod can produce it, thus, this operating unit should be in the solution
 - if peeler_fix_cost_prod is in the solution then its relative size must be 20
 - it has to consume 20 unit from mat_cost
 - □ the cost is 60





Modeling of ecological footprint





Emergy, footprint representation







Emergy, footprint representation

- Ecological footprint and emergy are two sustainability metrics what we would like to incorporate into our model
- Both of these metrics are extensive
 - the footprint of a network can be calculated by summarizing the footprint of its components
- We would like to limit our search according to footprint, so the initial structure has to be transformed to impose this constraint





Emergy, footprint representation

- New material nodes termed as footprint and emergy are introduced
- These materials will be the inlet for each operating unit which represent some physical process
 - the new nodes have limits for maximum inlet flowrate
- If footprint belongs to a raw material then an operating unit is introduced to represent the purchase, and the footprint material will be the inlet of this unit





Ratio of renewable and fossil energy production







Ratio of renewable and fossil energy production

- We may search for solutions which are not worse than an already known solution in terms of the ratio of renewable and fossil energy production
 - for example, if our current design ensures the parity of renewable and fossil energy production, then we would not be satisfied with a solution where the ratio of the renewables is less than 50%
- A technique is proposed here to ensure this ratio
- The idea is to introduce material nodes: sum_renewable and sum_fossil to keep track the corresponding energy production





Ratio of renewable and fossil energy production

- These materials are connected through a new operating unit (force_ratio) which ensures the required constraint
 - if the parameter C is set to 1 then we can burn natural gas to create 1 MWh of energy only if the same amount is produced either from biogas or grass silage
- Material sum_renewable is produced when biogas is burned or when heat and electricity is produced from grass silage
- Material sum_fossil is consumed when natural gas is burned or when electricity is consumed from the grid
- It can happen that the ratio is worse than before because both type of energy production is reduced but the renewable production in larger volume





Illustrative example





Assumptions

- The ecological footprint of the supply chain is dominated by the feedstocks and inputs
- The emergy footprint of the supply chain is also dominated by the feedstocks and inputs
- Methodology must be simple enough for wide application
- Supply chain is designed to produce 7.2 TJ/year of electricity and 18 TJ/year of heat





Applied tools

- PNS-Draw: graphically depict P-graphs
- PNS-Studio: solve and export synthesis problems





Software: PNS-Draw







Software: PNS-Studio

€ FeladatModellje.pns - Pns Studio

File Synthesize Options Help

Problem Solutions E-Materia E Operating Units - Raw Materials E-Loading_L1 PC_in_Veszprem_depo input Materials PC_in_Szekesfehervar_depo PC_in_Veszprem_depo: 1 unit/payout period PC body - Output Materials - Electronics PC_in_truck_in_Veszprem: 1 unit/payout period <New> - Loading_L3 intermediates - Input Materials PC_in_truck_in_Szekesfehervar PC_produced_in_Szekesfehervar: 1 unit/payout period PC_in_truck_in_Balatonalmadi Output Materials PC_produced_in_Szekesfehervar PC_in_truck_in_Szekesfehervar: 1 unit/payout period PC_in_truck_in_Veszprem E Loading_L2 <New> - Input Materials Products PC_in_Szekesfehervar_depo: 1 unit/payout period PC_in_Balatonalmadi - Output Materials <New> PC_in_truck_in_Szekesfehervar: 1 unit/payout period E Transport_T2 input Materials PC_in_truck_in_Szekesfehervar: 1 unit/payout period - Output Materials PC_in_truck_in_Balatonalmadi: 1 unit/payout period Unload_U - Input Materials PC_in_truck_in_Balatonalmadi: 1 unit/payout period - Output Materials PC_in_Balatonalmadi: 1 unit/payout period Assembly_A E Input Materials PC_body: 1 unit/payout period Electronics: 1 unit/payout period - Output Materials PC_produced_in_Szekesfehervar: 1 unt/payout period Transport_T1

- Input Materials

- Output Materials

<New>

PC_in_truck_in_Veszprem: 1 unit/payout period

- PC_in_truck_in_Balatonalmadi: 1 unit/payout period

Name Name of the material. It must be unique in the problem definition. Convert values automatically Delete Update Cancel PC_in_truck_in_Szekesfehervar - Material properties Name PC_in_truck_in_Szekesfehervar Type intermediate Quantity type capacity Maximum available flow 100000000 unit/payout period Maximum flow Mu unit/payout period Description Description Name Name of the material. It must be unique in the problem definition. Convert values automatically Update Cancel Delete Name PC in Balatonalmadi product. Quantity type capacity Required flow 240 unit/payout period Required flow Mu unit/payout period Maximum flow 100000000 unit/payout period Maximum flow Mu unit/payout period Price 0 €/unit (default) Price Mu €/unit Description Description Name Name of the material. It must be unique in the problem

PC_in_Veszprem_depo - Material properties

PC_in_Veszprem_depo

0 unit/payout period (default)

raw material

unit/payout period

unit/payout period

capacity

232 €/unit

Description

€/unit

Maximum available flow 200 unit/payout period

Name

Type

Price Price Mu

definition.

Description

Quantity type

Required flow

Required flow Mu

Maximum flow Mu

| | 🖂 Basic | | - |
|---|--|--|------|
| 1 | Name | Loading_L1 | 1 |
| | Working hours per year | 8000 h/yr (default) | |
| L | Payout period | 10 yr/payout period (default) | |
| L | Capacity constraints | | |
| L | Capacity constraints | | |
| l | Lower bound | 0 (default) | 1 |
| L | Upper bound | 900 | |
| | Cost parameters | | |
| | E Operating cost | | - 11 |
| | Fixed charge | 20 C/yr | |
| | Fixed charge Mu | £/yr | -11 |
| | Proportionality constant | 0 €/payout period | |
| | Proportionality constant Mu | £/payout period | |
| | E investment cost | | |
| | rixed charge | 00 | |
| | Pixed charge Mu | 0.0 | |
| L | Proportionality constant | 06 | |
| L | Proportionality constant Mu | e | |
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| | Convert values automatical Update CC Transport T1 - Operating Unit prop Basic Name Working hours per year Payout period Capacity constraints Capacity constraints Lower bound Upper bound Cost parameters | ty ancel Delete enties Transport_T1 3000 h/yr (default) 10 yr/payout period (default) 0 (default) 900 | - |
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| | Convert values automatical Update CC Traceood_T1=Coercorg Unit prop Basic Name Working hours per year Payout period Capacity constraints Capacity constraints Lower bound Upper bound Upper bound Upper bound Coparating cost Food charge | ly ancel Delete etter Transport_T1 8000 h/yr (default) 10 yr/payout period (default) 0 (default) 900 18 £/yr | |
| | Convert values automatical Update CC Tentroot II - Occounty Unit pro- Name Working hours per year Payout period Capacity constraints Capacity constraints Lower bound Upper bound Cost parameters Operating cost Pixed charge Fixed charge Mu | ly ancel Delete otion Transport_T1 8000 h/yr (default) 10 yr/payout period (default) 0 (default) 900 18 £/yr £/yr | |
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Illustrative example

- An example is presented here to show the application of the P-graph framework while taking into account sustainability issues
- This graph represents the potential energy conversion technologies of a small region
 - conventional fossil energy sources are available like the natural gas and the electricity from the grid
 - this region has agricultural waste product in the form of grass and corn cobs, which can be used for biogas production





Illustrative example

- both the biogas and the natural gas can be fed to a furnace to produce heat
- there are available wood from which pellet and chips can be produced, and wood can be burned directly
- pellet also can be produced from corn cob





Data: Properties of the raw materials

| Name | Cost | | Max. flow | |
|-------------------|------|-------|--------------|-------|
| electricity_grid | 149 | €/MWh | | |
| natural_gas | 0.5 | €/m³ | | |
| area_corn | | | 300 | ha/yr |
| area_corn_silage | | | 400 | ha/yr |
| area_grass_silage | | | 1 200 | ha/yr |
| area_wood | | | 600 | ha/yr |





Data: Properties of the products

| Name | Min. | flow |
|---------------------|-------|--------|
| hot_utility | 5 000 | MWh/yr |
| electricity_utility | 2 000 | MWh/yr |





Data: The inputs and outputs of the operating units of the case study

| Unit name | Input | Rate | | Output | Rate | | |
|--------------------------|-------------------|-------|----------------|---------------------|------|----------------|--|
| electricity_feeder | electricity_grid | 1 | MWh | electricity | 1 | MWh | |
| biogas_plant | | | | biogas_plant_c | 8000 | h | |
| biogas_prod_corn | biogas_plant_c | 13 | h | biogas | 600 | m ³ | |
| | corn_silage | 1 | t | | | | |
| | electricity | 0.13 | MWh | | | | |
| biogas_prod_grass | biogas_plant_c | 12 | h | biogas | 550 | m ³ | |
| | grass_silage | 1 | t | | | | |
| | electricity | 0.13 | MWh | | | | |
| corn_silage_prod | area_corn_silage | 1 | ha | corn_silage | 12 | t | |
| grass_silage_prod | area_grass_silage | 1 | ha | grass_silage | 12 | t | |
| biogas_CHP_plant | | | | biogas_CHP_plant_c | 8000 | h | |
| biogas_CHP_corn | biogas_plan_c | 4 | h | electricity | 1 | MWh | |
| | corn_silage | 0.694 | t | heat | 0.65 | MWh | |
| biogas_CHP_grass | biogas_plant_c | 4 | h | electricity | 1 | MWh | |
| | grass_silage | 0.758 | t | heat | 0.65 | MWh | |
| electricity_utility_prod | electricity | 1 | MWh | electricity_utility | 1 | MWh | |
| gas_burner | | | | gas_burner_c | 8000 | h | |
| biogas_burning | gas_burner_c | 1 | h | heat | 0.85 | MWh | |
| | biogas | 153 | m ³ | | | | |
| natural_gas_burning | gas_burner_c | 1 | h | heat | 0.85 | MWh | |
| | natural_gas | 91.9 | m ³ | | | | |
| corn_prod | area_corn | 1 | ha | corn | 9 | t | |
| | | | | corn straw | 14 | t | |





Data: The inputs and outputs of the operating units of the case study

| Unit name | Input | Rate | | Output | Rate | |
|---------------------------|-------------------|------|-----|-------------------|------|-----|
| pelletizer | | | | pelletizer_c | 8000 | h |
| corn_straw_pellet_prod | electricity | 0.15 | MWh | corn_straw_pellet | 1 | t |
| | heat | 0.5 | MWh | | | |
| | pelletizer_c | 0.5 | h | | | |
| | corn_straw | 1 | t | | | |
| wood_pellet_prod | electricity | 0.1 | MWh | wood_pellet | 1 | t |
| | heat | 0.85 | MWh | | | |
| | pelletizer_c | 0.5 | h | | | |
| | wood | 1 | t | | | |
| wood_chips_prod | electricity | 0.03 | MWh | wood_chips | 1 | t |
| | heat | 0.48 | MWh | | | |
| | wood | 1 | t | | | |
| wood_prod | area_wood | 1 | ha | wood | 3 | t |
| feeder | | | | feeder_c | 8000 | h |
| burner | | | | burner_c | 8000 | h |
| corn_straw_pellet_burning | corn_straw_pellet | 0.25 | t | heat | 1 | MWh |
| | feeder_c | 4 | h | | | |
| | burner_c | 4 | h | | | |
| wood_pellet_burning | wood_pellet | 0.25 | t | heat | 1 | MWh |
| | feeder_c | 4 | h | | | |
| | burner_c | 4 | h | | | |
| wood_chips_burning | wood_chips | 0.25 | t | heat | 1 | MWh |
| | feeder_c | 4 | h | | | |
| | burner_c | 4 | h | | | |
| wood_burning | wood | 0.3 | t | heat | 1 | MWh |
| | burner_c | 4 | h | | | |
| hot_utility_prod | heat | 1 | MWh | heat_utility | 1 | MWh |





Data: The overall cost of the operating units of the case study

| Unit name | Fixed | Prop. part |
|---------------------|---------|------------|
| | part | [€/yr] |
| | [€/yr] | |
| electr_feeder | 0 | 0 |
| corn_silage_prod | 0 | 960 |
| grass_silage_prod | 0 | 960 |
| corn_prod | 0 | 960 |
| wood_prod | 0 | 180 |
| biogas_plant | 35 000 | 49 286 |
| biogas_CHP_plant | 131 236 | 81 298 |
| biogas_prod_corn | 3 680 | 10 |
| biogas_prod_grass | 3 680 | 10 |
| biogas_CHP_corn | 9 822 | 4 |
| biogas_CHP_grass | 9 822 | 4 |
| gas_burner | 1 000 | 2 000 |
| biogas_burning | 0 | 0 |
| natural gas burning | 0 | 0 |

| Unit name | Fixed | Prop. part |
|--------------------------|--------|------------|
| | part | [€/yr] |
| | [€/yr] | |
| burner | 15 578 | 15 692 |
| wood_burning | 7 347 | 4 |
| wood_chips_burning | 7 347 | 3 |
| wood_pellet_burning | 7 347 | 3 |
| corn_straw_pellet_burnin | 7 347 | 3 |
| g | | |
| hot_utility_prod | 0 | 0 |
| wood_chips_prod | 30 820 | 3 |
| wood_pellet_prod | 10 400 | 2 |
| corn_straw_pellet_prod | 10 400 | 2 |
| electricity_utility_prod | 0 | 0 |
| pelletizer | 30 000 | 185 000 |
| feeder | 100 | 0 |





Computational results





Optimal structure in terms of cost



Computational time: < 1 s



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Solution structures

| Structure | Heat demand satisfied | Electricity demand satisfied | Cost [€/yr] | Ecological footprint | Emergy |
|-----------|---|-------------------------------|----------------|-------------------------|-----------|
| #1 | wood | grid | 476,363 | 1046 | 1,764,910 |
| #2 | biogas CHP by corn silage, wood | biogas CHP by corn silage | 476,433 | 749 | 234,594 |
| #3 | biogas CHP by grass silage, wood | biogas CHP by grass silage | 486,852 | 840 | 532,100 |
| #4 | biogas CHP by corn silage, wood chips | biogas CHP by corn silage | 521,283 | 796 | 245,744 |
| | | | | | |
| #13 | natural gas | grid | 572,956 | 690 | 2,706,600 |



Results




Raw Material & Energy Inputs

| Solution | Raw materials | | | | | | |
|-------------|-----------------------------|------------------------|----------------------|-----------------------------|------------------------------|----------------------|--|
| structures | electricity_grid [TJ/yr] | natural_gas [m³∕yr] | area_corn [ha/yr] | area_corn_silage [ha/yr] | area_grass_silage [ha/yr] | area_wood [ha/yr] | |
| Structure1 | 7.37 | | | | | 500.00 | |
| Structure2 | | | | 117.69 | | 367.73 | |
| Structure3 | | | | | 128.54 | 367.73 | |
| Structure4 | | | | 120.03 | | 393.66 | |
| Structure5 | 7.57 | | | | | 539.13 | |
| Structure6 | | | | | 131.10 | 393.66 | |
| Structure7 | | 399,272.00 | | 116.30 | | | |
| Structure8 | | | 72.96 | 126.77 | | | |
| Structure9 | | | | 124.78 | | 380.69 | |
| Structure10 | | 399,272.00 | | | 127.02 | | |
| Structure11 | | | 72.96 | | 138.46 | | |
| Structure12 | | | | | 136.29 | 380.69 | |
| Structure13 | 7.25 | 540,588.00 | | | | | |
| Structure14 | 7.99 | | | | | 529.10 | |
| Structure15 | 8.17 | | 102.04 | | | | |
| Structure16 | | | | 214.45 | | | |
| Structure17 | | | | 125.12 | 98.01 | | |
| Structure18 | | | | 90.05 | 135.88 | | |
| Structure19 | | | | | 234.67 | | |
| Structure20 | 7.95 | | | 125.00 | | | |
| Structure21 | 8.02 | | | | 136.36 | A | |



Computational results

- Multi-objective optimization usually has no clear winner
- Structure 1 has greater footprint than the base case (structure 13)
- Structure 2 is much better in terms of both ecological footprint and emergy and the cost is only slightly higher than the cost of Structure 1
- Structure 7 and 10 are better than the base case in emergy, ecological footprint, and cost as well
- Structure 16 is more expensive than the base case but there is a substantial drop in footprint here.
- Structure 22 and 23 produces more heat and electricity than required





Structure #13: Natural Gas & Electricity from the "Grid"





Structure #7: Corn Silage & Natural Gas





Structure #10: Grass Silage & Natural Gas





Structure #16: Corn Silage





Supply Chain Structures







Summary

- Environmental protection
- The concept of sustainability
- P-graph framework
- The metrics of sustainability
- Multi-period operating unit
- Modeling of ecological footprint
- Illustrative example
- Computational results







Conclusions

- Sustainability is about adaptively managing the environment on an on-going basis so as to insure that the Earth can continue to support human existence for the indefinite future
- Carefully designed supply chains can be made both cheaper and significantly more environmentally friendly than current practice while meeting societal needs











A felsőfokú informatikai oktatás minőségének fejlesztése, modernizációja

TÁMOP-4.1.2.A/1-11/1-2011-0104



Főkedvezményezett: **Pannon Egyetem** 8200 Veszprém

vezményezett: Szegedi Tudományegyetem 6720 Szeged Dugonics tér 13. Kedvezményezett:









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Thank you for your attention!



Additional information: www.p-graph.com



Multiobjective PNS problems



Multiobjective optimization

- In multiobjective optimization more than one goals should be taken into account.
- Unfortunately it often happens that some solutions which have excellent performance in one objective have very week performance in the others.





Applications in case of PNS

Usually in process network synthesis we are looking for a cheapest solution, but other objectives can be important as well:

- One of the most important goals is to decrease the pollution of environment. Cleaner technologies are often more expensive therefore in these cases the objectives are very different.
- One can consider the execution time of the process as a second objective function. It is not sure that the faster execution is also a cheaper one.
- The stability of the production can be also a further objective.





The approaches to solve multiobjective problems

There are several methods to study multiobjective problems, we will overview the following ones

- Determining Pareto optimal or weakly efficient solutions
- Using aggregating functions to form a singleobjective model
- Using Epsilon-Constraint method





Notations

- In general we suppose that we have k minimization functions denoted by f_1, f_2, \ldots, f_k . Note that it is not a restriction to consider minimization functions since taking the negative the maximization problem can be changed into a minimization one.
- The set of feasible solutions is denoted by S.
- In case of the PNS applications we will consider only two objective functions, the methods can be extended into the more general cases with some extra technical difficulties.





Notations in case of multiobjective PNS_i

- We mainly will consider the structural model, where an operating unit o_i has only fixed costs, denoted by cf_i and df_i . Then we have two objective functions: z_1 is the sum of the cf_i and z_2 is the sum of the df_i values of the selected operating units.
- We will also consider the more general fix charged linear cost model. Here the proportionality constants cp_i and dp_i are also assigned to the operating units, and z₁ is calculated by cf_i and cp_i and z₂ is calculated by df_i and dp_i.





Weakly efficient solutions

- We can say that a solution $x \in S$ is better than a solution $y \in S$ if it is better in each objective, which means that $f_i(x) < f_i(y)$ for each *i*.
- The solutions which are the best ones on this sense are called weakly efficient solutions.
- Formally we can say that a solution $x \in S$ is weakly efficient if there is no $y \in S$ such that f_i $(y) < f_i(x)$ is valid for each *i*.





Pareto optimal solutions

- On the other hand we can also say that a solution $x \in S$ is better than a solution $y \in S$ if it is better in at least one objective and not worse in the others.
- The solutions which are the best ones on this sense are called Pareto optimal solutions.
- Formally, a solution $x \in S$ is Pareto optimal if there are no $y \in S$ and j such that $f_i(y) \le f_i(x)$ is valid for each i and $f_j(y) < f_j(x)$.





Aggregated objective function

- Let g be a k-variable monoton function which is called the aggregation function.
- Then we can form the single-objective optimization problem where we are looking for the $x \in S$ where $g(f_1(x), f_2(x), \dots, f_k(x))$ is minimal.
- Usually g is a weighted sum with positive weights but more general functions can also be used.

Theorem: If g is a weighted sum with positive weigths then any optimal solution of the single objective aggregated problem is a Pareto optimal solution of the original one.





Proof

We use an indirect proof:

- Let x be an optimal solution of the aggregated problem and suppose that it is not Pareto optimal.
- Then we have an $y \in S$ such that $f_i(y) \le f_i(x)$ is valid for each *i* and there is a *j* with $f_i(y) < f_i(x)$.
- Since g is a weighted sum of f_i substituting x and y into g we obtain that g(y)<g(x) which is a contradiction.





Epsilon-constrained method

■ In the epsilon constrained method we have one distinguished objective function (suppose it is f_1) and the other objective functions are used to constrain the set of feasible solutions. In the model the bounds C_2 , C_3 ,..., C_k are given and we consider only the solutions $x \in S$ which satisfy $f_i(x) \leq C_i$ for i=2,...,k.

Theorem: An optimal solution of any singleobjective optimization problem received by the epsilon-constrained method is a weakly efficient solution of the original problem.





Proof

- Let x be an optimal solution of the aggregated problem and suppose that it is not weakly efficient.
- This means that there exists $y \in S$ such that
- $f_i(y) < f_i(x)$ is valid for each *i*.
- Then y is a feasible solution of the constrained problem, since by $f_i(y) < f_i(x) \le C_i$ for i=2,...,k.
- Then we obtain a contradiction by $f_1(y) < f_1(x)$.





Robust optimization

- In the optimizaton problems we often suppose that all costs are known exactly in advance. On the other hand, in real applications usually some uncertainty can change the data.
- In general, for most optimization model the problem of uncertainty is solved by stochastic optimization. On the other hand, in these cases we need some a priori information about the distribution of the data, which is usually not available in real applications.
- Another approach is a robust optimization, where the uncertainty is handled by deterministic worst case scenario. In these models we do not have the fixed values of the parameters we only know that they are in a given interval.





SSG based generation of Pareto optimal PNS solutions in structural PNS problems

- In the structural model the cost of a solution depends only on the operating units contained in it, therefore the SSG algorithm which lists all of the feasible solutions can be extended to determine the Pareto optimal ones.
- We have to use a candidate set *J* and in each step when a new solution is found we upgrade this set.
- If the solution is worse than some elements of J, then J is not changed.
- Otherwise the actual solution is put into J and those earlier elements of J which are worse are deleted.





Example

- Consider the problem shown in the next figure where 6 operating units o_1, o_2, \dots, o_6 are defined.
- The cost are given as follows:

| | 1 | 2 | 3 | 4 | 5 | 6 |
|----|---|---|---|---|---|---|
| cf | 3 | 1 | 2 | 9 | 6 | 3 |
| df | 2 | 3 | 2 | 8 | 2 | 6 |





The maximal structure of the example







The Pareto optimal solutions received by extended SSG

- The SSG algorithm lists all of the solutions. The first is $x_1 = \{O_1, O_4\}$ with $z_1(x_1) = 12$ and $z_2(x_1) = 10$ and we put it into the candidate list *J*.
- The second solution is $x_2 = \{o_2, o_4\}$ with $z_1(x_2) = 10$ and $z_2(x_2) = 11$, it is not worse than x_1 thus we put it into the candidate list J.
- The third solution is $x_3 = \{o_1 o_2 o_4\}$ with $z_1(x_3) = 13$ and $z_2(x_3) = 14$, it is worse than x_1 thus we do not put it into the candidate list *J*.
- The next solution is $x_4 = \{o_1, o_3, o_5\}$ with $z_1(x_4) = 11$ and $z_2(x_4) = 6$, it is better than x_1 and not worse than x_2 thus we put it into the candidate list *J*, and x_1 is deleted.





The Pareto optimal solutions received by extended SSG

- The next solution is $x_5 = \{o_2 \ o_3 \ o_5\}$ with $z_1(x_5) = 9$ and $z_2(x_5) = 7$, it is better than x_2 and not worse than x_4 thus we put it into the candidate list J, and x_2 is deleted.
- The next solution is $x_6 = \{o_1, o_2, o_3, o_5\}$ with $z_1(x_6) = 12$ and $z_2(x_6) = 9$, it is worse than x_5 thus we do not put it into the candidate list *J*.
- The next solution is $x_7 = \{o_3, o_6\}$ with $z_1(x_5) = 5$ and $z_2(x_5) = 8$, which is neither worse nor better than x_4 and x_5 thus we put it into J.
- All of the remaining 13 solutions are worse than one of the elements of *J*, thus the set of the Pareto optimal solutions is $\{x_{4,}x_{5,}, x_{7}\}$





Branch and bound based generation of Pareto optimal PNS solutions in structural PNS problems

- Usually a PNS problem has a lot of feasible solution and only a few of them are Pareto optimal. Therefore an algorithm which does not generate all of the feasible solutions can be more effective.
- We can also extend the Branch and Bound based ABB algorithm to generate Pareto optimal solutions.
- In this case we can exclude the sets of the feasible solutions where we know by the bounding functions that all solutions are worse then one of the elements in J.





Extension to the fix charged linear cost model

- In the structural model we have only a finite number of feasible solutions. In the more general version the material flows are alos considered, thus we have an infinite set of solutions.
- On the other hand we again have only finite number of structures which can be generated by SSG. Thus the problem is reduced to find the Pareto optimal solutions in case of fixed structures.
- This means that we have to solve a multiobjective linear programming problem which is widely studied.





Linear aggregated cost functions

- If there is a linear aggregation function then we can reduce the problem to the solution of a PNS problem.
- If the the aggregated function $z(x) = r_1 z_1(x) + r_2 z_2(x)$ then we can define the following PNS problem with the same set of operating units.
- For operating unit o_i the fix cost will be $ef_i = r_1 cf_i + r_2 df_i$ and the propotionality cost will be $ep_i = r_1 cp_i + r_2 dp_i$.
- Then the cost of a feasible solution of this new PNS problem will be the aggregated cost of the original problem.





Example

• Consider the problem shown in the next figure where 6 operating units o_1, o_2, \ldots, o_k are defined.

The cost are given as follows:

| | 1 | 2 | 3 | 4 | 5 | 6 |
|----|---|---|---|---|---|---|
| cf | 6 | 3 | 1 | 9 | 5 | 3 |
| df | 2 | 4 | 7 | 4 | 5 | 7 |





The maximal structure of the example






The aggregated optimal solutions

- We have three solutions such that any further solution contains some of them: $x_1 = \{o_1, o_4\}$ with $z_1(x_1) = 15$ and $z_2(x_1) = 6$, $x_2 = \{o_2, o_5\}$ with $z_1(x_2) = 8$ and $z_2(x_2) = 9$, $x_3 = \{o_3, o_6\}$ with $z_1(x_3) = 4$ and $z_2(x_3) = 14$.
- If we consider z_1 then x_3 is optimal.
- If we consider z_2 then x_1 is optimal.
- If we consider the aggregated objective $z=z_1+z_2$, then x_2 is optimal.
- We note that this also shows that all of these solutions are Pareto optimal.





Nonlinear aggregating functions

- If we use more difficult aggregation functions then the problem can not be reduced into a single obective PNS problem.
- In these cases we can extend the ABB algorithm into a version which can solve the problem. The set of the feasible solutions is independent on the objective function therefore we only have to define new bounding functions.
- The simplest way to define a new bound is to use the bounds given on the objectives z_1 and z_2 . If at some point we have bounds L_1 and L_2 on a set of feasible solutions, then $g(L_1, L_2)$ will bound the aggregated function on this set.





Nonlinear aggregating functions(2)

- On the other hand handling the objectives separately can yield weak bounds as the following example shows.
- Suppose we consider the set which contains three solutions: x_1 with $z_1(x_1)=12$ and $z_2(x_1)=40$, x_2 with $z_1(x_2)=25$ and $z_2(x_2)=25$, x_3 with $z_1(x_3)=35$ and $z_2(x_3)=15$. And let $g(x,y)=x^2+y^2$.
- Then the best bound on z_1 is 12, the best bound on z_2 is 15, thus using the bounds separately we cannot obtain better bound than 369 on the aggregated function. On the other hand the minimal value of the aggregated objective is 1250.





Epsilon-constrained method

- In this version the set of the feasible solutions and also the optimal solution are changing as the bounds are changed. Consider the example used in the aggregated problem.
- If $C_2=14$, then x_1, x_2, x_3 are all feasible thus x_3 is the optimal solution with $z_1(x_3)=4$.
- If we use $C_2=9$, then x_3 is excluded thus x_2 will be the optimal solution with $z_1(x_2)=8$.
- Finally, if we use $C_2=6$, then x_2 is also excluded thus x_1 will be the optimal solution with $z_1(x_1)=15$.





Branch and bound based approach

- In this model the objective is z₁ but the set of feasible solutions is changed, therefore we have to extend to ABB algorithm to handle this restricted sets of feasible solutions.
- One basic idea is to use the bounding function on z_2 to exclude some subset of solutions.
- If for a set of feasible solutions using the bounding function for z_2 we obtain that z_2 is at greater than C_2 for all of these solutions then we can exclude this set.





Robust PNS model

- In the robust model each operating unit o_i has an extended cost $c(o_i) + e(o_i)$. We will call $c(o_i)$ the nominal cost and $e(o_i)$ the extra cost of the operating unit.
- We have an a priori bound b, which means that b operating units can have the extended cost and the others have the nominal cost.
- We are interested in the worst case, therefore, if we consider a feasible solution of the problem in the robust version its cost will be the sum of the nominal costs of the operating units plus the sum of the *b* largest extra costs.





Example

- Consider the PNS problem of the next figure where there are three operating units: o_1 with $c(o_1)=5$, $e(o_1)=2$, o_2 with $c(o_2)=2$, $e(o_2)=2$ and o_3 with $c(o_3)=2$, $e(o_3)=2$.
- If we consider the standard problem then the optimal solution contains o_2 and o_3 and the optimal cost is 4.
- If we consider the robust version with b=1, then the optimal solution still contains o_2 and o_3 and the optimal cost is 6.
- But if we consider the robust version with b=2, then the optimal solution contains o_1 and and the optimal cost is 7.





The maximal structure of the example







Branch and bound based algorithm

- The set of feasible solution is the same as in the standard PNS problem therefore we have to extend the bounding function.
- The simplest function contains the total nominal cost of the selected operating units plus the sum of the b greatest extra costs among them.
- We receive a more difficult function if we increase this simplest one by the shortest path from the raw materials into the selected operating units, where the cost of a path is the sum of the nominal costs of the operating units contained in it.





Heuristic algorithm for the structural model

- Both the SSG and ABB algorithms have exponential running time in the worst case, therefore some huge problems migh not be solved by them.
- In these cases heuristic algorithms which produce a good feasible solution in a short time can be useful.
- Moreover, these algorithms can be also used to accelerate the branch and bound algorithms giving a good starting solution which increases the efficiency of excluding subsets.





ASUM and AMAX heuristics(1)

- These greedy type algorithm use estimations on the cummulated costs of the materials (MA) and operating units (OP).
- The algorithms builds a solution step by step adding every time an operating unit to the solution.
- For each operating unit it calculates the sum of the estimated production cost of the input materials and the estimated cost of the operating unit. This sum is divided by the number of desired materials produced by the operating unit. The algorithm chooses the operating unit where this ratio is minimal.





ASUM and AMAX heuristics(2)

- At the beginning the set of desired material is the set of the desired products. Later in each step the input materials of the selected operating unit is put into this set and its output materials are deleted.
- The difference in the heuristics is in calculating the estimated costs of the input materials. ASUM takes the sum of the MA values, AMAX consider the maximum of the MA values.
- Checking the axioms S1 to S5 one can prove easily that the heuristics give a feasible solution for every function MA and OP.





OP function

- In the estimation of the cost of the operating unit we have to face with the problem of robustness, we do not know whether the nominal or the extended cost will be used in the solution. We can use the following solutions.
- Weighted cost: In this case we use some weighted average of the two costs thus $OP(o_i) = \alpha c(o_i) + (1 \alpha)(c(o_i) + e(o_i))$ for some $0 \le \alpha \le 1$.
- Worst case cost: In this case we use the extended cost unless we already selected b operating units with at least as big extra cost as the actual unit has. In the latter case we use the nominal cost.
- Hibrid cost: we use the weighted cost in the first case instead of the worst case.





MA function

- The estimated cost of the materials depends on the cost of the operating units, thus we will use here the weighted cost of the operating units.
- We use the function which was used to calculate lower bound in some branch and bound algorithm changing the cost of the operating unit into the estimation.
- The general definition of this cost function is very difficult therefore we will only define it for cycle free PNS problems below.





MA function in cycle free P-graphs

- We will use two sets of materials / denotes the materials with the given MA values and J denotes the complement set where we have to calculate the value of MA. At the beginning / contains the raw materials with MA(m)=0, and later in each step one element is moved from J to I.
- We always choose such a material *m* from *J* which is only produced by operating units having input materials in *I*.
- We calculate a production cost c for each such operating unit producing m as follows.





MA function in cycle free P-graphs

- Calculate the sum of the maximum of the MA values of the input materials and the weighted OP cost of the operating unit. (Note that by the definition of m we know that MA is known for all inut materials.)
- Let MA(m) be the minimum of the production costs calculated above for the operating units producing m. We move m from J to I.
- The procedure ends when J becomes empty which means that MA is calculated for all materials.





Robust extension of the fix charged linear cost model

- We can define in two ways the robust extension of the fix charged linear cost model.
- If we use robustness only in the fix costs then we can extend the ABB algorithm in the same way as in the structural model changing only the bounding function.
- If we define robustness also in the proportionality constants, then we have to solve robust linear programming problems in the bounding function of the branch and bound algorithm.





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Solving standard optimization problems with the P-graph framework



Goals

- Introduction of modelling techniques of the Pgraph framework for problems featuring properties different from those of the original chemical process planning area.
- The standard optimization problems do appear seldomly in their original form in real life. In most of the cases, practical problems include other parameters and constraints, that are difficult to implement in the dedicated algorithms. In contrast, the models presented here can be extended more easily for additional problem paramaters.





Considered problems

- Minimal spanning tree
- Shortest path
- Maximal flow
- Transportation problem





Finding the minimal spanning tree

- Given is a weighted graph $G=(V, \mathcal{E}, w)$, where
 - V is the set of vertices
 - ${\ensuremath{\mathcal{E}}}$ is the set of edges (an edge is a set of two vertices)
 - $W: \mathcal{E} \rightarrow \mathbb{R}$ is a weight function for the edges
- The objective is to find a subgraph $G' \subseteq G$ such that
 - G' is a tree
 - The sum of the weights of the edges in G' is minimal
- The problem can be solved to optimality efficiently by using the algorithms of Prim or Kruskal





Finding the minimal spanning tree with the P-graph framework

- Modelling
 - Materials correspond to vertices of the original graph
 - To a dedicated vertex, v^* a raw material is assigned. All the other materials are of product type.
 - The maximal amount of the used v^* is |V|-1,
 - For all the other materials (products), the required quantity is 1.
 - Prices, costs are not assigned to any of the materials.
 - Operating units correspond to the edges of the graph
 - For all {v,v'} edge, two operating units are assigned: ({v},{v'}) and ({v'},{v})
 - The fix cost is given by the weight of the edge: $w(\{v, v'\})$
 - Propotional costs and capacity limits are not introduced.





Finding the minimal spanning tree with the P-graph framework, cont'd

| | = | \overline{V} |
|-----------|---|---|
| R | = | $\{v^*\}$, where v^* is arbitrary chosen from V |
| I | = | Ø |
| P | = | $V \setminus \{v^*\}$ |
| 0 | = | $\{(\{v_1\},\{v_2\}) \{v_1,v_2\}\in\mathcal{E}\}$ |
| min_m | _ | $\begin{cases} V - 1 & m = v^* \\ 1 & \text{otherwise} \end{cases}$ |
| max_m | = | $\begin{cases} V - 1 & m = v^* \\ 1 & \text{otherwise} \end{cases}$ |
| cap_o | = | ∞ for all $o \in O$ |
| fix_o | = | $w(\{v_1, v_2\})$, where $o = (\{v_1\}, \{v_2\})$ |
| $prop_o$ | = | 0 for all $o \in O$ |
| $price_m$ | = | 0 for all $m \in M$ |

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Finding the minimal spanning tree Example







Finding the minimal spanning tree P-graph model for the example







Finding the minimal spanning tree Solution given by the ABB algorithm for the P-graph representation







Finding the minimal spanning tree Solution of the example based on the optimal PNS structure







Finding the shortest path

- Given is a weighted directed graph D=(V,A,w), a source vertex *s*, and a destination vertex *d*, where
 - V is the set of vertices
 - $A \subseteq V \times V$ is the set of arcs
 - $W: A \rightarrow \mathbb{R}$ is a weight function for the arcs
- The objective is to find a path from s to d with minimal weight sum
- The problem can be solved to optimality efficiently by using the algorithm of Dijkstra.





Finding the shortest path with the P-graph framework

- Modelling
 - Materials correspond to the vertices of the graph
 - The source vertex s is assigned with a raw material
 - The destination vertex *d* belongs to a product
 - All the other vertices are represented by an intermediate
 - The consumed amount from s, and the required quantity from d is 1, while it is forbidden to remain any amount of the intermediates
 - Prices, costs are not introduced for the materials.
 - Operating units correspond to the arcs
 - For each arc (v,v'), an operating unit $(\{v\},\{v'\})$ is introduced
 - The fix cost is the weight of the arc, w((v,v'))
 - Proportional cost are not introduced, and the capacity limit is 1 for all of the units.





Finding the shortest path with the P-graph framework cont'd

| M | = | \overline{V} |
|-----------|---|--|
| R | = | $\{s\}$ |
| I | = | $V \setminus \{s, d\}$ |
| P | = | $\{d\}$ |
| 0 | = | $\{(\{v_1\},\{v_2\}) \{v_1,v_2\}\in A\}$ |
| min_m | _ | $\left\{ egin{array}{ccc} 1 & m=s,d \ 0 & 	ext{otherwise} \end{array} ight.$ |
| max_m | = | $\left\{ \begin{array}{ll} 1 & m = s, d \\ 0 & \text{otherwise} \end{array} \right.$ |
| cap_o | = | 1 for all $o \in O$ |
| fixo | = | $w((v_1, v_2))$, where $o = (\{v_1\}, \{v_2\})$ |
| $prop_o$ | = | 0 for all $o \in O$ |
| $price_m$ | = | 0 for all $m \in M$ - |

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Finding maximal flow

- Given is a weighted directed graph D=(V,A,w), a source vertex s, and a destination vertex d, where
 - *V* is the set of vertices
 - $A \subseteq V \times V$ is the set of arcs
 - $W: A \to \mathbb{R}$ is a weight function for the arcs.
- The objective is to find a wight function w' such that
 - $W'(a) \le w(a)$ holds for all of the arcs
 - . The Kirchoff junction law is satisfied for all vertices except s and d
 - The overall weight of the arcs leading from s is maximal
- The problem can be solved to optimality efficiently by the algorithms of Ford & Fulkerson





Finding the maximal flow with the P-graph framework

- Modelling
 - Materials correspond to the vertices of the graph
 - The source vertex s is assigned with a raw material
 - The destination vertex *d* belongs to a product
 - All the other vertices are represented by an intermediate
 - Minimal and maximal limits are not introduced for the materials
 - The price of the product is 1, the other materials does not have a price, cost or penalty assigned.
 - Operating units correspond to the arcs
 - For all (v, v') arc an operating unit $(\{v\}, \{v'\})$ is assigned.
 - The capacity limit is the weight of the arc, i. e., w((v,v'))
 - Proportional and fixed costs are not introduced.





Finding the maximal flow with the P-graph framework cont'd

| M | = | V |
|--------------|---|--|
| R | = | $\{s\}$ |
| | = | $V \setminus \{s, d\}$ |
| P | = | $\{d\}$ |
| 0 | = | $\{(\{v_1\}, \{v_2\}) \{v_1, v_2\} \in A\}$ |
| min_m | = | 0 minden $m \in M$ |
| max_m | _ | $\left\{ egin{array}{ccc} \infty & m=s,d \ 0 & 	ext{otherwise} \end{array} ight.$ |
| cap_o | = | $w((v_1, v_2))$, where $o = (\{v_1\}, \{v_2\})$ |
| $\int fix_o$ | = | 0 for all $o \in O$ |
| $prop_o$ | = | 0 for all $o \in O$ |
| $price_m$ | = | $\begin{cases} 1 & m = d \\ 0 & \text{otherwise} \end{cases}$ |

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Transportation problem

- Given are a set of supply sources *S* and destinations *D*, moreover:
 - For all $s \in S$ source, a produced amount of a product is given
 - For all $d \in D$ destination, a demand for the amount of the product is given
 - For each *s*,*d* pair, the proportional transportation cost is given
- The objective is to find a weight function -representing the transportation amounts for the complete bipartite graph with partitions S and D such that
 - For all source $s \in S$ the aggregated weight of the adjacent edges does not exceed the produced amount.
 - For all $d \in D$ destination, the aggregated weight of the adjacent edges reach the demand
 - The wighted sum of the transportations costs is minimal
- The problem can efficiently be solved to optimality by the simplex algorithm





Solving the transportation problem with the P-graph framework

- Modelling
 - Materials correspond to sources and destinations
 - For all source $s \in S$ a raw material is assigned
 - For all destination $d \in D$ a product is assigned
 - The maximal limit for the raw material of each $s \in S$ is the production limit of s
 - The lower bound for the amount of the product for each $d \in D$ is the required amount of d
 - Prices and costs are not defined for the materials.
 - Operating units correspond to the transportation routes
 - For all $s \in S$ and $d \in D$ an operating unit ({s},{d}) is assigned
 - The proportional cost of the units is the proportional transportation cost between s and d
 - Capacity limits and fixed costs are not introduced.




Solving the transportation problem with the P-graph framework

| M | = | $S \cup D$ |
|------------|---|---|
| R | = | S |
| I | = | Ø |
| P | = | D |
| 0 | = | $\{(\{s\},\{d\}) s\in S, d\in D\}$ |
| min_m | = | $\begin{cases} dem_m & m \in D\\ \infty & \text{otherwise} \end{cases}$ |
| \max_{m} | = | $\begin{cases} supp_m & m \in S \\ \infty & \text{otherwise} \end{cases}$ |
| cap_o | = | ∞ for all $o \in O$ |
| fix_o | = | 0 for all $o \in O$ |
| $prop_o$ | = | $cost_{s,d}$ where $o = (\{s\}, \{d\})$ |
| $price_m$ | = | 0 for all $m \in M$ |





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Modelling of production systems

Integration



Introduction

- Heat integration
- Integration of PNS and scheduling





Heat integration





Introduction

The process contains heat stream

Cold streams need heating
Hot streams need cooling

The cost consists of

Operating units cost
Raw materials cost
Heat exchanges cost





Heat exchanger network (HEN)

- The heating and cooling duties can be satisfied by
 - Hot or cold utilities
 - For example steam or water which have cost
 - Other heat stream
- Heat exchanger unit is necessary
 - Cost of heat exchange





Input of HEN

- The set of hot streams (F^H)
- The set of cold streams (F^C)
- The rate and the heat capacity of materials streams
- The set of heat sources (U^H) and heat sinks (U^H) , their temperatures and costs
- The cost of heat exchangers





Heat stream of a material

- A material stream can have temperatures
- If the temperature of a material is different on different operating unit, it needs heat exchange
- The rate of enthalpy flow is proportional with the flow rate of the material





Latent heat

- An operating unit needs heating or cooling to remain its temperature constant
- The latent heat has temperature and rate of enthalpy flow
- An operating unit can have multiple latent heats
 - A part of the operating unit has cooling duty an other part has heating duty





hP-graph

- The hP-graph contains both operating and heat-exchanger units
- The node for a heat-exchanger unit for heating is indicating by a bar with solid lower half

For cooling, by a bar with a solid upper half

When an operating unit has latent heat, the node for it is extended by an appropriate heatexchanger unit





hP-graph









Extension of material nodes

- Heat streams with different temperatures cannot mixed
- In hP-graph each operating unit has it own material node
- Material flows are represented by fictive operating units or heat exchangers





Extension of a material node



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Temperatures

- Let t_{ij}^{in} and t_{ij}^{out} denotes the input and the output temperature of material m_i for operating unit o_j , respectively
- Let l_j denotes the number of latent heats of operating unit o_j
- Let h_{ij} denotes the rate of latent heat i of operating unit o_j

 $h_{ij} > 0$ if the operating unit releases heat

 $h_{ij} < 0$ if the operating unit absorbs heat

• Let TM_{ij} denotes the temperature of the latent heat





Heat streams

- A material stream can be denoted by a triple (i, j, k)
 - \Box The material (m_i)
 - \Box The operating unit producing it (o_j)
 - \Box The operating unit consuming it (o_k)
- A heat stream is such a material stream which has temperature parameters for both operating units





Heat streams

The set of hot streams $\mathbf{F}^{H} = \{(i, j, k): t_{i,i}^{out} > t_{i,k}^{in}, m_{i} \in \mathcal{M}, o_{i} \in \varphi^{-}(m_{i}), o_{k}\}$ $\in \varphi^+(m_i) \} = \{FH_1, FH_2, \dots, FH_{n_{FH}}\}$ The set of cold streams $F^{C} = \{(i, j, k): t_{ii}^{out} < t_{ik}^{in}, m_{i} \in \mathcal{M}, o_{j} \in \varphi^{-}(m_{i}), o_{k}\}$ $\in \varphi^+(m_i) \} = \{FC_1, FC_2, \dots, FC_{n_{FC}}\}$ • For simplicity let $t_{0,\ldots}^{(i,j,k)}$ and $t_{1,\ldots}^{(i,j,k)}$ denotes t_{ij}^{out} and t_{ii}^{in} such that $t_0^{(i,j,k)} < t_1^{(i,j,k)}$





Latent heat

- A latent heat can be denoted by a pair (i, j)
 - The operating unit (o_j)
 - The number of the latent heat $(i = 0, 1, ..., l_j)$
- Set of cold heat sources

$$\mathbf{L}^{H} = \left\{ (j, i) : h_{ji} > 0, o_{j} \in \mathcal{O}, i \in \{1, ..., l_{j}\} \right\} = \left\{ LH_{1}, LH_{2}, ..., LH_{n_{LH}} \right\}$$

- Set of hot heat sources
- $\mathbf{L}^{C} = \left\{ (j, i) : h_{ji} < 0, o_{j} \in \mathcal{O}, i \in \{1, 2, \dots, l_{j}\} \right\} = \left\{ LC_{1}, LC_{2}, \dots LC_{n_{LC}} \right\}$
- Let $t^{(i,j)}$ denotes the temperature of the latent heat (i,j)





Heat exchange

- Two heat streams, or a heat stream and a heat source, or two heat sources can exchange heat if their temperature intervals has common part
- A part is enough because a heat stream or a heat source can exchange heat several times with different heat streams and heat sources





Inherent temperature intervals

- Inherent temperature intervals are the narrowest intervals on which heat exchange can occur
- Sorting all temperatures in increasing order
 - If more heat stream or heat source have the same temperature it presents only once in the list
 - $\Box t_1, t_2, \dots, t_{n_e+1}$, where if i < j then $t_i < t_j$
- $E_p = [t_p, t_{p+1}], p \in \{1, ..., n_e\}$ are the inherent temperature intervals





Inherent streams

- All heat streams are divided into inherent streams according to the inherent temperature intervals
- Hot inherent streams

$$\begin{split} \mathbf{L}^{H} &= \{(i, j, k, p): (i, j, k) \in \mathbf{F}^{H}, t_{p} \geq t_{0}^{(i, j, k)}, t_{p+1} \\ &\leq t_{1}^{(i, j, k)}, p \in \{1, \dots, n_{e}\}\} = \{FSH_{1}, FSH_{2}, \dots FSH_{n_{FSH}}\} \end{split}$$

Cold inherent streams

$$L^{C} = \{ (i, j, k, p) : (i, j, k) \in F^{C}, t_{p} \ge t_{0}^{(i, j, k)}, t_{p+1} \\ \le t_{1}^{(i, j, k)}, p \in \{1, ..., n_{e}\} \} = \{ FSC_{1}, FSC_{2}, ..., FSC_{n_{FSH}} \}$$





Composite substreams

- Composite substreams are the merging of neighbor inherent streams of a heat stream
- If the (i, j, k) heat stream has d 1 inherent temperature intervals then $\binom{d+1}{2}$ subinterval exists
- Each subinterval has the form of $l_{qs} = [t_q, t_{s+1}]$, where $p \le q \le s \le p + d 1$





Composite substreams

Hot composite substreams

$$I^{H} = \{(i, j, k, q, s): (i, j, k) \in F^{H}, I_{qs} \\ \subseteq [t_{0}^{(i, j, k)}, t_{1}^{(i, j, k}]\} = \{SSH_{1}, SSH_{2}, \dots, SSH_{n_{SSH}}\}$$

Cold composite substreams

$$I^{C} = \{(i, j, k, q, s): (i, j, k) \in F^{C}, I_{qs} \\ \subseteq [t_{0}^{(i, j, k)}, t_{1}^{(i, j, k}]\} = \{SSC_{1}, SSC_{2}, \dots, SSC_{n_{SSC}}\}$$





Potential exchanges

- The potential exchanges of component substreams
- Define only for hot streams because it is symmetric





Potential exchanges

• Potential exchanges of hot component substreams with cold component substreams $IEE(SSH) = \{SSC, i = (i', i', k', a', s') \in I^C; a \leq I^C\}$

$$|FF(SSH_{l}) = \{SSC_{l'} = (i', j', k', q', s') \in I^{\circ} : q \le q', s \le s'\}, SSH_{l} = (i, j, k, q, s) \in I^{H}$$

Potential exchanges of hot component substreams with cold latent heat

$$JFL(SSH_{l}) = \{LC_{l'} = (j', i') \in L^{C}: t_{q} \le T_{i'j'}\}, \\ SSH_{l} = (i, j, k, q, s) \in I^{H}$$





Potential exchanges

Potential exchanges of hot latent heats with cold component substreams

$$JLF(LH_{l}) = \{SSC_{l'} = (i', j', k', q', s') \in I^{C}: T_{ij} \le t_{s'+1}\}, LH_{l} = (j, i) \in L^{H}$$

Potential exchanges of hot latent heats with cold latent heats

$$JLL(LH_{l}) = \{LC_{l'} = (j', i') \in L^{C}: T_{ij} \le T_{i'j'}\}, LH_{l} = (j, i) \in L^{H}$$





Heat exchanges with utility

Potential exchanges of cold component substreams with hot utility

$$JFU(FSC_l) = \{ u \in U^H : UT_u \ge t_{p+1} \}, FSC_l = (i, j, k, p) \in E^C$$

Potential exchanges of hot component substreams with cold utility

$$JFU(FSH_l) = \{u \in U^C : UT_u \le t_p\}, FSH_l = (i, j, k, p) \in E^H$$





Heat exchanges with utility

Potential exchanges of cold latent heats with hot utility

 $JLU(LC_l) = \{ u \in \mathbf{U}^H : UT_u \le T_{ji} \}, LC_l = (j, i) \in \mathbf{L}^C$

Potential exchanges of hot latent heats with cold utility

 $JLU(LH_l) = \{ u \in \mathbf{U}^C : UT_u \ge T_{ji} \}, LH_l = (j, i) \in \mathbf{L}^H$





Mathematical model

- Extension of the linear PNS model
- The constraints does not change
 - Lower bounds on the amounts of products to be manufactured to meet the demand
 - Availability of raw materials
 - Mass balance



NP ALLAN PROPERTY

hP-graph

- T ($\subseteq \mathcal{M}$) denotes the sot of materials which have temperature
- Let $m_i \in T$, $o_k \in \varphi^-(m_i)$ and $o_l \in \varphi^+(m_i)$
 - \square m_i^k and m_i^l denote the new material nodes belonging to o_k and o_l , respectively
 - $\begin{tabular}{ll} $$ $ t_{ik}^{out} $ and $ t_{il}^{in} $ denote $ the temperature $$ of m_i^k and m_i^l, respectively $$ $$
 - h_{i}^{kl} denotes the artificial operating unit of m_{i} from o_{k} to o_{l}
 - $\square w_i^{kl}$ the amount of material go through h_i^{kl}







Constraints for new materials

- M_i and K_i denote the set of new materials and the set of new operating units for $m_i \in T$, respectively
- Let $ir_{kj} = 1$ and $or_{kj} = 1$ for all $o_k \in \bigcup_{i \in T} K_i$ and $j \in \psi(o_k)$
- Let φ'^- and φ'^+ operator defines the operating units generating and consuming material of a hP-gráf, respectively





Constraints for materials

$$l_{i} \leq \sum_{\substack{o_{k} \in \varphi^{-}(i) \\ m_{i} \in \mathcal{M} \setminus T}} x_{k} or_{ki} - \sum_{\substack{o_{k} \in \varphi^{+}(i) \\ n_{j} \in \mathcal{M} \setminus T}} x_{k} or_{kj} - \sum_{\substack{o_{k} \in \varphi^{\prime^{+}}(j) \\ m_{j} \in M_{i}, m_{i} \in \mathcal{M} \setminus T}} x_{k} ir_{kj} \leq u_{j},$$





Heat transfer

The rate of release or absorption of heat

 Positive for hot streams and latent heats
 Negative for cold streams and latent heats

 Heat stream

$$QFH_{l} = c_{i}w_{i}^{jk}(t_{p+1} - t_{p}), FSH_{l} = (i, j, k, p) \in E^{H}$$
$$QFC_{l} = c_{i}w_{i}^{jk}(t_{p+1} - t_{p}), FSC_{l} = (i, j, k, p) \in E^{C}$$

Latent heat

$$QLH_{l} = h_{ji}x_{j}, LH_{l} = (j, i) \in L^{H}$$
$$QLC_{l} = h_{ji}x_{j}, LC_{l} = (j, i) \in L^{C}$$





Variables for heat transfer

- Define only for hot streams because it is symmetric
 - Nonnegative variables
- The first index denotes the hot and the second denotes the cold stream or latent heat

□
$$QFF_{ij}$$
: $SSH_i \in I^H$, $SSC_j \in JFF(SSH_i)$
□ QFL_{ij} : $SSH_i \in I^H$, $LC_j \in JFL(SSH_i)$
□ QLF_{ij} : $LH_i \in L^H$, $SSC_j \in JLF(LH_i)$
□ QLL_{ij} : $LH_i \in L^H$, $LC_j \in JLL(LH_i)$





Variables for utility

- Nonnegative variables
- The order of indexes denotes the direction of heat transfer, i.e. the first index is the hot source, the second one is the cold source

■
$$QFU_{iu}$$
: $FSH_i \in E^H$, $u \in JFU(FSH_i)$
■ QUF_{ui} : $FSC_i \in E^C$, $u \in JFU(FSC_i)$
■ QLU_{iu} : $LH_i \in L^H$, $u \in JLU(LH_i)$
■ QUL_{ui} : $LC_i \in L^C$, $u \in JLU(LC_i)$





Heat balance

For each hot latent heat (LH_l), the rate of heat is the sum of heat transfer to cold streams, cold latent heats and cold utilities






Heat balance

For each cold latent heat (LC_l), the rate of heat is the sum of heat transfer from hot streams, hot latent heats and hot utilities







Heat balance

• For each hot stream ($FSH_l = (i, j, k, p)$) all composite substream must be taking into account







Heat balance

• For each cold stream ($FSC_l = (i, j, k, p)$) all composite substream must be taking into account







Heat streams heat transfer cost

- Suppose materials m_i and $m_{i'}$ exchange heat
 - $\Box A_{ii'}$ denotes the unit cost of heat-transfer area
 - $\Box U_{ii'}$ denotes the heat transfer coefficient
- The cost of heat exchange between composite substreams SSH_l and SSC_l

1

$$CFF_{ll'} = A_{ii'} \frac{1}{U_{ii'}LMTD(t_s, t_{q+1}, t_{s'}, t_{q'+1})}$$

$$SSH_l = (i, j, k, q, s) \in I^H,$$

$$SSC_{l'} = (i', j', k', q', s') \in JFF(SSH_l)$$





LMTD

• Logarithmic mean temperature difference $LMTD(x_1, x_2, y_1, y_2) = \frac{(x_1 - y_1) - (x_2 - y_2)}{\ln \frac{x_1 - y_1}{x_2 - y_2}}$





Latent heats heat transfer cost

Let m a material which is used for heat transfer $CFL_{ll'} = A_{im} \frac{1}{U_{im}LMTD(t_s, t_{a+1}, T_{i'i'}, T_{i'i'})},$ $SSH_{l} = (i, j, k, q, s) \in I^{H}, LC_{l'} = (j', i')$ $CLF_{ll'} = A_{mi'} \frac{1}{U_{mi'}LMTD(T_{ii}, T_{ii}, t_{s'}, t_{q'+1})},$ $LH_{l} = (j, i) \in L^{H}, SSC_{l'} = (i', j', k', q', s') \in JFL(LH_{l})$ $CLL_{ll'} = A_{mm} \frac{1}{U_{mm}} \frac{2}{(T_{ji} + T_{j'i'})},$ $LH_{l} = (j, i) \in L^{H}, LC_{l'} = (j', i') \in JLL(LH_{l})$





Utilities heat transfer cost

- In the model the cost of the heat transfer is linear
 - \Box *UC_u* denotes the cost coefficient of utility *u*





Objective function

The cost of the PNS and the cost of the heat exchange

$$\min \sum_{o_i \in \mathcal{O}} (fix_i y_i + prop_i x_i) + \sum_{r_j \in \mathcal{R}} \left(price_j \sum_{o_i \in \varphi^+(j)} x_i ir_{ij} \right) \\ + \sum_{QFF_{jj'}} CFF_{jj'} QFF_{jj'} + \sum_{QFL_{jj'}} CFL_{jj'} QFL_{jj'} \\ + \sum_{QLF_{jj'}} CLF_{jj'} QLF_{jj'} + \sum_{QFU_{iu}} UC_u QFU_{iu} + \sum_{QLU_{iu}} UC_u QLU_{iu}$$





Solution

- It can be solved by a modified ABB algorithm
- The branching do not change
- The bounding contains the new extended model
 - The operating units excluded from the structure are not presented in the model





PNS and scheduling





Introduction

- In PNS the operating units are continuous
- In the real life processes can be batch processes
 - They consume all input materials at the start and produce output only at the finish
- An operating unit can be used in different locations of the system without overlapping the operation in time
 - Scheduling





Scheduling

- The input of a scheduling problem can be defined by the structure of the process (recipe) and the set available equipment units
 - Multiple equipment units are available for a task
 - The operating time of a task depends on the assigned equipment unit
- An equipment unit must be assigned to each task
- An equipment unit cannot work on multiple tasks simultaneously
- Changeover time is the shortest time between two task of the same equipment

□ Cleaning, setup, ...





Batch

- The production is based on batches
- To perform the recipe once generates one batch of a product
- If performing the recipe does not generate enough material, it has to be repeated
 - Multiple batches





Objective function

- Most common aims
 - Inimizing makespan for given amount of products
 - Maximizing profit in a given timehorizon
 - Minimizing earliness, tardiness
 - Due dates are given for products
 - Minimizing cost





S-graph framework

- To represent a scheduling problem and its solution we use a directed graph representation called S-graph
- A branch and bound algorithm can determine the optimal solution





Recipe-graph

- The recipe can be represented by a special Sgraph, so called recipe-graph
- Nodes denote the tasks (task-nodes) and the products (product-nodes)
- Recipe-arcs denote the order of the tasks
 - The direction of the arcs are same as the direction of the material flow
 - The weight of a recipe-arc is the minimal difference of the starting time of the two connected task-nodes
 - If multiple equipment units are available the weight is equal to the shortest operation time





- Three product (A, B, C) are to be produce
 Three consecutive steps for each
- The sets S1, S2, ..., S9 are the sets of available equipment units for the corresponding tasks

 (¹/_{E1}) ³ (²/_{S2}) ⁶ (³/_{S3}) ⁹ (¹⁰) ^A









Scheduling on S-graph

Scheduling

- Assign an equipment unit for each task
- Define a total order of the tasks of the same equipment unit
- Directed arcs (schedule-arcs) denote the operational order of equipment units
 - A schedule-arcs start from all the task-nodes following the actual node in the recipe-graph and point into the next task-node of the equipment unit
 - The weight of the arc is equal to the changeover time





- Equipment unit E1 starts it work on task 1
- Fills its material into equipment unit assigned to task 2
- Continues its work on task 6 then task 7







Schedule-graph

- An schedule-graph is a special acyclic S-graph which represents a solution
- There exists a unique schedule-graph for each solution
- In a schedule-graph all task (task-node) has been scheduled

According to the actual equipment-task assignment





- Blue schedule-arcs belong to E1
- Red schedule-arcs belong to E2
- Green schedule-arcs belong to E3







B&B algorithm

The most common aim is to minimize the makespan (the finishing time of the system)

□ The amount of product is given apriori

- The algorithm assign an equipment unit to a task in each step and determine its place in the activity list of the equipment unit
- The recipe-graph belongs to the root of the search tree
- A schedule-graph belongs to each leaf
- The bounding function is a longest path algorithm
 For feasibility test it uses cycle search algorithm





Integrated problem

PNS

Synthetize a process

- Scheduling
 - Schedule a given process
- Integrated problem
 - Synthetize a process which can generate all product in a given timehorizon





Integrated problem

- Operations (tasks) denotes the material transformations
 - Like operating units in PNS
- Operations can be performed by equipment units
 - Like in scheduling
- Aim
 - Determine the optimal structure
 - Give a feasible schedule in timehorizon





P-graph

- The P-graph of the synthesis problem is the base of the recipe
- The maximal structure must be acyclic
 - Cycles can be broken by introducing multiple batches





Integrated problem

- The equipment units assignment to operations affects the cost, the operating time and the capacity
- Cost are calculates from the costs of operations
 - Raw material costs are not taking into account
- Retrofit design
 - There are a set of available equipment units which have no investment cost
 - New equipment units can be purchased





Parameters

- The PNS parameters are the same
- Additional parameters are needed





Types of equipment units

- E is the set of equipment unit types
 - It contains the available and the purchasable types
- k_j is the number of available equipment units of type e_j
- cost_j is the investment cost of an equipment unit of type e_j
- The costs, the operating times and the capacities are same for two equipment units of the same type





Plausible equipment units

- $OE(o_i)$ is the set of plausible equipment unit types for performing operation o_i
- Suppose that the cost of performing operation o_i with equipment unit type e_j is linear
 - $\Box a_{ij}$ denotes the proportional cost
 - The total cost is $a_{ij}x_i$ where x_i variable denotes the capacity of the operation o_i





Mass flow

- The mass flow on a equipment unit has bounds
- low_{ij} and upp_{ij} is the lower and the bound of operation o_i using equipment unit type e_j , respectively

 $\Box \ low_{ij} \le x_i \le upp_{ij}$





Operating time

• $time_{ij}$ is the operating time of operation o_i performing by an equipment unit of type e_j

It does not depend on time mass flow

- $ctime_{ii'j}$ is the changeover time of an equipment unit of type e_j between performing operation o_i and $o_{i'}$
- TIME is the timehorizon





Solution procedure

- Based on ABB algorithm
- New decisions about equipment units
 - Assignment of equipment units to operations
 - Using an available equipment unit or buy new one
 - Scheduling





Search tree

- First level
 - Original decisions of ABB
- Second level
 - Choosing of equipment unit type
- Third level
 - Decision about buying or not buying equipment unit





- Let m_1 the current material
- It can be produced by operations o_1 and o_2
- Suppose that $OE(o_1) = \{e_1, e_3\}$, $OE(o_2) = \{e_2, e_3, e_4\}$
- There are available equipment units for each type











- Multiple decision where multiple types are available for an operation
 - $|OE(o_1)| * |OE(o_2)| = 6 \text{ decisions in the right side of the tree}$






Example

- Possible decisions
 - Two children buying, not buying
 - Three children buying one, buying two, not buying
 - Four children buying two, buying for the first, buying for the second, not buying





Bounding

- Lower bound for cost
- Feasibility check with scheduling





Lower bound

- Relaxation of the PNS model extended by constraints
 - \Box If operation o_i is excluded from the structure

 $0 \le x_i \le 0$

□ If o_i is included in the structure and the type of equipment unit (e_i) is decided

 $low_{ij} \le x_i \le upp_{ij}$

 \Box If o_i is included and type of equipment unit is not decided

$$\min_{e_j \in OE(o_i)} low_{ij} \le x_i \le \max_{e_j \in OE(o_i)} upp_{ij}$$

 \Box If there is no decision about o_i

$$0 \le x_i \le \max_{e_j \in OE(o_i)} upp_{ij}$$





Feasibility test

- Search for a scheduling of the structure with makespan less than timehorizon
- Scheduling works only in a fix structure
 - Solution-structure for the current decisions
- SSG algorithm can generate all solutionstructures
- The generation stops when feasible schedule has been found

One feasible schedule is enough





Scheduling of solutionstructures

- Fictive tasks for undecided operations
 - No equipment unit for them
 - Do not need to schedule
 - Operating time is the smallest operating time of the operation
- Recipe-graph is necessary for scheduling
 - \Box P-graph \rightarrow recipe-graph





P-graph \rightarrow recipe-graph

- One task-node for each operation
- One product-node for each product
- Recipe-arc for each connection
 - □ If o_i producing a material and o_j consuming it → recipe-arc from task-node of o_i to task-node of o_j
 - □ If o_i producing product \rightarrow recipe arc from task-node of o_i to the corresponding product-node
 - The weight of the arc is the smallest operating time of the potential equipment units



Example







Literature

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PNS Software Tools: PNS Draw and PNS Studio



Table of Contents

- PNS Draw
- PNS Studio
- Example







Introduction

- P-graph methodology is a good approach for
 - Process Design
 - Process Optimization
 - Flowsheet Optimization
 - Process Systems Engineering
 - Process Network Synthesis (PNS)
- The P-graph algorithms are supported by software tools
 - PNS Draw
 - PNS Studio





PNS Draw

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PNS Draw

- System Requirements
 - P3 800 CPU
 - 256 MB RAM
- Supported Windows Platforms:
 - Windows 2000 with Service Pack 3 and .NET 2.0
 - Windows XP with Service Pack 2 and .NET 2.0
 - Windows Vista
 - Windows 7
 - Windows 8





Features

- Draw materials, operating units, connections
- Edit connection arrow position and define breakpoints and Bezier curves
- For PNS : define object's name and flow rates
- Define colors for objects
- Multiple object moving
- Zoom
- Grid and align to grid
- Export P-graph to PNG image format, SVG vector graphics format, PNS Studio format
- One step Undo / Redo



- Adding materials and operating units
 - First option: Drag the material or operating unit symbol in the toolbar and drop to the editor area.
 - Second option: Change the draw mode in the toolbar to material or operating unit and click on the editor area to put them.







- Connecting objects
 - Select the Link option in the Drawing Mode dropdown list.
 - Click on the first object then click on the second object.







Selecting objects

- Click on the object to select one object.
- Press SHIFT key and click on another object to add to the selection, or remove from selection.
- Press down the left mouse button and move the mouse to select the objects. You can use the SHIFT key to add or remove objects from selection.





- Scroll and zoom
 - Zoom: Ctrl + mouse wheel
 - Scroll Up-Down: mouse wheel
 - Scroll Left-Right: SHIFT + mouse wheel
 - Move the editor area: press down the right mouse button and move the mouse





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Using PNS Draw Add and remove breakpoints to lines

- There are two breakpoints:
 - temporary (small dot)
 - line breakpoint (bigger dot)
 - Adding: Select a line (with left mouse button), the temporary breakpoints will be shown then move these to create new line breakpoints.
 - Removing: Select a line then select the line breakpoint then press the Delete key.





Keys

- Ctrl + U: undo
- Ctrl + Y: redo
- Ctrl + S: save
- Ctrl + C: copy
- Ctrl + V: paste
- Ctrl + D: duplicate
- Delete: delete selected objects
- Shift: invert selection
- Alt: free moving of objects (when snap to grid is on)

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PNS Draw Screenshot



Download link: <u>http://www.p-graph.com/pnsdraw/</u>





PNS Draw XML Output File Format

```
<Material ID="1" Name="material 1" Title="" Type="0">
      <ParameterList>
        <Parameter Name="price" Prefix="Price: " Value="-1" MU="" Visible="false" />
        <Parameter Name="reqflow" Prefix="Required flow: " Value="-1" MU=""
                                                                        Visible="false" />
        <Parameter Name="maxflow" Prefix="Maximum flow: " Value="-1" MU=""
                                                                        Visible="false" />
      </ParameterList>
      <Coords>
        <x>900</x>
        <Y>300</Y>
      </Coords>
      <Label Text="">
        <Offset>
          <X>103</X>
          < Y > -100 < /Y >
        </Offset>
        <FontSize>-1</FontSize>
        <Color>-16777216</Color>
      </Label>
          . . .
```





PNS Draw XML Output File Format

<OperatingUnit ID="3" Name="operatingunit 1" Title=""> <ParameterList> <Parameter Name="caplower" Prefix="Capacity, lower bound: " Value="-1" MU="" Visible="false" /> <Parameter Name="capupper" Prefix="Capacity, upper bound: " Value="-1" MU="" Visible="false" /> <Parameter Name="investcostfix" Prefix="Investment cost, fix: " Value="0" MU="" Visible="false" /> <Parameter Name="investcostprop" Prefix="Investment cost, proportional: " Value="0" MU="" Visible="false" /> <Parameter Name="opercostfix" Prefix="Operating cost, fix: " Value="0" MU="" Visible="false" /> <Parameter Name="opercostprop" Prefix="Operating cost, proportional: " Value="0" MU="" Visible="false" /> <Parameter Name="payoutperiod" Prefix="Payout period: " Value="-1" MU="" Visible="false, /> <Parameter Name="workinghour" Prefix="Working hours per year: " Value="-1" MU="" Visible="false" />

</ParameterList> <Coords> <X>900</X> <Y>900</Y> </Coords>

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PNS Studio

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PNS Studio

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 - At least P3 800 CPU
 - □ At least 256 MB RAM
- Supported Windows Platforms:
 - Windows 2000 with Service Pack 3 and .NET 2.0
 - Windows XP with Service Pack 2 and .NET 2.0
 - Windows Vista
 - Windows 7
 - Windows 8





PNS Studio

• 4 parts of window: materials, operating units, parameters of materials, paramters of operating units

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PNS Studio: Materials

- Materials: raw materials, intermediates, and products
- Operating units with input and output materials

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PNS Studio: Default values Options menu

→ Default Values

| | Default Values × | | | | |
|---|-----------------------------|--------------------|------------------|--|--|
| | Material | | | | |
| | Required flow | 0 (e.g.: t/yr) | | | |
| | Maximum flow | 10000000 (e.g.: t. | /yr) | | |
| | Price | 0 (e.g.: €/t) | | | |
| | Operating unit | | | | |
| | Flow rate | 1 (e.g.: t/yr) | | | |
| | Operating cost | | | | |
| | Fixed charge | 0 €/yr | | | |
| | Proportionality constant | 0 €/yr | | | |
| | Investment cost | | | | |
| | Fixed charge | 0€ | | | |
| | Proportionality constant | 0€ | | | |
| | Capacity constraints | | | | |
| | Lower bound | 0 | | | |
| | Upper bound | 10000000 | | | |
| | Solver numerical limits | | | | |
| | Upper limit | 10000000 | | | |
| | Maximum number of solutions | 10 | | | |
| R | equired flow | | | | |
| | Update | Cancel | Restore defaults | | |

0/0



PNS Studio: Default Measurement Units

Options menu

 → Default
 Measurement
 Units

| Default Measurement Units | | | | | |
|---|-------------------------------------|-------------------|------------------|---|--|
| | Default measurement units of a | vailable quantity | types | ~ | |
| | mass | t | ~ | | |
| | volume | m ³ | | | |
| | amount of substance | kmol | | | |
| | energy, work, quantity of heat | MJ | | | |
| | time | уг | | | |
| | currency | € | | | |
| | length | m | | | |
| | electric current | A | | | |
| | area | m² | | | |
| | speed | m/s | | | |
| | acceleration | m/s ² | | | |
| | force | N | | | |
| | power | MW | | | |
| | capacity | unit | | | |
| Ξ | Default ratios of time units | | | | |
| | Default working hour per year value | 8000 h/yr | | | |
| | Default payout period value | 10 yr/payout per | iod | | |
| Ξ | Default quantity type | | | | |
| | Default quantity type | mass | | | |
| Ξ | Default derived units based on | quantity, time ar | nd currency | | |
| | Default material flow MU | t/yr | | | |
| | Default price MU | €/t | | | |
| | Default investment cost MU | € | | | |
| | Default operating cost MU | €/yr | | | |
| Ξ | Default measurement unit conv | ersion | | | |
| | Automatically convert values | False | | ~ | |
| mass Selecting this quantity type item as material quantity type, item value will be used to generate default quantity based derived measurement units. | | | | | |
| | Update | Cancel | Restore defaults | | |





PNS Studio: Parameters of materials and operating units

| A - Material properties | | | | |
|--|-----------------|-------------------------|--|--|
| Name | A | | | |
| Туре | product | | | |
| Quantity type | mass | | | |
| Required flow | 4 t/yr | | | |
| Required flow Mu | t/yr | | | |
| Maximum flow | 10000000 | 10000000 t/yr (default) | | |
| Maximum flow Mu | t/yr | | | |
| Price | 0 €/t (default) | | | |
| Price Mu | €∕t | | | |
| Description | Description | | | |
| Name Name of the material. It must be unique in the problem definition. Convert values automatically | | | | |
| Update | Cancel | Delete | | |

| 03 | - Operating Unit properties | | | | |
|--|-----------------------------|----------------|------------------|---|--|
| Ξ | Basic | | ^ | | |
| | Name | 03 | | | |
| | Working hours per year | 8000 h/yr (de | fault) | | |
| | Payout period | 10 yr/payout j | period (default) | | |
| Ξ | Capacity constraints | | | | |
| | Capacity constraints | | | | |
| | Lower bound | 0 (default) | | | |
| | Upper bound | 10000000 (d | lefault) | | |
| | Cost parameters | | | | |
| | Operating cost | | | | |
| | Fixed charge | 2 €/yr | | 1 | |
| | Fixed charge Mu | €/yr | | | |
| | Proportionality constant | 1€/yr | | | |
| | Proportionality constant Mu | €/yr | | | |
| | Investment cost | | | | |
| | Fixed charge | 0€ | | | |
| | Fixed charge Mu | € | | | |
| | Proportionality constant | 0€ | | | |
| | Proportionality constant Mu | € | | | |
| | Overall cost | | ~ | • | |
| Name Name of the operating unit. It must be unique in the problem definition. Convert values automatically | | | | | |
| | Update Ca | ancel | Delete | | |





PNS Studio: P-graph algorithms

- Options menu → Synthesize menu
- MSG is the abbreviation of Maximal Structure Generation, which is an algorithm for PNS problems polynomial time



that determines maximal structure for the problem in

- SSG is an algorithm that determines the all feasible solution structure for a PNS problem
- SSG+LP and ABB: To get the optimal structure we have to run the SSG+LP or ABB algorithm





PNS Studio: Example







PNS Studio: Result of MSG algorithm

| 低大 | | | | |
|--|---|--------------|----------|--|
| File | Synthesize | Options | Help | |
| i 🗋 🛛 | j 📔 💿 | | | |
| Problem | 1 Solutions [M | SG] - MintaP | elda.pns | |
| Materia E, F, A Operati O3, O4 Maxima Materia E, F, A Operati O3, O4 | als(7): , G, C, D, B ing units(4): , O1, O2 al Structure: als(7): , G, C, D, B ing units(4): , O1, O2 | | | |
| End. | | | | |







PNS Studio: Result of SSG algorithm

| 1 . | MintaPelda.pns - Pns Studio | - 0 × |
|---|-----------------------------|-------|
| File Synthesize Options Help | | |
| i 🗋 📂 🛃 🞯 | | - |
| Problem Solutions [SSG] - MintaPelda.pns | | |
| Materials(7): E. F. A. G. C. D. B Operating units(4): O3, O4, O1, O2 | | ^ |
| Maximal Structure: Materials(7): E, F, A, G, C, D, B Operating units(4): 03, 04, 01, 02 | | |
| Solution structure #1: Materials(4): E, A, G, C Operating units(2): O3, O1 | | |
| Solution structure #2: Materials(5): F. A, G, C, D Operating units(2): 04, 01 | | |
| Solution structure #3: Materials(6): E, F, A, G, C, D] Operating units(3): O3, O4, O1 | | |
| Solution structure #4: Materials(5): F, A, C, D, B Operating units(2): O4, O2 | | |
| Solution structure #5: Materials(6): F, A, G, C, D, B Operating units(3): 04, 01, 02 | | |
| Solution structure #6: Materials(7): E, F, A, G, C, D, B Operating units(4): O3, O4, O1, O2 | | |
| End. | | * |
| | | |



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PNS Studio: Result of SSG algorithm

Materials(7): E, F, A, G, C, D, B Operating units(4): O3, O4, O1, O2

Maximal Structure: Materials(7): E, F, A, G, C, D, B Operating units(4): O3, O4, O1, O2

Solution structure #1: Materials(4): E, A, G, C Operating units(2): 03, 01

Solution structure #2: Materials(5): F, A, G, C, D Operating units(2): O4, O1 Solution structure #3: Materials(6): E, F, A, G, C, D Operating units(3): O3, O4, O1

Solution structure #4: Materials(5): F, A, C, D, B Operating units(2): O4, O2

Solution structure #5: Materials(6): F, A, G, C, D, B Operating units(3): 04, 01, 02

Solution structure #6: Materials(7): E, F, A, G, C, D, B Operating units(4): O3, O4, O1, O2

683 Contraction of the second second

End.



PNS Studio: Parameters for the PNS problem

| Operating units | Fixed charge | Proportional cost |
|------------------------|--------------|-------------------|
| 01 | 4 | 1 |
| 02 | 3 | 1 |
| 03 | 2 | 1 |
| 04 | 2 | 0.5 |

| Raw material | Constraint |
|--------------------------|----------------------------|
| Е | ≤ 10 |
| Product | Constraint |
| А | ≥ 4 |
| | |
| Raw material | Price |
| Raw material E | Price 0.8 |
| Raw material E F | Price 0.8 1.6 |




PNS Studio: Optimal and 2nd best solution

| 低人 | MintaPelda.r | |
|---|---|---------------|
| File Synthesize Options Help | | |
| 🗋 💕 🛃 🞯 | | |
| Problem Solutions [SSGLP] - MintaPelda. | ons (3) | |
| Solution #1: Total cost: 11,2 €/yr | ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ | |
| ⇒ Solution #1: Total cost: 11,2 €/yr ⇒ Materials: ⇒ E: consumed amount = 4 t/yr ⇒ A: produced amount = 4 t/yr, ⇒ G: balanced ⇒ C: balanced | , Cost: 3,2 €/yr Cost: 0 €/yr | MintaPelda.pr |
| i Operating units: i O3, Size factor: 1, Cost: 3 €/γ i O1, Size factor: 1, Cost: 5 €/γ | rr r Problem Solutions [INSIDEOUT] - MintaPelda.pns (3) | |
| | Solution #2: Total cost: 13,1456 €/yr | ¥ |
| | Solution #2: Total cost: 13,1456 €/yr Materials: E: consumed amount = 3,872 t/yr, Cost: 3,0976 €/yr F: consumed amount = 1,6 t/yr, Cost: 0 €/yr A: produced amount = 4 t/yr, Cost: 0 €/yr G: produced amount = 0,032 t/yr C: balanced D: produced amount = 1,44 t/yr Operating units: O3, Size factor: 0,968, Cost: 2,968 €/yr O4, Size factor: 0,16, Cost: 2,08 €/yr O1, Size factor: 1, Cost: 5 €/yr | |





Webpage: www.p-graph.com

| •× • P-graph F | ior: Process Synthesis; Process + | | _ 0 |
|---------------------------|---|----------------------------------|-------|
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| ature Review | For broad and outstanding contributions to the analysis, synthesis, and control of process and material sy | ystems. | |
| <u>onstration</u> rams | The CAST Award Lecture: | | |
| ed Sites | from Microscopic World to Microscopic World through Mazes of Process Graphs and from Microscopic World to Mesoscopic World through Drunkards' Paths | | |
| <u>rs</u> | by L. T. Fan | | |
| <u>e Wiki</u> | Download PowerPoint presentation. | | |
| o Webmaster | Book chapter about the P graph framework in a major chemical engineering textbook | | |
| | Web Site for Chapter 4 Flowsheet Synthesis and Development of Plant Design and Economics for Chemical Engineers Fifth Edition By Peters, Timmerhaus, and West | | |
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